

#### CURRENT STATUS OF CCU TECHNOLOGIES & ROLE OF HYDROGEN

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- ➤The global challenges
- ➢ Possible solutions
- >CO<sub>2</sub> conversion pathways
  - Electrochemical
  - Biological
- >CO<sub>2</sub> to Fuel (Thermochemical)
- ➤Technology comparison
- ➢Global CCUS status

### Carbon neutrality by 2050: the most urgent mission in the world



https://www.motive-power.com/npuc-resource/carbon-neutral-goals-by-country/

# The energy transition is on-going but it won't be easy... revolution



2 objectives in contradiction:

- Limit GHG emissions
- Meet the worldwide increasing energy demand!



www.carbontracker.org



#### Meeting the increasing demand is already a challenge in itself!





BP Statistical Review of World Energy 2020.





#### Budget by 2050 for having 80% chances to stay below 2 °C



### Reaching climate neutrality won't be easy...

- Belgium CO<sub>2</sub> emissions ~ 100 Mt/a
- This corresponds to ~ 8.6 t/hab.a
  - Everyday, each of us puts 24 kg CO<sub>2</sub> into the environment !!
- Source: Our world in data

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- Related reference: https://doi.org/10.5194/essd-12-3269-2020
- https://ourworldindata.org/co2/country/belgium
- https://ourworldindata.org/co2-emissions





### **Possible answers: Trias Energetica**



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Lysen E., The Trias Energica, Eurosun Conference, Freiburg, 1996



# CO<sub>2</sub> capture

- It's a question of fluid separation!
  - Sources usually contain  $CO_2$ ,  $N_2$ ,  $H_2O$ ,  $H_2$ ,  $CH_4$ ,  $O_2$  ...
  - □ CO<sub>2</sub> concentration varies between 0.04% and almost 100%
  - Mature (exist for >50 years) & flexible, but costly!





### And then, what with the CO<sub>2</sub>: waste or feedstock?

- CCS (excluding EOR) is a cost only technology!
  - Requires infrastructure off-site (pipelines, ships, storage sites determined by geology)
  - Basically permanent landfilling
    Any better idea?
- We'll need CO<sub>2</sub> as a source for carbon!
  - Our society is based on carbon
  - If we ban fossils, we can get carbon only from
    - Biomass



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# Main CO<sub>2</sub> re-use pathways

- Direct use, no transformation
- **Biological transformation**
- Chemical transformation
  - To lower energy state
    - Carbonatation
  - To higher energy state

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=> At large scale, need to make sure that energy comes from renewables!

Frenzel et al, 2014. Doi:10.3390/polym6020327







LEVELIZED COST OF SOLAR AND WIND DERIVED POWER VERSUS DEPLOYED CAPACITY





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Grim et al., 2020. Transforming the carbon economy: challenges and opportunities in the convergence of lowcost electricity and reductive CO<sub>2</sub> utilization. Energy & Environmental Science, 13(2), pp.472-494.



#### **REUSING CARBON DIOXIDE**

Companies are turning the greenhouse gas into many products. Some products lock  $CO_2$  away for decades, but others are short-lived solutions, so the gas quickly ends up in the atmosphere.



chemicals often requires hydrogen (H2) from industrial waste gases or from electrolysis of water.



Peplow, M., 2022. Nature, 603(7903), pp.780-783.

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#### REDUCTIVE AND NON-REDUCTIVE PATHWAYS FOR CO<sub>2</sub> CONVERSION



23/05/2022 ©VITO – Not for distribution Grim et al., 2020. Transforming the carbon economy: challenges and opportunities in the convergence of low-cost electricity and reductive CO<sub>2</sub> utilization. Energy & Environmental Science, 13(2), pp.472-494.



