

# Experimental investigation of flow pattern and sediment deposition in rectangular shallow reservoirs

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## Abstract

This work involved the experimental investigation of flow pattern, preferential regions of deposition and trap efficiency as a function of the length of rectangular shallow reservoirs. Four flow patterns were identified (from longer to shorter reservoirs): an asymmetric flow with two reattachment points, an asymmetric flow with one reattachment point, an unstable flow, and a symmetric flow without any reattachment point. Using dye visualizations, the median value and the temporal variability of the reattachment lengths were precisely measured for the asymmetric flows. For each stable flow, sediment tests with plastic particles were carried out. The regions of deposition on the bed of the reservoir were clearly a function of the flow pattern. The transition from an asymmetric flow pattern to a symmetric flow pattern was responsible for an abrupt decrease of the trap efficiency; a number of regression laws were discussed to take it into account.

**Key Words:** Deposition, Flow patterns, Reservoirs, Sediment, Shallow water

## 1 Introduction

Tanks, basins, ponds, lagoons (called reservoirs below) are commonly used in hydraulic engineering. Because of generally quiescent conditions, these works are conducive to the

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1 settling of particles. Therefore, reservoirs must be carefully designed according to the role  
2 they will play. For example, sedimentation must be maximized in settling basins (stormwater  
3 treatment, protection of irrigation or hydro-electric power structures, *etc.*) whereas it must be  
4 minimized in storage facilities (irrigation, hydro-electric power generation, flood control,  
5 *etc.*).

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7 The prediction of deposition as a function of the geometry of the reservoir, the hydraulic  
8 conditions and the sediment characteristics is still a great challenge. While empirical and  
9 semi-empirical methods have been developed for the last sixty years to determine the amount  
10 of deposits (see for example Jothiprakash and Garg 2008 for reservoirs, Garde *et al.* 1990,  
11 Ranga Raju *et al.* 1999 for basins; Kowalski *et al.* 1999 for combined sewer detention tanks;  
12 Luyckx *et al.* 1999 for high side weir overflows), they cannot determine their spatial  
13 distribution, which is required to well define the sediment removal strategy. To get this  
14 information, the knowledge of the flow pattern is a prerequisite. It is also questionable  
15 whether the relative imprecision of these methods is not because they express the trap  
16 efficiency of the reservoir (the ratio of the deposited mass to the incoming mass) without  
17 taking into account the flow pattern.

18  
19 Saul and Ellis (1992) highlighted that complex flow patterns take place in rectangular storage  
20 tanks and that the flow pattern governs the sediment transport processes. Stovin and Saul  
21 (1994) carried out experiments in a 2.00 m long and 0.97 m wide storage tank. The circular  
22 inlet and outlet were respectively 0.19 m and 0.15 m in diameter. The water depth was about  
23 0.20 m (the geometry was quasi bi-dimensional). The velocity in the inflow pipe was 0.56  
24 m/s. Crushed olive stone was used as the model sediment (median grain size  $\approx 0.050$  mm,  
25 density  $\approx 1,500$  kg/m<sup>3</sup>). The writers showed that the flow field was characterised by a large

1 clockwise circulation and a small counter clockwise circulation in the upstream left corner of  
2 the tank (asymmetric flow pattern); deposits were located in three preferential regions: in both  
3 upstream corners of the tank and in the core of the large circulation zone. Varying the inflow  
4 velocity (in the range  $\approx 0.1 - 0.7$  m/s), Stovin and Saul (1996) proposed a linear relationship  
5 between the percentage of the bed that is covered by deposits and the trap efficiency.

6  
7 Kantoush et al. investigated the influence of the geometry of shallow reservoirs on flow  
8 patterns and sedimentation by suspended sediments (Kantoush 2008, Kantoush *et al.* 2008).  
9 His benchmark case was a 0.20 m high water flow entering a 6.00 m long and 4.00 m wide  
10 reservoir by a 0.25 m wide channel at a velocity of 0.14 m/s. In this situation the main flow  
11 was deflected on the right wall, leading to the formation of a large counter clockwise  
12 circulation zone in the whole structure and a small clockwise circulation zone in the right inlet  
13 corner (the jet may also be deflected on the left wall, depending on the experiment). Similar  
14 patterns were observed when decreasing the breadth of the reservoir (3.00 m, 2.00 m, 1.00 m  
15 and 0.50 m for which the flow was fully reattached in the downstream zone of the reservoir).  
16 Asymmetry disappeared when decreasing the length of the reservoir (5.00 m, 4.00 m, and  
17 3.00 m). For these geometries, the jet was not deflected at entrance in the reservoir, leading to  
18 the formation of two large symmetric circulation zones. The writer used crushed walnut shells  
19 (median grain size  $\approx 0.050$  mm, density  $\approx 1,500$  kg/m<sup>3</sup>) to study morphological evolution.  
20 Nevertheless, the flow pattern was not steady during sediment tests, probably because of the  
21 large amount of deposits near the inlet of the reservoir (these deposits led to change the  
22 direction of the jet entering the basin during experiments).

23  
24 A number of experimental studies were conducted in more complex geometries. Modifying  
25 the basic chamber configuration described above, Stovin (1996) highlighted some effects of

1 the gradient benching and the length to breadth ratio on sediment distribution. Dufresne *et al.*  
2 (2009) showed that flow and sediment distribution became quasi-symmetric when increasing  
3 the water level above the top of the inlet pipe. The influence of columns and obstacles (a wall  
4 located in front of the inlet) on sediment deposition was also investigated (Dufresne 2008).

