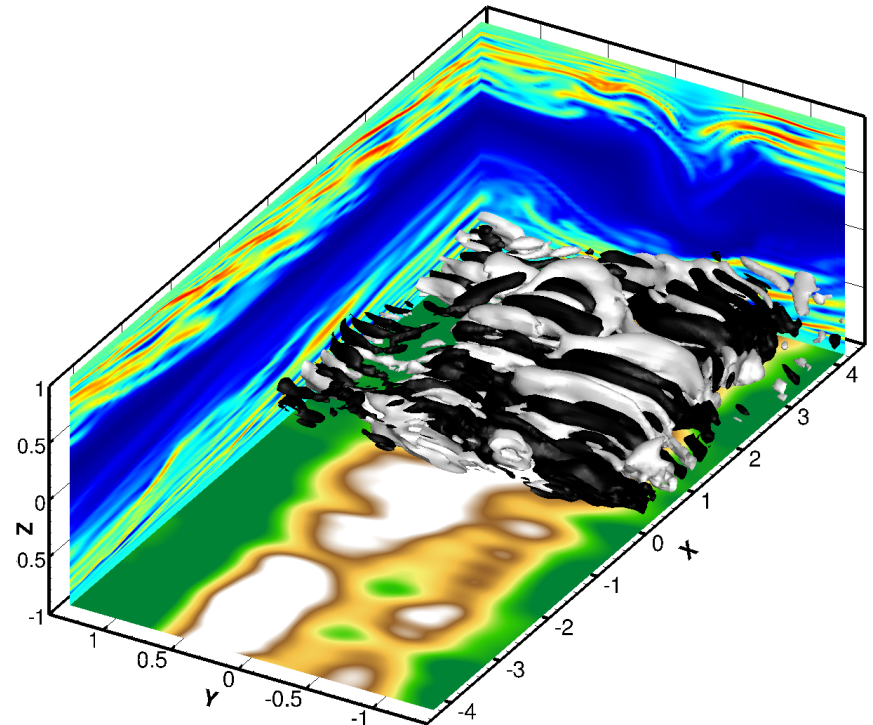


Role of Elasto-Inertial Turbulence on channel flow drag

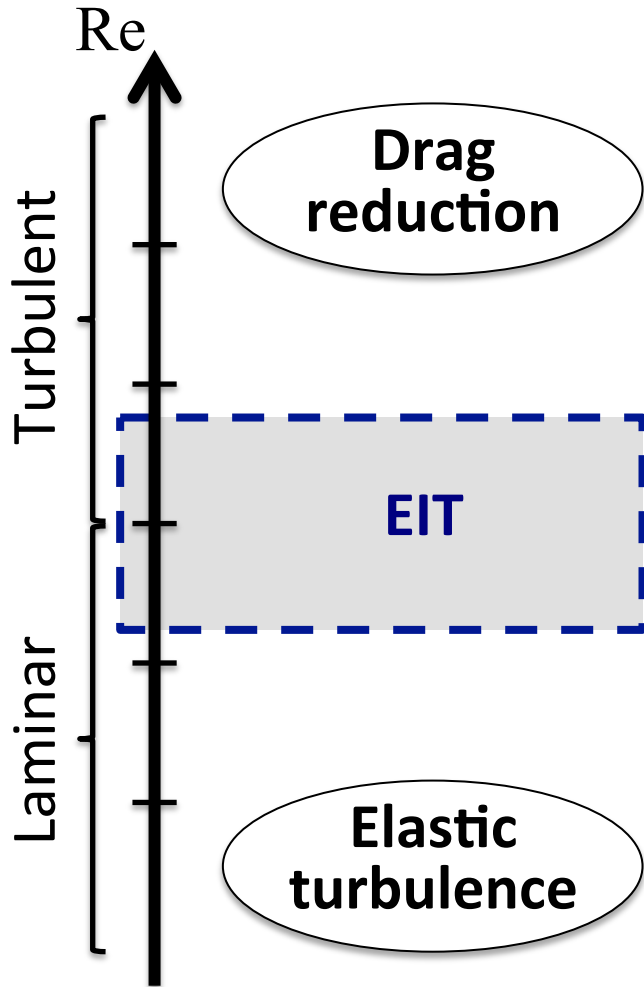
S. Sid¹, Y. Dubief² & V.E. Terrapon¹

¹ University of Liege (Belgium)