#### VALUE-DRIVEN CO<sub>2</sub> CONVERSION







- **O** Formic acid: small market, but H<sub>2</sub> carrier and 'liquid syngas'
- **O** Oxalic acid: small market, but high value/volume derivatives
- **Fuels:** legislation, incentives / large market

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#### POWER2X DEPLOYMENT ROADMAP



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#### **Electrochemical CO<sub>2</sub> reduction reaction**



# Copper-based catalysts, high selectivity for valuable fuels and chemicals, ethylene and alcohols



#### The binding energy of Cu to the intermediate is neither strong nor weak.

Wenxing Chen\* et al. ACS Energy Lett. 2021, 6, 3992–4022

# What it takes for industrialization?



Current density of 1.3 A cm<sup>-2</sup> But FE of 45%, Cell voltage ~ 4.5 V

World record of FE FE of 87%, Current density of ~32 mA cm<sup>-2</sup>, Cell voltage of 2.02 V

García de Arquer et al., Science 367, 661–666 (2020)

Andrew A. Gewirth\* et al. Nature Catalysis | VOL 4 | JANUARY 2021 | 20-27



#### **CURRENT DENSITY VS STABILITY**

# "Yeah, your catalyst might have high current but how is its long term stability?"



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# **Degradation Mechanisms**





### **SnO<sub>2</sub> Reduction**



Van Dale et al., 2021. Sn-Based Electrocatalyst Stability. ACS Energy Letters, 6, 4317-4327.









### From lab scale: 1 cm<sup>2</sup>, 4 cm<sup>2</sup>, 10 cm<sup>2</sup>



### To Pilot scale: 20 cm<sup>2</sup> up to 600 cm<sup>2</sup>



# Booster: 20V 20A

### **High pressure reactor: 20**

#### CO2 ELECTROLYZERS

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- H2020 LOTER.2M and ETF PROCURA projects TRL 6 5 kW pilot in progress today
- ECO2FUEL Green Deal project: 50 kW electrolyzer in 2023
- Towards renewable fuels ranges (e.g. methanol, C<sub>1</sub>-C<sub>4</sub>...), also gasses: H<sub>2</sub>, CO, ...
  - 50 kW (5000 h/y): 20 t methanol/y (100 % select., 50 % η<sup>energy</sup>)





### **vito** DEMONSTRATOR CONSTRUCTION



#### BES FOR BIOLOGICAL AND ENZYMATIC CONVERSIONS



Katuri et al. 2018, Adv. Mat. 30 (1707072), 1-18

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🧡 vit	0	BIOCHEMIC	CALS A	ND BIOFUELS (	OBTAINED F	ROM CO2	IN MES	
Product	Highest production rate (g/(L·d))	Main carbon sources	рН	т (°С)	Potentiostatic control (V vs. SHE)	Galvanostatic control (mA/cm²)	Cathode	Reference
Acetate	77	NaHCO <sub>3</sub>	5.2	35	-1.10	n.a	3D-reticulated vitreous carbon	Jourdin et al. (2016)
Butyrate	5.70	CO <sub>2</sub> :N <sub>2</sub> 30:70 %	5.8	32	-0.85	-5 to -12	Carbon felt	Jourdin et al. (2019)
Caproate	2.41	Ethanol, CO <sub>2</sub> and NaHCO <sub>3</sub>	7.0	30	n.a.	-1.0	Carbon felt	Jiang et al. (2020)
Butanol	0.06	CO2	8.0	29	-0.80	n.a.	Gas diffusion electrode	Srikanth et al. (2018b)
Ethanol	0.18	CO <sub>2</sub>	8.0	29	-0.80	n.a.	Gas diffusion electrode	Srikanth et al. (2018b)
Ethanol	0.05	CO <sub>2</sub>	5.4	25	-0.80	n.a.	Granular graphite	Blasco-Gómez et al. (2019)
Isopropanol	0.06	CO <sub>2</sub> :N <sub>2</sub> 10:90%	5.0	30	n.a.	-0.5	Carbon felt	Arends et al. (2017)
Methane	12.5 <sup>b</sup>	NaHCO <sub>3</sub>	7	30	n.a.	-1.0 to -3.5	Graphite felt	Geppert et al. (2019)
23/05/2022 @V/ITO = Not for dis	tribution	Dessi et al., 2021 chemicals from C	I. Microbi CO2 emis	al electrosynthesis: To sions. Biotechnology A	owards sustainab Advances, 46, p.1	le biorefineries 1 107675.	or production c	of green





#### Wide product distribution mix

De Luna et al., 2019. What would it take for renewably powered electrosynthesis to displace petrochemical processes? Science, 364(6438).

