REACTIVE TRANSPORT MODELLING OF AMMONIUM: 1D CONCEPTUAL MODELLING AND COMPARISON OF REACTIVE TRANSPORT CODES

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Abstract Contamination of ammonium, as main inorganic contaminant, resulted from disposal of ammoniacal liquor at a former coal carbonisation plant at Mansfield, UK. Previous research for evaluating natural attenuation revealed strong retardation of ammonium in the aquifer due to ion exchange in the aquifer. In a first modelling approach a conceptual 1D-model example is considered where an ammonium contaminated aquifer is flushed by pristine background groundwater. Two multicomponent reactive transport models, PHT3D (Prommer et al., 2001) and PHREEQC-2 (Parkhurst and Appelo, 1999) were used for the model example and a comparison between the codes was made.

INTRODUCTION

Disposal of ammoniacal liquor coming from a former coal carbonisation plant at Mansfield, UK, gave rise to contamination of the groundwater by both organic and inorganic contaminants (Broholm et al., 1998; Jones et al., 1998). The ammoniacal liquor was dumped in small lagoons where it could infiltrate into the groundwater. High levels of dissolved ammonium (up to ~ 350 mg/l NH4-N) in the groundwater revealed ammonium as the main inorganic contaminant present in the aquifer. When entering the aquifer ammonium is retarded by ion exchange in the aquifer, where ammonium exchanges onto the aquifer sediment releasing the native cations of the sediment. After contamination has stopped leaking into the aquifer, the ammonium will be exchanged off the aquifer sediment by the flushing of the aquifer with pristine background groundwater under natural groundwater gradient conditions.

Because ammonium is competing for ion exchange with several other cations simultaneously, a multi-component reactive transport model is required that can handle ion exchange reactions among multiple cations. The modelling example, presented in this paper, serves as a first step for future 2D/3D simulations.

MULTICOMPONENT REACTIVE TRANSPORT MODEL

Recently (Prommer et al., 2001) developed a MODFLOW/MT3DMS-based reactive multicomponent transport model. The model couples via a sequential approach, the three-dimensional transport simulator MT3DMS (Zheng and Wang, 1999) with the geochemical model PHREEQC-2 (Parkhurst and Appelo, 1999). The model uses total aqueous component concentration (Engesgaard and Kipp, 1992; Yeh and Tripathi, 1989) as primary dependent variable. The reactive transport equation is then given as (Prommer et al., 2001):

for mobile components: $\frac{\partial C}{\partial t} = \frac{\partial}{\partial x_i} \left(D_{ij} \frac{\partial C}{\partial x_j} \right) - \frac{\partial}{\partial x_i} (v_i C) + r_{reac}$

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and for immobile components: $\frac{\partial C}{\partial t} = r_{reac}$

where v_i is the pore water velocity in direction x_i , D_{ij} is the hydrodynamic dispersion coefficient, r_{reac} is a source/sink rate due to the chemical reaction and *C* is the total aqueous component concentration, defined as: $C = c + \sum_{i=1,n_s} \gamma_i^s s_i$ where *c* is the molar concentration of

the (uncomplexed) aqueous component, n_s is the number of species in dissolved form that have complexed with the aqueous component, γ_i^s is the stoichiometric coefficient of the aqueous component in the *i*th complexed species and s_i is the molar concentration of the *i*th complexed species.

Since PHREEQC-2 can handle reactive transport calculations, yet only in 1D, as well, the code was used to compare results of the modelling example with the PHT3D code. Both codes use the same geochemical reaction module but a different scheme to couple the hydrodynamic transport and geochemical reactions (see figure 1).



Figure 1: Coupling scheme between hydrodynamic transport and geochemical reactions. C^k and C^{k+1} are the total aqueous components concentrations at the old and new time levels, respectively, and R_c is the source/sink term linking the transport module with the reaction modules.

1D-MODEL EXAMPLE

The model example (figure 2) consists of a 1D flowtube that represents the ammonium contaminated aquifer with an injection well at the influent boundary to simulate the continuously flushing by pristine background groundwater after the contamination has stopped. The concentration at the end of the flowtube serves as observation point. Table 1 and 2 show the physical parameters and the hydrogeochemical initial and boundary conditions for the model example. For the reactive transport calculations the thermodynamic data from the PHREEQC-2 code are used (Parkhurst and Appelo, 1999).