² University of Vermont



Polymers and turbulence



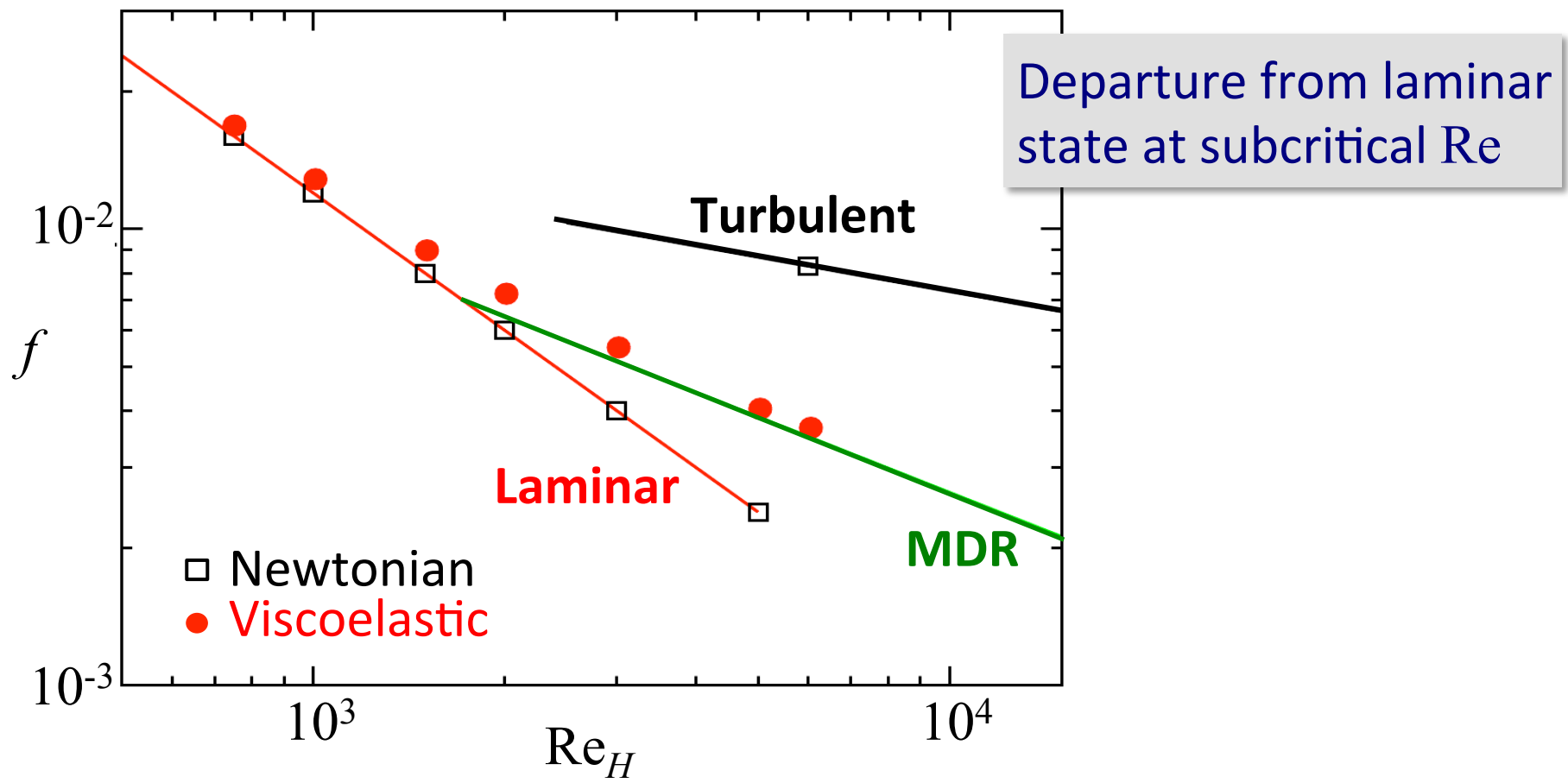
Elasto-Inertial Turbulence

- Non-laminar chaotic state