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# **Thermochemical CO<sub>2</sub> conversion: power-to-fuel**

Idea: store renewable energy in the C-C and C-H bonds



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### **Decisive advantage: a fantastic volume energy density!**



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### **Energy storage**

# Quick calculations

- How many cars tanking at the same time are needed to develop a power of 3 GW<sub>th</sub> (i.e. a nuclear plant)?
  - 1 L/s gasoline transfer
  - Gasoline ~ 35 MJ/L
  - => 1 car = 35 MW<sub>th</sub>
  - 3 GW<sub>th</sub> ~ 85 cars





# CO<sub>2</sub> to fuels

#### Methane

- $\bigcirc CO_2 + 4 H_2 \rightarrow CH_4 + 2 H_2O$
- Sabatier reaction,  $\Delta H^\circ = -165 \text{ kJ/mol}$
- Commercial uses:
  - Great Plain synfuel plant
  - Methanation in ammonia synthesis
  - Producing fuel on Mars
    - $CO_2 + 4 H_2 \rightarrow CH_4 + 2 H_2O$
    - CH<sub>4</sub> used as fuel, H<sub>2</sub>O electrolyzed for (re)generating H<sub>2</sub> and O<sub>2</sub>
  - □ Jupiter1000 in Marseille (Fos-sur-mer), Audi e-gas plant (54% efficiency)...
- CH<sub>4</sub> is a greenhouse gas!
  - Lock-in effect of infrastructures...



https://www.sciencedirect.com/science/article/pii/S13640321173 11346#s0110 https://en.wikipedia.org/wiki/Sabatier\_reaction





# CO<sub>2</sub> to fuels

#### Methanol

#### □ CO + 2 H<sub>2</sub> → CH<sub>3</sub>OH ( $\Delta$ H<sub>300K</sub> = - 90.8 kJ/mol) □ CO<sub>2</sub> + 3 H<sub>2</sub> → CH<sub>3</sub>OH + H<sub>2</sub>O ( $\Delta$ H<sub>300K</sub> = - 49.2 kJ/mol)



#### Haldor Topsoe, > 10 000 t/d





### **Power to Liquid : methanolisation**



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### Recent announcements ...



Became North-C-Hydrogen in 2022 due to non-selection of the project for European funding



8000 ton/y, operation start: due in 2023 https://powertomethanolantwerp.com/





# CO<sub>2</sub> to fuels

- DME ( $CH_3$ -O- $CH_3$ )
  - □ 2 CH<sub>3</sub>OH → CH<sub>3</sub>-O-CH<sub>3</sub> + H<sub>2</sub>O ( $\Delta$ H° = 23.4 kJ/mol)
  - Similar to diesel fuel, but stored under pressure
  - Can be made from methanol, or directly CO<sub>2</sub>



# $CO_2$ to fuels

#### Syngas

- Reverse water-gas shift
  - $CO_2 + H_2 \rightarrow CO + H_2O$  $\Delta H^\circ = + 40.9 \text{ kJ/mol}$
- Dry Reforming
  - $CO_2 + CH_4 \rightarrow 2 CO + 2 H_2$  $\Delta H^\circ = + 247.3 \text{ kJ/mol}$
- Co-electrolysis:

**ENGINEERING** 

- $H_2O \rightarrow H_2 + 0.5 O_2$  E°= 0.41 V vs.NHE
- CO<sub>2</sub> -> CO + 0.5 O<sub>2</sub> E°= 0.53 V vs.NHE