5

6 This study focuses on rectangular shallow reservoirs, as illustrated in Figure 1. Here,  $L$  =  
7 length of the reservoir;  $B$  = breadth of the reservoir;  $b$  = breadth of the inlet and outlet  
8 channels;  $\Delta B$  = lateral expansion;  $h$  = water depth; and  $U$  = inflow velocity. The aim of this  
9 work is firstly to investigate the preferential regions of deposition for the main flow patterns  
10 that can take place in rectangular shallow reservoirs; secondly, to study the influence of the  
11 flow pattern on the trap efficiency.

12

## 13 **2 Experimental investigation**

### 14 2.1 Experimental set-up

15 The experiments were carried out at the engineering hydraulics laboratory of the University of  
16 Liège, Belgium. The experimental set-up diagrammatically shown in Figure 1 consisted of a  
17 10.40 m long and 0.985 m wide glass channel in which blocks can be arranged to build  
18 different geometries of rectangular reservoirs. The base of the flume was horizontal.

19

20 The flow entered the channel from a stilling basin through a porous screen in order to prevent  
21 fluctuations in water level and make the velocity field uniform. The flow was then contracted  
22 to the desired breadth of the inlet channel ( $b$ ) in a converging section with circular shape; the  
23 inlet section of the reservoir (with straight parallel walls) was 2.00 m long. At the entrance of  
24 the reservoir, the flow suddenly expanded to the breadth of the reservoir ( $B$ ). At the exit of the  
25 reservoir, the flow suddenly contracted to the outlet channel breadth ( $b$ ). The outlet channel

1 was 1.00 m long; its downstream boundary corresponded to a gate (to control the water level)  
2 and a waterfall. All the surfaces were made of glass, except the two parallel walls of the inlet  
3 and outlet channels (PVC) and the converging section (metallic sheets). In this study, the  
4 lateral expansion equaled 0.350 m. Three lengths were investigated: 1.80, 2.20 and 7.00 m;  
5 they were chosen after trial and error so that different flow patterns could be observed  
6 (symmetric flow, asymmetric flow with one reattachment point and asymmetric flow with  
7 two reattachment points).

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9 The volumetric flow rate was measured with an electromagnetic flowmeter upstream of the  
10 flume; it was also measured with a triangular weir in the water collection channel downstream  
11 of the waterfall in order to enhance accuracy on small values. Water depth in the reservoir  
12 was measured with a level meter in the middle of the breadth 0.10 m downstream of the  
13 entrance of the reservoir and 0.10 m upstream of the exit of the reservoir. The maximum  
14 difference between the two values was 0.002 m. Therefore only the upstream value is reported  
15 hereafter.

## 16 17 2.2 Sediment

18 Granular plastic (Styrolux 656 C) was chosen as the model sediment. The particles were  
19 elliptical cylinders with a density of  $1020 \text{ kg/m}^3$  (given by the producer BASF). We randomly  
20 selected 30 particles and measured their dimensions using a Vernier caliper, and their fall  
21 velocities in a water column. The results show that the sediment characteristics are relatively  
22 uniform (see Table 1). Based on these measurements, 2.4 mm (cube root of the mean volume)  
23 was chosen as the characteristic sediment size; 25 mm/s, as the characteristic fall velocity.

## 24 25 2.3 Experimental procedure

1 After preliminary sediment tests, one single inflow velocity was chosen for all the  
2 experiments (0.28 m/s). This velocity was sufficiently high to avoid deposition in the inlet  
3 channel and near the entrance of the reservoir (in order to avoid modifications of the direction  
4 of the incoming jet), and sufficiently low to allow deposition in the reservoir.

5

6 Two kinds of experiments were carried out. The first one consisted in flow tests; their aim  
7 was to describe (qualitatively and quantitatively) the flow pattern. The second one consisted  
8 in sediment tests; their aim was to describe the spatial distribution of deposits and the trap  
9 efficiency of the reservoir. The experimental conditions are given in Table 2 (flow tests) and  
10 Table 3 (sediment tests). Here,  $U$  = velocity in the inlet channel;  $\rho$  = water density;  $\mu$  = water  
11 viscosity;  $g$  = gravitational acceleration;  $u_*$  = shear velocity;  $\rho_s$  = sediment density,  $d$  =  
12 sediment size;  $w$  = sediment fall velocity; and  $q_s$  = sediment discharge. The uncertainty was  
13 about 0.002 m in the water depth (level meter) and about 0.01 m/s in the velocity (based on  
14 uncertainties in discharge and water depth). The water temperature was between 18 and 20°C,  
15 depending on the experiment. In order to check the reproducibility, all the experiments were  
16 repeated (except test F15-a for which the flow did not stabilize). Successive tests are named  
17 “a”, “b”, etc.

18

## 19 2.4 Flow tests

20 Visual investigations employing dye injections disclosed the flow pattern: symmetry or  
21 asymmetry, number of circulation zones, approximate locations of reattachment points.  
22 Despite steady boundary conditions, a wake zone (characterized by unsteadiness) took place  
23 downstream of the entrance of the reservoir. Therefore, successive dye injections were  
24 generally needed to describe a “mean” behavior.

25

1 The reattachment is defined as the point upstream of which the longitudinal velocity is  
2 negative (from downstream to upstream) and downstream of which the longitudinal velocity  
3 is positive (from upstream to downstream). Because of the unsteadiness of the flow, Chu et al.  
4 (2004) proposed to define it as “the point where the movements to the upstream and  
5 downstream directions are equally probable” (this definition corresponds to the median  
6 reattachment). To our knowledge, only the median position has been reported in the literature,  
7 using for example visualization of displacement of confetti on the water surface (Babarutsi *et*  
8 *al.* 1989, Babarutsi and Chu 1991, Chu *et al.* 2004). Only Abbott and Kline (1962)  
9 characterized the fluctuations of the reattachments lengths by taking a large number of points  
10 (see for example Figures 11 and 12 of their paper: the writers showed a band of two  
11 regression curves instead of a single one). In the present study, we better characterized these  
12 fluctuations by determining the velocity distribution along the wall near the median  
13 reattachment. Preliminary tests allowed us to define the following protocol.