- **Elastic** and **inertial** instabilities

-
- 2D
 - Small-scale critical

Friction factor – Simulations

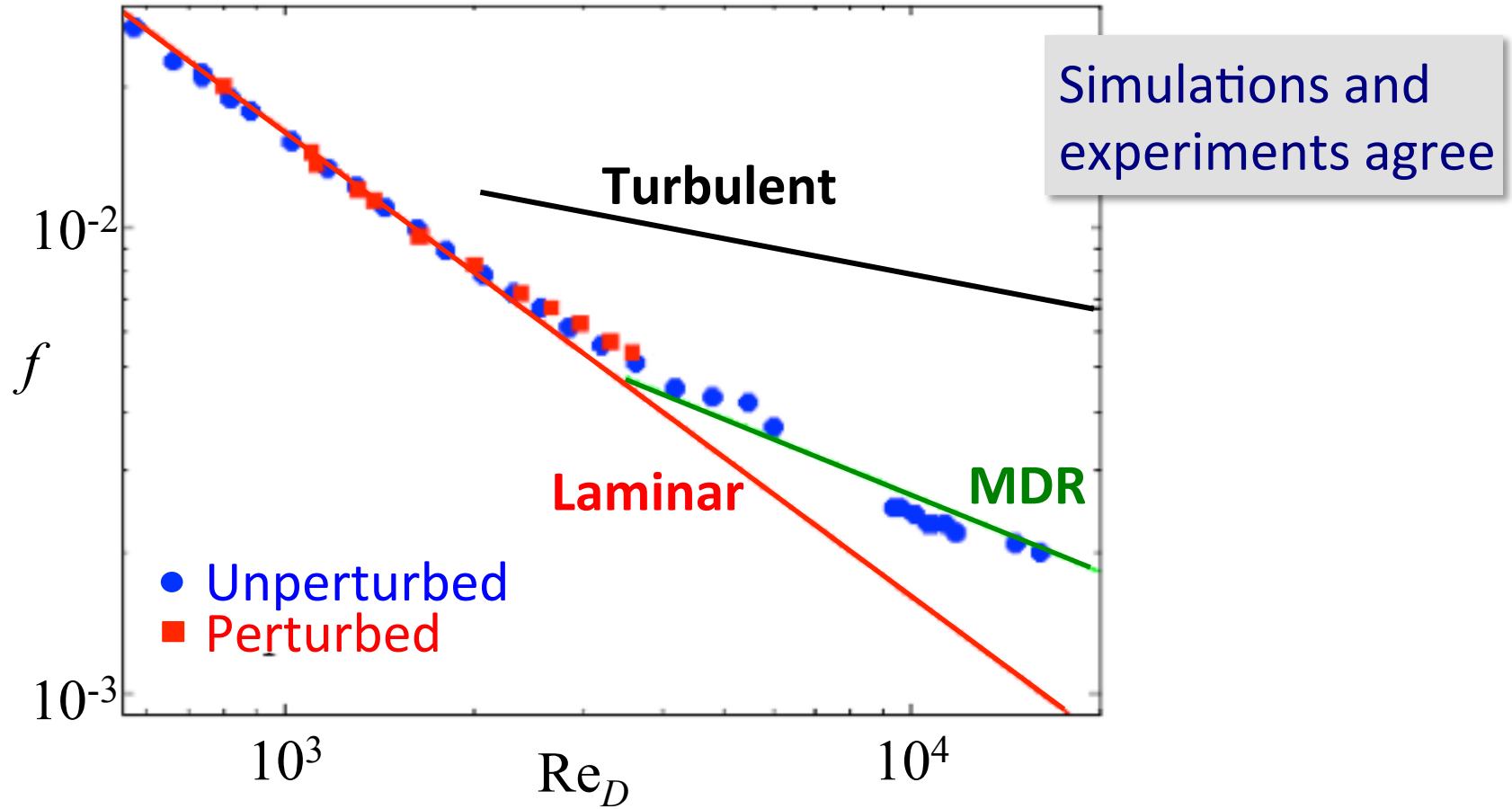
Channel flow (FENE-P)