NETL, WGSR



Wikipedia, SOEC



# CO<sub>2</sub> to fuels: gas-to-liquids (Fischer-Tropsch)

Gasoline:

■ 8 CO + 17 H<sub>2</sub> 
$$\rightarrow$$
 C<sub>8</sub>H<sub>18</sub> + 8 H<sub>2</sub>O  
 $\Delta$  H<sub>298K</sub> = -1276 kJ/mol

Jet fuel

■ 11 CO + 23 
$$H_2 \rightarrow C_{11}H_{24}$$
 + 11  $H_2O$   
 $\Delta H_{298K}$  = -1721 kJ/mol

Global reaction from CO n CO + (2n+1)  $H_2 \rightarrow C_n H_{2n+2} + n H_2O$ 

Global reaction from  $CO_2$ n  $CO_2$  + (3n+1)  $H_2 \rightarrow C_nH_{2n+2}$  + 2n  $H_2O$ 

```
Difference is the RWGS: CO_2 + H_2 \leftrightarrow CO + H_2O
```



Rasmussen, 2019. Implementation of Fischer-Tropsch Jet Fuel Production in the Danish Energy System



# CO<sub>2</sub> to fuels

Fischer-Tropsch fuels

- Similar to gasoline, complex mixture
- □ Sunfire: 58 m³/a, Efficiency ~70%



Figure 5

Sunfire PtL demonstration plant (top) using high-temperature electrolysis (middle) for the production of Fischer-Tropsch crude (bottom)



Sources: top: sunfire GmbH Dresden/CleantechMedia; sunfire GmbH Dresden/renedeutscher.de







#### **Recent announcement**

Carbon neutral kerosene

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ENGINEERING

# BELGIUM'S NEXT CENTURY SAF / E-FUEL ECOSYSTEM

Neutral Kero Lime Presentation to Energia

Autoworld, Octobre 28<sup>th</sup>, 2021

**►** ILÈGE

https://trends.levif.be/economie/entreprises/dukerosene-wallon-neutre-en-carbone/article-normal-1466097.html?cookie check=1637791560



#### **Recent announcement**

Capture de CO<sub>2</sub> + électrolyse + synthèse Fischer-Tropsch



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https://trends.levif.be/economie/entreprises/dukerosene-wallon-neutre-en-carbone/article-normal-1466097.html?cookie\_check=1637791560





#### **DREAM PRODUCTION**







#### https://www.plasteurope.com/news/detail.asp?id=234342

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23/05/2022 ©VITO – Not for distribution https://www.agro-chemistry.com/news/photanol-to-build-demo-plant-on-akzonobel-site-delfzijl/



#### **GLOBAL PIPELINE OF COMMERCIAL CCUS FACILITIES OPERATING & IN DEVELOPMENT**



IEA, Global pipeline of commercial CCUS facilities operating and in development, 2010-2021, IEA, Paris <u>https://www.iea.org/data-and-statistics/charts/global-pipeline-of-commercial-ccus-facilities-operating-and-in-development-2010-2021</u>

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#### TOP TECHNICAL BARRIERS AND AREAS FOR FUTURE RESEARCH ACROSS CO2R PATHWAYS