14

15 Once the reattachment had been roughly located by dye visualization, the method consisted in  
16 injecting drops of dye at various points against the wall near the reattachment point. In each  
17 point, 100 drops of dye were injected at a frequency of one drop every 2 seconds; for each  
18 drop, the sense of the flow was observed by eye. A displacement of the dye from upstream to  
19 downstream corresponded to a positive velocity whereas a displacement from downstream to  
20 upstream corresponded to a negative velocity. The number of injected drops (100) and the  
21 duration of measurement (100 times 2 seconds) were chosen after preliminary tests to ensure  
22 a statistically meaningful result. Since the objective of this work is the study of deposits, the  
23 reattachment lengths were measured near the bottom of the reservoir (0.04 m above the bed).  
24 Nevertheless, “reasonable” two-dimensionality of the flow was always checked by dye  
25 visualization.

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A 95% confidence interval of the proportion of negative velocities was calculated using a small sample method in order to estimate the “uncertainty” of each measurement (see Wonnacott and Wonnacott 1977, p. 224). The 95% confidence intervals of the median reattachment lengths were determined using interpolations of the upper-bounds and lower-bounds of the confidence intervals between locations for which the proportions are closest to 50%. The 95% confidence intervals of the median reattachment lengths are given in Table 2 ( $R_1$  and  $R_2$  for respectively the shorter one and the longer one).

Another piece of information was extracted from these measurements: the reattachment lengths fit a normal distribution. By minimizing the sum of the differences between the measured and the normal proportions in square, the mean,  $\mu$ , and the standard deviation,  $\sigma$ , of a Gaussian distribution were determined. These values are also given in Table 2.

Table 4 summarizes the flow conditions in a dimensionless form. Based on dimensional analysis and literature, six dimensionless flow parameters govern the flow pattern: the dimensionless length (ratio of the length to the lateral expansion), the lateral expansion ratio (ratio of the lateral expansion to the breadth of the inlet channel), the vertical confinement (ratio of the lateral expansion to the water depth), the Reynolds number, the Froude number, and the bed friction number (see Table 4). Here,  $c_f$  is the bed friction coefficient; it was estimated using the formula recommended by the ASCE task force on friction factor in open channel flow (see Henderson 1966, p. 95). The bed friction coefficient was used to estimate the shear velocity too. Instead of the lateral expansion  $\Delta B$ , the breadth  $B$  could have been used as the representative lateral dimension of the reservoir.



1 In order to allow asymmetric flow patterns to develop in long basins, a lateral expansion ratio  
2 greater than 0.25 was chosen (see Abbott and Kline 1962 about “infinitely” long reservoirs).  
3 The vertical confinement was chosen sufficiently low to avoid friction effect: the friction had  
4 probably no influence on the flow pattern since 0.003 is small compared to the critical values  
5 highlighted in the literature (0.05 – 0.10 for unilateral expansions, see Chu *et al.* 2004). The  
6 dimensionless lengths were chosen by trial and error in order to find the transition between  
7 asymmetric and symmetric flows. Based on preliminary tests about sediment transport (see  
8 above), a Froude number of 0.20 was chosen. The range of Reynolds numbers shows that the  
9 flows were fully turbulent.

10

## 11 2.5 Sediment tests

12 In order to avoid flocculation, the plastic sediment was wet prior to experiment. It was input  
13 into the inflow 2.00 m upstream of the entrance of the reservoir. The injection consisted in  
14 discrete batches of 80 g (dry mass) over 10 second time intervals. The total period of injection  
15 was 10 minutes for each experiment. The inflow concentration was 0.50 g/L. Based on  
16 uncertainties in discharge, sediment mass and time period, the uncertainty in the inflow  
17 concentration was about 0.02 g/L.

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19 Using a net, particles were collected in the waterfall downstream of the reservoir in three time  
20 periods: between 2 and 4 minutes after the beginning of the injection, between 5 and 7  
21 minutes, and between 8 and 10 minutes. Each sample was dried and weighted, so that the  
22 mean outflow concentration could be calculated for the three time intervals. The trap  
23 efficiency,  $\eta$ , was calculated for each period using Equation 1. Here,  $c_{in}$  = inflow  
24 concentration;  $c_{out}$  = outflow concentration.

$$25 \quad \eta = \frac{c_{in} - c_{out}}{c_{in}} \quad (1)$$

1 The uncertainty in the outflow concentration was between 0.005 and 0.020 g/L (depending on  
2 the outflow concentration), which leads to an absolute uncertainty in the efficiency of 10% –  
3 15% (0.10 – 0.15).

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5 For each experiment, the bed of the reservoir was filmed over time in order to monitor the  
6 deposits. The spatial distributions of deposits given below are based on these movies.

7

8 Table 5 summarizes the dimensionless sediment parameters: the dimensionless bed shear  
9 stress, the particle Reynolds number (calculated with the shear velocity), the dimensionless  
10 fall velocity (ratio of the fall velocity to the shear velocity), and the dimensionless solid  
11 discharge. Observations by eye showed that bed-load and suspended load coexisted in the  
12 inlet channel (the dimensionless fall velocity was about 2). However, bed-load was the  
13 predominant mode of transport in the reservoir.