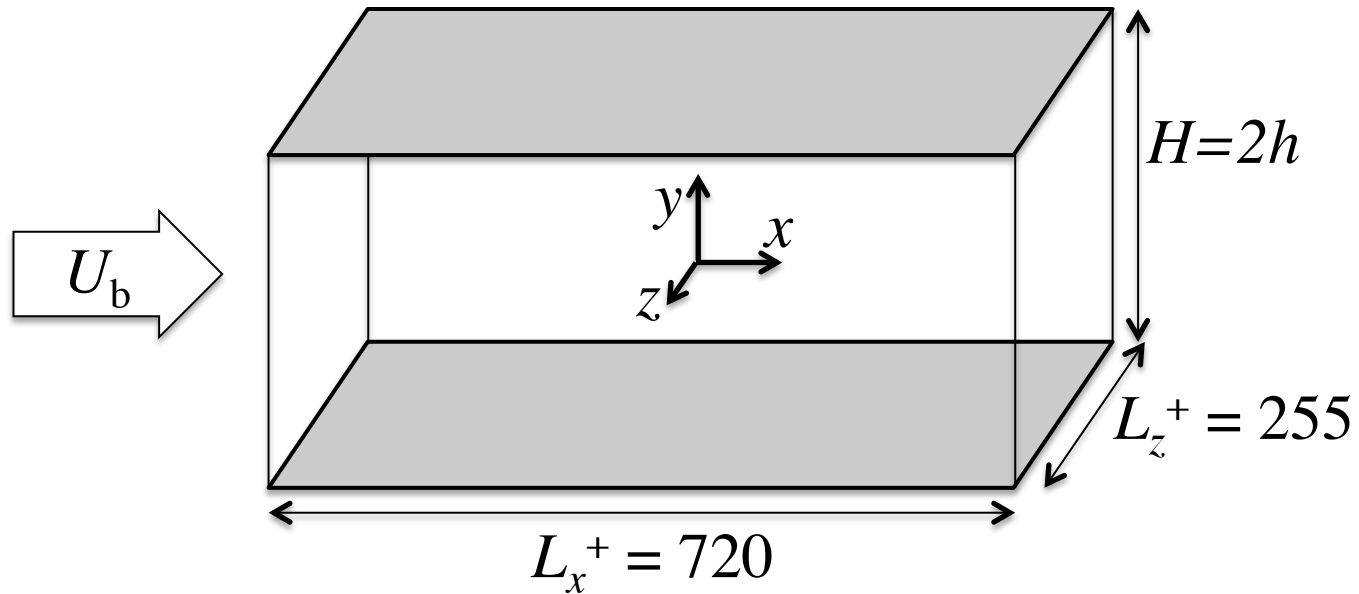
Dubief *et al.* (Phys. Fluids, 2013)
Terrapon *et al.* (J. Turbul., 2014)

Friction factor – Experiments

Pipe flow with 500 ppm PAAm solution



Numerical methodology



- DNS with **FENE-P** model
- Periodic **channel** flow (const. pressure gradient)
- **2D** (512×128) and 3D (256×128×128)
- Initial **perturbation** (blowing and suction at walls)
- 2 different **codes** with different numerics