		DIRECT			INDIRECT		
	Elec	trochemical	Bioelectrochemical (MES)	Plasma	Bioelectrochemical (Fermentation)	Thermochemical	
	C1 (TRL: 4-6)	C <sub>2+</sub> (TRL: 1-3)	TRL: 1–3	(TRL: 1-3)	TRL: 4-7	TRL: 5-8	
Major Technical Challenges	<ul> <li>Scale up reactor / supporting systems</li> <li>Increase long-term system stability</li> </ul>	<ul> <li>Improve energy efficiency; reduce cell overpotential</li> <li>Increase selectivity to individual C<sub>1+</sub> products</li> <li>Increase single-pass CO<sub>2</sub> conversion</li> </ul>	Develop fundamental understanding of electron transfer mechanism(s)     Raise CQ, reduction rates     Increase product titers and cell toxicity limits     Increase CQ, solubility / current density	<ul> <li>Decouple energy efficiency / conversion correlation</li> <li>Raise yield to C<sub>2*</sub> products</li> <li>Develop commercially viable reactor design</li> </ul>	<ul> <li>Increase solubility of gaseous reactants</li> <li>Reduce separation costs</li> <li>Increase product titers and cell toxicity limits</li> </ul>	<ul> <li>Process intensification and scale-down</li> <li>Develop multi-functional water and CO<sub>2</sub> tolerant catalysts</li> <li>Improve product selectivity</li> </ul>	
Research Needs	Transition to gas-phas     Standardize testing pr     Develop accelerated d     Test possible anodic ch     Optimize reaction contransport)     Develop of new cataly	e, membrane electrode assemblies otocols egradation testing methods emistries to replace OER ditions (electrolyte, pH, mass tic materials and membranes	Expanded testing of mixed and pure cultures     Develop bio-compatible gas diffusion electrodes     Genetic engineering	Develop specialized packed-bed catalysts for plasma conditions     Electronics development     Scalable reactor design	<ul> <li>Raise product titers</li> <li>Improve reactant delivery / mixing</li> <li>Develop low-cost <i>in-situ</i> separations</li> </ul>	Rapid screening of active materials     Improve catalyst performance     through promoter additives     Intelligent systems integration and     reactor design	
Advantages	Commercially deploye     Tunable distribution of     100% theoretical conv     High theoretical energ     Access to high-value, h products	d for C, species f over 20+ products ersion of CO <sub>2</sub> y conversion efficiency high-volume intermediates &	<ul> <li>Can form C-C bonds at ~100% selectivity</li> <li>Specialized chemistry accessible through genetic modifications</li> <li>~98.6 % theoretical conversion of CO<sub>2</sub></li> <li>High theoretical energy conversion efficiency</li> </ul>	Adaptable to transient usage; quick to reach steady-state     Feedstock flexible     100% theoretical conversion of CO <sub>2</sub>	<ul> <li>Can form C-C bonds at ~100% selectivity</li> <li>High TRL, deployed commercially</li> <li>~98.6 % theoretical conversion of CO<sub>2</sub></li> </ul>	<ul> <li>Direct access to high volume fuels and chemicals markets</li> <li>Highest TRL; deployed commercially at large-scale</li> <li>Long history of R&amp;D investments; existing infrastructure</li> </ul>	
Limitations	<ul> <li>Low selectivity to C<sub>2+</sub> p</li> <li>Reported products lim</li> <li>Low TRL to C<sub>2+</sub> product</li> <li>Rapid deactivation and stability</li> </ul>	products ited in carbon number $\leq 4$ is d limited testing on long-term	<ul> <li>Low productivity</li> <li>Limited number of direct C<sub>1</sub>-C<sub>3</sub> products</li> <li>Poorly understood reaction mechanisms</li> </ul>	Low TRL     High power demand     Low selectivity to C <sub>2+</sub> products	<ul> <li>Poor mass transfer</li> <li>Limited number of direct C<sub>1</sub>-C<sub>3</sub> products</li> <li>Large system footprint</li> <li>Lower theoretical energy conversion efficiency</li> </ul>	<ul> <li>Challenged economics at small-scale</li> <li>Limitations in CO<sub>2</sub> equilibrium conversion</li> <li>Lower theoretical energy conversion efficiency</li> </ul>	

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#### PROPOSED TIMELINE OF CO<sub>2</sub> UTILIZATION METHODS