14

### 15 **3 Results**

#### 16 3.1 Flow patterns

17 Dye visualizations highlighted four different flow patterns. They are reported in Tables 2 and  
18 3.

19

20 When the length of the reservoir was 1.80 m, the flow presented a symmetric behavior, as  
21 illustrated in Figure 3 (pattern S0). The jet went in a straight way from the entrance to the exit  
22 of the reservoir; two symmetric circulation zones took place in the reservoir. It was also  
23 observed that the counter-currents detached from the wall approximately 0.3 m downstream  
24 of the inlet section of the reservoir, leading to the formation of a small circulation zone in  
25 each upstream corner. This zone was not drawn as a two-dimensional circulation in Figure 3

1 because dye visualization highlighted three-dimensional effects (vertical eddies); this  
2 behavior is consistent with the observations of Abbott and Kline (1962).

3

4 Symmetry disappeared when increasing the length of the reservoir to 2.20 m. The jet was  
5 deflected on one side of the reservoir. It reattached the wall after a distance named  $R_1$  in figure  
6 3, which led to the formation of a large circulation zone. A smaller circulation zone took place  
7 upstream of the reattachment. This flow pattern is denoted by “A1”.

8

9 For intermediate length (2.00 m), the flow did not stabilize in spite of steady boundary  
10 conditions: it fluctuated between a symmetric behavior (S0) and an asymmetric behavior  
11 (A1). The fluctuations between these two patterns were not periodic and seemed to be  
12 completely random. This type of flow is reported as “A1/S0” in Table 2. Even if the flow was  
13 unsteady in this situation, it was completely different from the meandering jet (periodic  
14 behavior) observed by Kantoush (2008) when decreasing the water depth below 0.20 m.

15

16 For the longest reservoir (7.00 m), the flow still remained asymmetric. As for a length of 2.20  
17 m, the flow reattached on one side of the reservoir after a distance  $R_1$  but also possibly on the  
18 opposite wall after a distance  $R_2$ . In this situation, the flow was fully reattached in the  
19 downstream zone of the basin (all the x-velocities in a transversal section are positive).  
20 Successive dye visualizations showed that the longer reattachment was highly unsteady, and  
21 sometimes completely missing. This third stable pattern is illustrated in Figure 3 (A2).

22

23 These results highlight a transition between symmetric and asymmetric flows for a  
24 dimensionless length in the range 5.1 – 6.3 (the flow was symmetric below and asymmetric  
25 above). This critical range is different from the results of the experiments carried out by

1 Kantoush (2008) for which the transition occurred for a dimensionless length in the range  
2 2.7 – 3.2. This shows that the dimensionless length is not sufficient to predict the flow  
3 pattern; additional dimensionless parameters from Table 4 are needed. There have been  
4 several attempts to define a criterion for forecasting the flow pattern in rectangular shallow  
5 reservoirs, from the simplest length to breadth ratio (Kantoush 2007) to more complex criteria  
6 involving the length of the reservoir, its breadth (eventually the lateral expansion) and the  
7 breadth of the inlet channel (Kantoush 2008, Dewals et al. 2008, Dufresne 2008). Among  
8 these criteria, only the one defined in Equation (2) and based on numerical simulations of  
9 Dufresne (2008) is consistent with the two experimental campaigns. Indeed, the range  
10 corresponding to the transition highlighted by Kantoush (2.2 – 2.6) partially overlaps the  
11 range highlighted in the present study (2.3 – 2.9). Moreover, these two ranges are consistent  
12 with the critical value that Dufresne (2008) recommended: symmetric flows below 2.36 and  
13 asymmetric flows above 2.36.

$$14 \quad A_L = \frac{L}{B} \left( \frac{B}{b} \right)^{0.2} = \frac{L}{B^{0.8} b^{0.2}} \quad (2)$$

15 Nevertheless, the relatively close hydraulic conditions of the two campaigns raise the question  
16 of the validity of this geometrical criterion in more general situations (various water depths  
17 and various velocities). Further investigations varying the lateral expansion ratio, the vertical  
18 confinement and the Froude number are currently in progress in order to find a general  
19 criterion.

20

### 21 3.2 Reattachment lengths

22 Figures 4 and 5 display the negative velocity distributions near reattachment for the  
23 experimental condition F4 (tests “a” and “c”), which corresponds to the flow pattern A2.  
24 Using these figures, the median reattachment length and the range of fluctuation of the  
25 reattachment length can be precisely determined. In Table 2, the median reattachment length

1 is given using a 95% confidence interval (measurement uncertainty); the range of fluctuation  
2 is given using the mean and the standard deviation of a Gaussian distribution (temporal  
3 variability). From Figure 4, we are for example 95% confident that the median reattachment  
4 length  $R_1$  of experiment F4-a was between 1.16 and 1.21 m. Using the normal distribution,  
5 one can also extract that the reattachment length was between 1.05 and 1.31 m during 80% of  
6 the time; it was smaller than 1.05 m during 10% of the time, and greater than 1.31 m during  
7 10% of the time.

8  
9 The comparison between Figures 4 and 5 highlights the different nature of the two  
10 reattachments. Whereas the first one was rather steady over time (standard deviation about  
11 0.10 m), the second one was highly unsteady (2.1 m), which means that it fluctuated over a  
12 long distance on the wall of the reservoir. Here, it must be precised that the distribution of the  
13 negative velocities of the second reattachment is not rigorously normal (one can see in Figure  
14 5 that the distribution of the second reattachment length is truncated by the downstream wall  
15 of the reservoir). Nevertheless, we also describe the second reattachment using the mean and  
16 the standard deviation of a Gaussian law in order to make possible comparison between  $R_1$   
17 and  $R_2$ . At a distance of 6.5 m from the entrance, the proportion of negative velocities was  
18 close to 50%, which means that the reattachment completely disappeared during about half  
19 the time (the length of the reservoir is 7.00 m). Therefore, the instantaneous flow fluctuated  
20 between A1 and A2 while the median flow was A2, which is consistent with previous dye  
21 visualizations (the second reattachment was sometimes missing). The high unsteadiness of the  
22 second reattachment length was also highlighted by Abbott & Kline (1962) about flow over  
23 backward facing steps.