Simulation results of the modelling example show that large numbers of pore volumes (i.e., a nondimensional time parameter where elapsed time is divided by the hydrodynamic residence time (Brusseau, 1994)) are needed to flush the ammonium (figure 3) off the aquifer sediment at the observation point at the end of the flowtube. When the exchange front has passed the entire flow tube the concentrations of the more selective cations in respect with ammonium (Ca and Mg) increase to reach the concentration levels of the background water. Figure 3 shows also the effect of flushing the aquifer on the pH. During the first twelve pore volumes ammonium into the groundwater causes a drop of pH due to the reaction: $NH_4^+ \square NH_3 + H^+$. When the exchange front has passed the observation point after twelve pore volumes, the pH increases again and is in equilibrium with the incoming pristine background water.



Figure 2: Conceptual 1D-model example

Table	1:

Physical parameters used for example problem. Data from (Jones, 2001).

Parameter	Unit	
Length of flowtube	m	30
Spatial discretisation interval	m	1
Final solution time	days	5000
Longitudinal dispersivity	m	0.5
Hydraulic conductivity	m day ⁻¹	2.5
Effective porosity	-	0.2
Prescribed flux influent boundary ^a	m ³ day ⁻¹	0.02375
Prescribed head effluent boundary ^a	m	1

^a Calculated based on the observed hydraulic gradient of 0.0095 and the hydraulic conductivity.

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Table 2

Initial and boundary conditions: chemical concentrations (concentrations in moles per liter, unless otherwise specified) and hydrogeochemical parameters. Data from (Jones, 2001).

Parameter	Contaminated groundwater (flowtube)	Background groundwater
		(influent boundary)
CEC	$0.122 (eq/l)^{c}$	
pH	7.9	8.3
O ₂	2.5 x 10 ⁻⁴	bdl
Na	8.6×10^{-4}	$1.3 \ge 10^{-3}$
Κ	1.3×10^{-4}	1.3 x 10 ⁻⁴
NH4-N	6.9×10^{-3}	bdl
Mg	$1.4 \ge 10^{-3}$	$5.0 \ge 10^{-5}$
Ca	1.8×10^{-3}	1.5 x 10 ⁻⁴
Cl^{a}	2.5×10^{-3}	3.2×10^{-3}
SO_4	1.6×10^{-3}	9.9 x 10 ⁻⁴
NO ₃	ns	8.9 x 10 ⁻⁴
$C(4)^{b}$	2.8×10^{-3}	2.9 x 10 ⁻³

^a Adjusted to achieve charge balance ^b Calculated based on alkalinity measures.

ns = not sampled

bdl = below detection limit



Figure 3: Total aqueous component concentration (moles per liter except for pH) versus pore volumes calculated at the observation point at the end of the flow tube.

COMPARISON OF SIMULATION RESULTS

Figure 4 shows the comparison of simulation results from the two codes. For transport of a non-reactive solute, as shown for Cl, both codes lead to the same results. For transport of a reactive solute, as shown for NH4-N, there exists a discrepancy for a reaction time step, Rt, of 10 days in the PHT3D code. Rt defines the time step at which the code switches to the geochemical reaction calculation whereas the transport time step (advection-dispersion) is calculated internally by the MT3DMS code to meet the various stability criteria [Zheng, 1999 #251] (see alsofigure 1). A discrepancy arises when, as in the case with Rt = 10 days, several

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transport time steps for advection-dispersion transport are performed before the program switches to the geochemical reaction calculation. This results in a loss in accuracy of the modeling of the exchange front in our example. This is confirmed by (Engesgaard and Traberg, 1996) who stated also that the accuracy of a sequential coupling approach is dependent on the time step. PHREEQC-2 simulation results don't show this behavior because only one single time step is used for the reactive transport calculation and the geochemical reactions are calculated after both the advective and dispersive steps (see figure 1).



Figure 4: Comparison between the simulation results of PHT3D and PHREEQC-2 showing the effect of decreasing Rt upon the accuracy of the reactive transport modeling (concentrations are in moles per liter).

SUMMARY AND CONCLUSIONS

A 1D model example for multicomponent reactive transport of ammonium was set up for future 2D/3D simulations. The example showed strong retardation of ammonium due to ion exchange on the aquifer sediment and the consequent influence on pH.

Furthermore simulation results obtained by two reactive transport codes were compared in order to asses their accuracy. It is shown that for the PHT3D code the reaction time step Rt should approach the time step calculated internally by the MT3DMS module for advective dispersive transport.

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