5 to 10 years		10 te	o 50 years	70+ years	
Electrocatalysis	Photocatalysis	Biohybrid	Nanoporous Confinement	Chain Insertion	Molecular Machines
<ul> <li>Flexible electricity source</li> <li>Closest to scale and commercial application</li> <li>Dependent on the cost of electricity</li> </ul>	<ul> <li>Direct solar to fuel conversion</li> <li>Portable</li> <li>No CO<sub>2</sub> solubility issues</li> <li>Efficiencies and activities are still low</li> </ul>	<ul> <li>Coupling of enzymes to inorganic water splitting</li> <li>Microbial synthesis</li> <li>Complicated molecule synthesis</li> <li>Stability is still an issue</li> </ul>	<ul> <li>Catalysis of hydrocarbons achieved in zeolites and MOFs</li> <li>High temperatures and pressures required</li> </ul>	<ul> <li>Metal catalysts for polymerization through chain insertion.</li> <li>Currently highly adopted by industry</li> <li>Have yet to be demonstrated with CO<sub>2</sub></li> </ul>	<ul> <li>Artificial enzymes with dynamic components</li> <li>Potential for tandem catalysis with high selectivity</li> <li>Has yet to be demonstrated</li> </ul>

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Bushuyev et al., 2018. What should we make with  $CO_2$  and how can we make it? Joule, 2(5), pp.825-832.



- Multiple valorization routes are possible via CCU (several pathways) with different challenges associated to each pathways. Power to X route is a promising one allowing integration with renewable energy.
- > The multiple pathways are at different level of TRL.
- > There is a cost associated to each pathway and it varies according to different variables.
- Thermochemical and bioelectrochemical routes offer the most technically feasible near-term opportunities for CCU, representing immediately deployable pathways to high-value and relatively high-volume products 

  face inherent challenges with respect to lower equilibrium conversion (thermochemical) and a limited C1–C3 product distribution (biochemical), potentially hindering their long-term viability
- Direct electrochemical pathway show long-term promise and can theoretically overcome these limitations, yet currently face numerous technical barriers preventing near-term market adoption

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### **State of technologies CCUS**

#### Cost of CO<sub>2</sub> capture and re-use

- CCU routes are more expensive than fossil under both near- (2020s) and long-term (2050s) assumptions. In the near-term, CCU commodities are at least twice the cost of their fossil counterparts. In the long-term, cost premiums can decrease significantly due to reductions in the cost of green hydrogen and CO<sub>2</sub> capture.
- Economic competitiveness of CCU routes is reliant on a 'cost of emission', estimated in the long-term between USD 120-225/tCO2.

#### Structural impact on CO<sub>2</sub> prices due to European Green Deal



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IEAGHG, 2021-03 CO2 Utilisation Reality Check: Hydrogenation Pathways. <u>https://www.ieaghg.org/publications/technical-reports/reports-list/9-technical-reports/1052-2021-03-co2-utilisation-reality-check-hydrogenation-pathways</u> <u>https://ember-climate.org/data/carbon-price-viewer/</u>



### State of technologies CCUS

- Avoiding > 1 GtCO<sub>2</sub> requires very high levels of market penetration
  - For methanol: if methanol captures the entirety of the current market and then expands into the heavy-duty trucks market plus the plastics markets
  - For middle distillate hydrocarbons: only if they capture the entirety of today's aviation fuels and heavy-duty trucks market.
  - For formic acid: even if the CCU product were to penetrate the entire formic acid market, the abatement currently achievable is limited to approximately 2 MtCO<sub>2</sub>.
- CCU pathways must be designed carefully to ensure lower life cycle emissions than the alternative pathways.





# ULiège: FRITCO<sub>2</sub>T platform

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### Perspective

- We live in a carbon-based society, with very good reasons for that !
- A CO<sub>2</sub> neutral future is in sight with passionating (and huge) challenges for engineers!
- This will require a large penetration of hydrogen as an (intermediate) energy carrier





Martens et al., (2017) The Chemical Route to a  $CO_2$ -neutral world, *ChemSusChem* Saeys (2015), De chemische weg naar een  $CO_2$ -neutrale wereld, Standpunt KVAB





# Thank you for your attention





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**Interreg** 2 Seas Mers Zeeën European Regional Development Fund











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