FENE-P model

Continuity $\nabla \cdot \mathbf{u} = 0$

Momentum
$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla p + \frac{\beta}{\text{Re}} \nabla^2 \mathbf{u} + \frac{1-\beta}{\text{Re}} \nabla \cdot \mathbf{T} + \frac{dP}{dx} \mathbf{e}_x$$

Polymer stress
$$\mathbf{T} = \frac{1}{\text{Wi}} \left(\frac{\mathbf{C}}{1 - \text{tr} \mathbf{C} / L^2} - \mathbf{I} \right)$$

Conformation tensor
$$\frac{\partial \mathbf{C}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{C} = \nabla \mathbf{u} \cdot \mathbf{C} + \mathbf{C} \cdot \nabla \mathbf{u}^T - \mathbf{T}$$

Ratio of solvent viscosity to zero-shear viscosity $\beta = 0.97$

Maximum polymer extension $L = 70.9$

Reynolds number $\text{Re}^+ = 85$

Weissenberg number $\text{Wi}^+ = 40, 100$

Similar results at lower Re^+

Advection and small scales

$$\underbrace{\frac{\partial \mathbf{C}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{C}}_{\text{Advection}} = \underbrace{\nabla \mathbf{u} \cdot \mathbf{C} + \mathbf{C} \cdot \nabla \mathbf{u}^T - \mathbf{T}}_{\text{Nonlinear source term}} \left[\underbrace{+ \frac{1}{\text{ReSc}} \nabla^2 \mathbf{C}}_{\text{GAD}} \right]$$



- No diffusion
- Hyperbolic
- Sub-Kolmogorov scales
- Need stabilization

Global artificial diffusion (GAD)

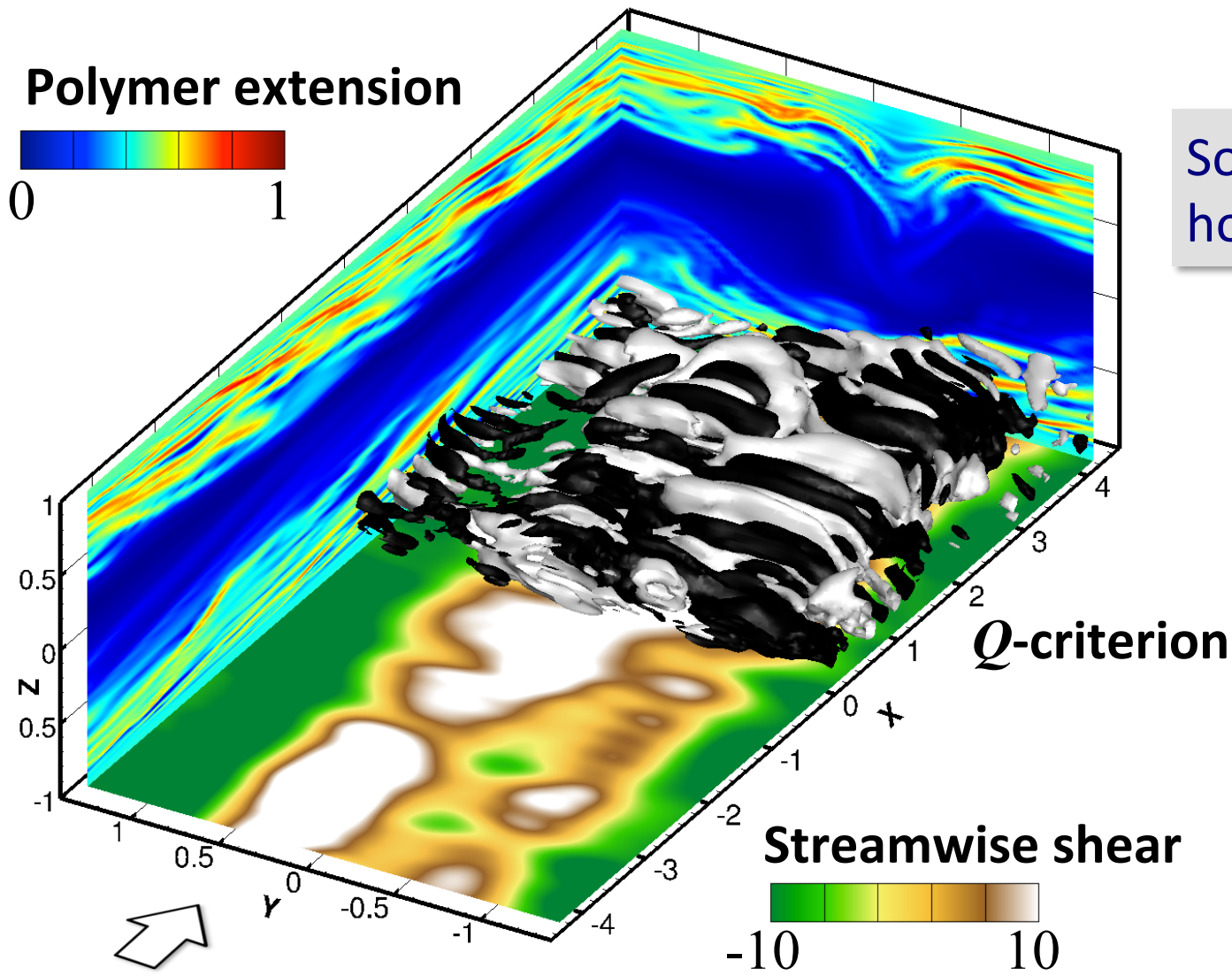
- A** • Used by many with $\text{Sc}_{\text{num}} \sim 1$
- But $\text{Sc}_{\text{polymer}} \sim 10^6$