24

1 The median reattachment length  $R_l$  measured for the experimental condition F14 was a little  
2 bit smaller than the value measured for F4 (1.04 – 1.10 m and 1.03 – 1.06 m instead of 1.16 –  
3 1.21 m and 1.15 – 1.18 m), which may be interpreted as an effect of the longitudinal  
4 confinement. Nevertheless, it can be said that the flow patterns A1 and A2 are quasi-identical  
5 in the upstream zone of the reservoir (same order of magnitude for the median position and  
6 the variability of the reattachment). They only significantly differ in the downstream zone of  
7 the reservoir.

8

9 It can be noticed that the median reattachment length of the “last” asymmetric flow before the  
10 transition to symmetric pattern was approximately equal to half the length of the reservoir  
11 (1.04 – 1.10 and 1.03 – 1.06 m compared to 2.20 m). This behavior was similar in the  
12 experiments of Kantoush (2008): the writer showed that when the breadth of the reservoir  
13 equaled 4.00 m, the transition occurred between the lengths 5.00 and 6.00 m; the mean  
14 reattachment length for a length of 6.00 m was  $\approx 2.65$  m (see Figure 4.16 of his thesis).

15

### 16 3.3 Spatial distribution of deposits

17 Figure 6 displays the preferential zones of deposition for the three stable flow patterns after  
18 10 minutes of sediment input (a clear pattern of deposition was observed after 4 – 5 minutes  
19 for all the sediment tests). Since the borders of the deposition zones slightly evolved over time  
20 (because of the unsteadiness of the flow), Figure 6 is only a sketch of the deposits at a given  
21 “time” (it is representative of a few seconds). The comparison between grey zones (tests a)  
22 and dotted lines (tests b) exhibits the same general shape of deposits.

23

24 From this figure, it can be concluded that the location of the deposits is clearly a function of  
25 the flow pattern. When the length was 1.80 m (flow pattern S0), the pattern of sediment

1 deposition was quasi-symmetric: deposition took place in each inlet corners. The size of the  
2 deposition regions was approximately a few centimeters to 0.3 m in width and 0.4 – 0.8 m in  
3 length. The shape of the downstream part of these zones was elongated and corresponded to  
4 deposits regularly eroded (wake zone).

5  
6 Like the flow pattern, the pattern of sediment deposition became asymmetric when increasing  
7 the length. When the reservoir was 2.20 m long (flow pattern A1), three regions of deposition  
8 took place on the bed: the two inlet corners and the core of the large circulation zone. Here,  
9 the jet was deflected on the right wall of the reservoir. Despite its relatively small area (about  
10 0.6 m long and 0.2 m wide), the zone of deposition in the core of the large circulation zone  
11 contained the largest amount of deposits. After 10 minutes of injection, the thickness of  
12 particles was about 20 mm (several layers of particles) while it was less than 5 mm in the  
13 others zones. In this zone, the deposits were regularly eroded due to the relative unsteadiness  
14 of the flow, but they remained captured in the circulation current and escaped only by  
15 intermittent “bursts”. In the right inlet corner, the region of deposition was about 0.4 m long  
16 and 0.2 – 0.3 m wide. As for the 1.80 m long reservoir, the downstream part of this region  
17 was regularly eroded because of the wake. The left inlet corner region consisted of very  
18 scattered deposits that were brought by the current from downstream to upstream. Regularly,  
19 the first and the third regions were connected by a narrow band of (intermittent) deposits (see  
20 dotted lines).

21  
22 When the length was 7.00 m (flow pattern A2), two main zones of deposition were identified.  
23 As for the flow pattern A1, a first region took place in the right inlet corner (the jet was  
24 deflected to the right). A second region of deposition took place mainly in the downstream  
25 zone of the reservoir. Its length was about 6.0 m and its width varied between a few

1 centimeters to approximately 0.4 – 0.6 m in its downstream part. Probably because of the  
2 unsteadiness of the flow in this zone (fluctuations of the longer reattachment length), the  
3 deposits were regularly eroded. This region of deposition was quasi-symmetric in the  
4 downstream part of the reservoir (where the flow was fully reattached). Contrarily to the  
5 experimental condition ST2, there was no region of deposition in the left inlet corner of the  
6 reservoir. This can be explained by the fact that the current from downstream to upstream that  
7 took place in this zone contained a small amount of particles (they settled or escaped before  
8 being brought back to the upstream zone of the reservoir).

9

### 10 3.4 Trap efficiency

11 As shown in Table 3, the efficiencies  $\eta_1$ ,  $\eta_2$  and  $\eta_3$  (corresponding to the three time periods)  
12 are scattered for a given length. Different reasons explain this behavior: the time needed by  
13 the particles to travel between the inlet and the outlet (one can see that 2 minutes were not  
14 sufficient to get “equilibrium” between the inflow and the outflow concentrations when the  
15 length was 7.00 m), the uncertainty of the measurements (10% – 15%), and the natural  
16 variability (although the equilibrium is reached, the difference between  $\eta_3$  obtained for ST1-a  
17 and ST1-b is greater than the uncertainty). The first reason leads to reject the  $\eta_1$  values as  
18 meaningful efficiencies for the longest reservoir whereas the  $\eta_2$  and  $\eta_3$  values and all the  
19 efficiencies obtained for the other lengths are considered hereafter.