Local artificial diffusion (LAD)

- B** • Only locally applied
- Never needed at low Re

3D simulation at supercritical Re

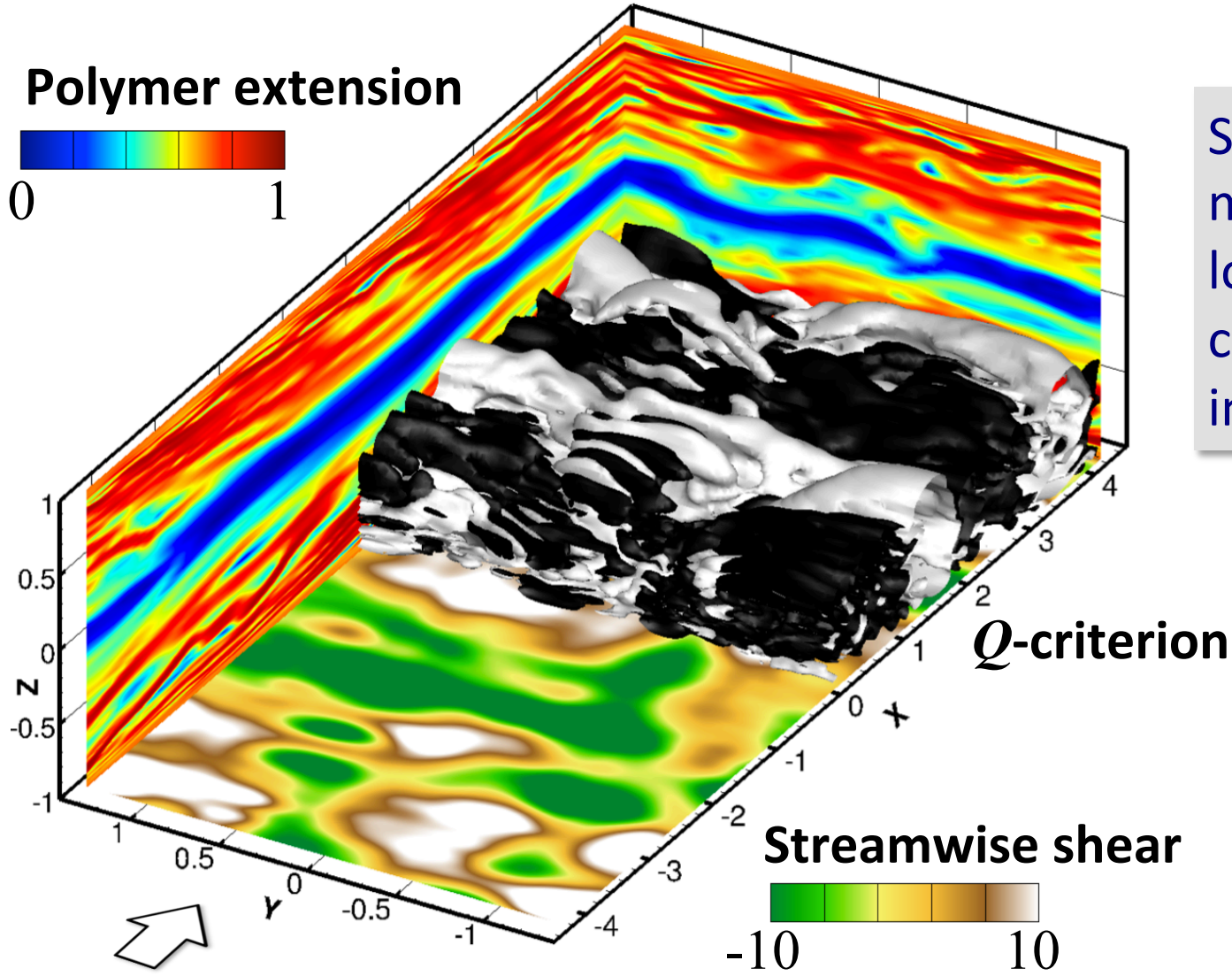