20

21 The natural variability was probably due to the unsteadiness of the flow, the unsteadiness of  
22 the sediment input (discrete batches) and also the nature of sediment transport itself,  
23 especially because bed-load was predominant. Indeed, Böhm et al. (2004) showed that even  
24 under well-controlled experimental conditions and despite steady supply, solid discharge  
25 exhibits significant variations with time. One explanation given by the writers was the



1 collective entrainment of deposited particles, which was observed during our own  
2 experiments. This physical variability leads to define some ranges of efficiency rather than  
3 single values. Table 6 shows these approximate ranges as a function of the length of the  
4 reservoir. In this table, both uncertainty and variability are taken into account.

5

6 The influence of the length of the reservoir on the efficiency is illustrated in Figure 7. It can  
7 be seen that the decrease of the efficiency between 2.20 and 1.80 m is the same order of  
8 magnitude as the decrease between 7.00 and 2.20 m (about 20% – 25%). Therefore, the  
9 transition from an asymmetric flow to a symmetric flow is responsible for a break in the  
10 efficiency curve of the reservoir.

11

12 Even if the flow patterns observed for a length of 7.00 m and a length of 2.20 m were very  
13 similar, it is interesting to notice that the nature of deposition seemed to be different, probably  
14 because the particles were jailed in the circulation current for experiments ST2-a and ST2-b.  
15 Based on the sketches of the experimental deposits (Figure 6), the areas of deposition were  
16 estimated. Whereas the area of deposition was about 0.3 m<sup>2</sup> for a length of 2.20 m, it was  
17 around 1.9 m<sup>2</sup> (six times bigger) for a length of 7.00 m. In the same time, the efficiency only  
18 increases from the range 10% – 40% to 30% – 60%. One explanation is that the particles are  
19 concentrated in the center of the circulation zone for the flow pattern A1 (as “jailed” by the  
20 flow) whereas they are much dispersed for the flow pattern A2.

21

22 Although the number of points is too low and the values too scattered to propose a final  
23 relationship between the length of the reservoir and the efficiency, assumptions can be made  
24 and discussion is open. To do so, it can be added that the efficiency should tend towards zero  
25 when decreasing the length. But the efficiency does not necessarily tend towards 100% when

1 increasing the length (even if it is fully reattached, the flow may be able to carry a non-zero  
2 solid discharge because of the relatively small breadth of the flume).

3  
4 Exponential laws were often proposed as efficiency relationships (Sumer 1977 cited by Garde  
5 et al. 1990, Garde et al. 1990, Ranga Raju and Kothiyari 2004 for settling basins; Luyckx et al.  
6 1999 for the parameters of the efficiency relationship of a high side weir overflow). In this  
7 study, contrarily to the cited relationships, the constant  $L_0$  of such a law (see Equation 3) must  
8 be different from zero to accurately reproduce the abrupt change around the transition; this  
9 parameter is the length for which the efficiency becomes zero. The two other constants are  $\eta_0$ ,  
10 a maximum efficiency (for infinitely long reservoir) and  $\alpha$ , the inverse of a characteristic  
11 length (to represent the spread of the curve). This exponential relationship leads to negative  
12 values when the length is lower than  $L_0$ ; therefore, the expression is replaced by zero in this  
13 situation.

$$14 \quad \begin{aligned} \eta &= 0\% & \text{if } L \leq L_0 \\ \eta &= \eta_0 \left(1 - e^{-\alpha(L-L_0)}\right) & \text{if } L \geq L_0 \end{aligned} \quad (3)$$

15 The inconvenience of such a law is that the constant  $L_0$  has no meaning in relation to the flow  
16 pattern. A sigmoid law (as written in Equation 4) is more relevant to highlight the transition  
17 between symmetric and asymmetric flows in the efficiency relationship. Here, the constants  
18 of the law are a maximum efficiency,  $\eta_0$ , the inverse of a characteristic length,  $\alpha$ , and a critical  
19 length,  $L_0$ . This last parameter is the length for which the transition between asymmetry and  
20 symmetry occurs and is therefore between 1.80 and 2.20 m.

$$21 \quad \eta = \frac{\eta_0}{1 + e^{-\alpha(L-L_0)}} \quad (4)$$

22 The exponential law, the sigmoid law and two linear relationships (comparable slopes but  
23 different intercept points) are illustrated in Figure 7; all of them reproduce the general shape  
24 of the experimental data.

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The laws described above are some possibilities for taking into account the transition between symmetric and asymmetric flow patterns in a single efficiency relationship, but it is perhaps unrealistic to seek such a goal. In this case, the only way would be to use different regression laws depending of the flow pattern.

**4 Conclusions**

The objective of this work was to investigate the influence of the flow pattern on preferential regions of deposition and trap efficiency in rectangular shallow reservoirs. The great flexibility of the experimental set-up allowed easily changing the length of the reservoir and precisely determining the transition between symmetric and asymmetric flow patterns.

Four flow patterns were identified (from longer to shorter reservoirs): an asymmetric flow with two reattachment points (A2), an asymmetric flow with one reattachment point (A1), an unstable flow (A1/S0), and a symmetric flow without any reattachment point (S0). Using dye visualizations, the median value and the temporal variability of the reattachment lengths were precisely measured for the asymmetric flow patterns A1 and A2.

For each stable flow, sediment tests with plastic particles were carried out. The regions of deposition on the bed of the reservoir were mapped; they were clearly a function of the flow pattern. The transition between symmetric to asymmetric flow patterns was responsible for an abrupt increase in the efficiency curve. We discussed a number of regression laws to take it into account.

1 Further investigations are currently in progress in order to find forecasting criteria of the flow  
2 pattern varying the dimensionless length, the lateral expansion ratio, the vertical confinement  
3 and the Froude number. Based on this work, the data about trap efficiency available in  
4 literature should be reanalyzed in order to better define efficiency relationships.

5

## 6 **Acknowledgments**

7 We acknowledge Alain Dewart, Didier Lallemand, Maurice Salme and Dieudonné  
8 Stouvenakers for the building of the experimental set-up. We also acknowledge the  
9 University of Liège for the allocation of a postdoctoral fellowship to the first author.

10

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24

25

1 **Tables**

2

	Minimum value	Mean value	Maximum value
Height [mm]	2.30	2.55	2.85
Major axis [mm]	2.30	2.65	3.00
Minor axis [mm]	1.85	2.10	2.30
Density [kg/m <sup>3</sup> ]	-	1020 (given by BASF)	-
Fall velocity [mm/s]	20	25	30

3

Table 1. Features of the particles.

<i>Test ID</i>	$\Delta B$ [m]	$b$ [m]	$L$ [m]	$h$ [m]	$U$ [m/s]	<i>Flow pattern</i>	$R_1$ [m] (95% confidence interval)	$\mu_1$ [m]	$\sigma_1$ [m]	$R_2$ [m] (95% confidence interval)	$\mu_2$ [m]	$\sigma_2$ [m]
F4-a	0.350	0.285	7.000	0.201	0.28	A2	1.16 – 1.21	1.18	0.10	-	-	-
F4-b	0.350	0.285	7.000	0.200	0.29	A2	1.15 – 1.18	1.16	0.06	-	-	-
F4-c	0.350	0.285	7.000	0.203	0.27	A2	-	-	-	6.0 – 6.5	6.4	2.1
F14-a	0.350	0.285	2.200	0.205	0.27	A1	1.04 – 1.10	1.07	0.09	∅	∅	∅
F14-b	0.350	0.285	2.200	0.207	0.28	A1	1.03 – 1.06	1.05	0.06	∅	∅	∅
F15-a	0.350	0.285	2.000	0.204	0.27	A1/S0	-	-	-	∅	∅	∅
F16-a	0.350	0.285	1.800	0.206	0.27	S0	∅	∅	∅	∅	∅	∅
F16-b	0.350	0.285	1.800	0.204	0.27	S0	∅	∅	∅	∅	∅	∅

Table 2. Summary of flow test conditions and main results (“-” for “non-measured”, “∅” for “does not exist”).

<i>Test ID</i>	$\Delta B$ [m]	$b$ [m]	$L$ [m]	$h$ [m]	$U$ [m/s]	<i>Flow pattern</i>	$C_{in}$ [g/L]	$\eta_1$	$\eta_2$	$\eta_3$
ST1-a	0.350	0.285	7.000	0.199	0.28	A2	0.50	73%	49%	57%
ST1-b	0.350	0.285	7.000	0.196	0.28	A2	0.50	69%	50%	34%
ST2-a	0.350	0.285	2.200	0.200	0.28	A1	0.50	26%	18%	36%
ST2-b	0.350	0.285	2.200	0.197	0.29	A1	0.50	31%	28%	32%
ST3-a	0.350	0.285	1.800	0.204	0.27	S0	0.51	13%	2%	7%
ST3-b	0.350	0.285	1.800	0.207	0.27	S0	0.50	9%	1%	6%

Table 3. Summary of sediment test conditions and main results.



Dimensionless parameter	Value(s)
$\frac{L}{\Delta B}$	5.1, 5.7, 6.3 and 20.0
$\frac{\Delta B}{b}$	1.23
$\frac{\Delta B}{h}$	between 1.69 and 1.78
$\frac{4\rho Uh}{\mu}$	between 210,000 and 228,000
$\frac{U}{\sqrt{gh}}$	between 0.19 and 0.21
$\frac{c_f \Delta B}{2h}$	$\approx 0.003$

Table 4. Dimensionless flow parameters.

Dimensionless parameter	Value
$\frac{\rho u_*^2}{(\rho_s - \rho)gd}$	$\approx 0.3$
$\frac{\rho u_* d}{\mu}$	$\approx 30$
$\frac{w}{u_*}$	$\approx 2$
$\frac{q_s}{\sqrt{\left(\frac{\rho_s}{\rho} - 1\right)gd^3}}$	$\approx 0.5$

Table 5. Dimensionless sediment parameters.

Length [m]	Trap efficiency
1.80	0% – 20%
2.20	10% – 40%
7.00	30% – 60%

Table 6. Ranges of trap efficiencies varying the length of the reservoir.

## List of figures

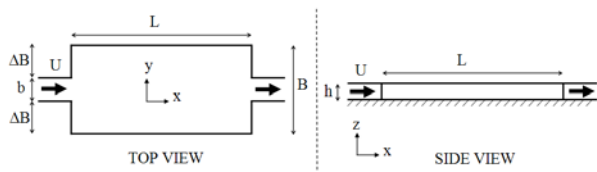


Fig. 1. Schemes of a rectangular shallow reservoir.

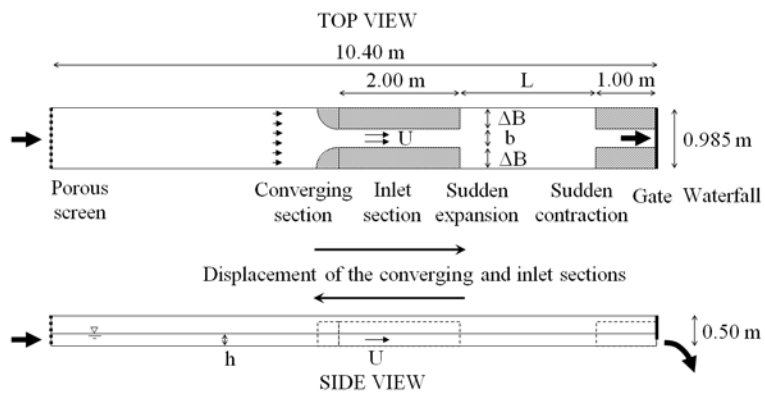


Fig. 2. Sketch of the experimental set-up.

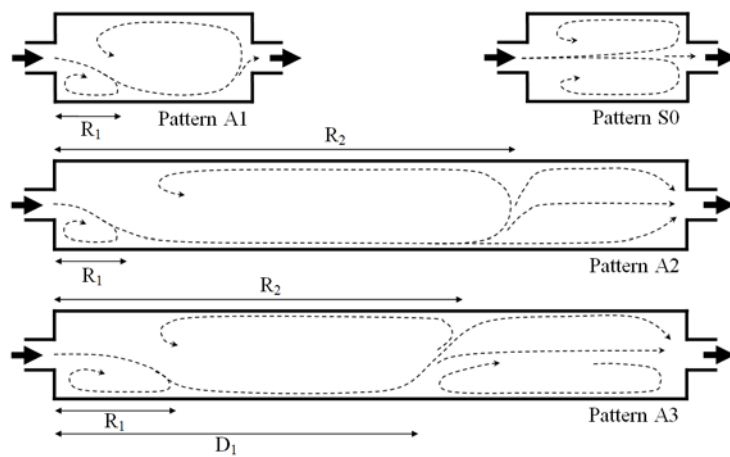


Fig. 3. Schemes of the three stable flow patterns (not to scale).

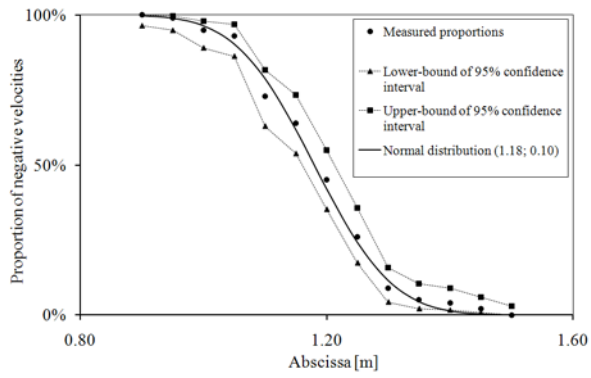


Fig. 4. First reattachment of test F4-a.

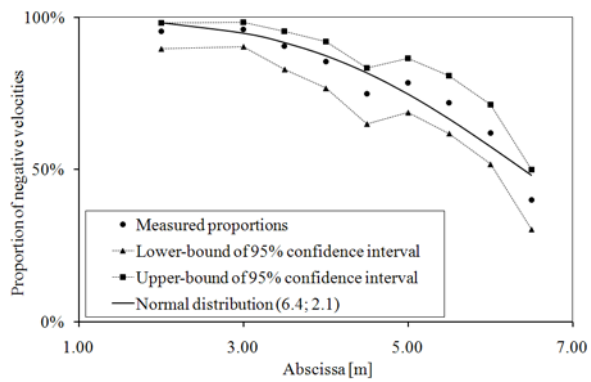


Fig. 5. Second reattachment of test F4-c (the normal distribution is truncated).

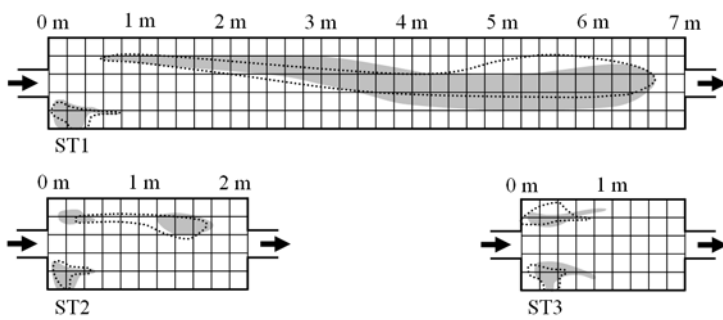


Fig. 6. Experimental deposits on the bed of the reservoir (grey zones correspond to tests a; dotted lines, to tests b).

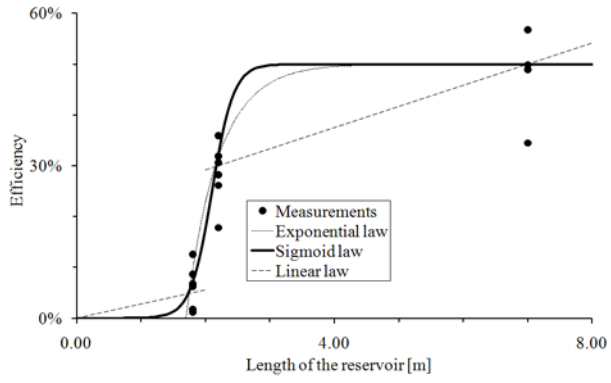


Fig. 7. Efficiency varying the length of the reservoir (parameters of the exponential law:

$\eta_0 = 50\%$ ,  $\alpha = 2 \text{ m}^{-1}$ ,  $L_0 = 1.7 \text{ m}$ ; sigmoid law:  $\eta_0 = 50\%$ ,  $\alpha = 6 \text{ m}^{-1}$ ,  $L_0 = 2.1 \text{ m}$ ).