$Wi^+ = 40$



Some spanwise homogeneity

3D simulation at supercritical Re

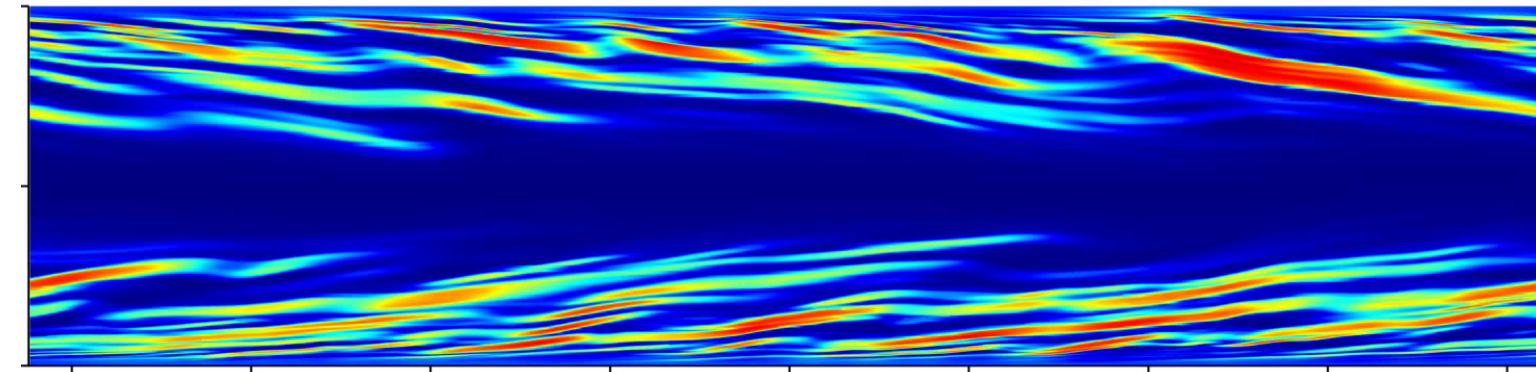
$Wi^+ = 100$



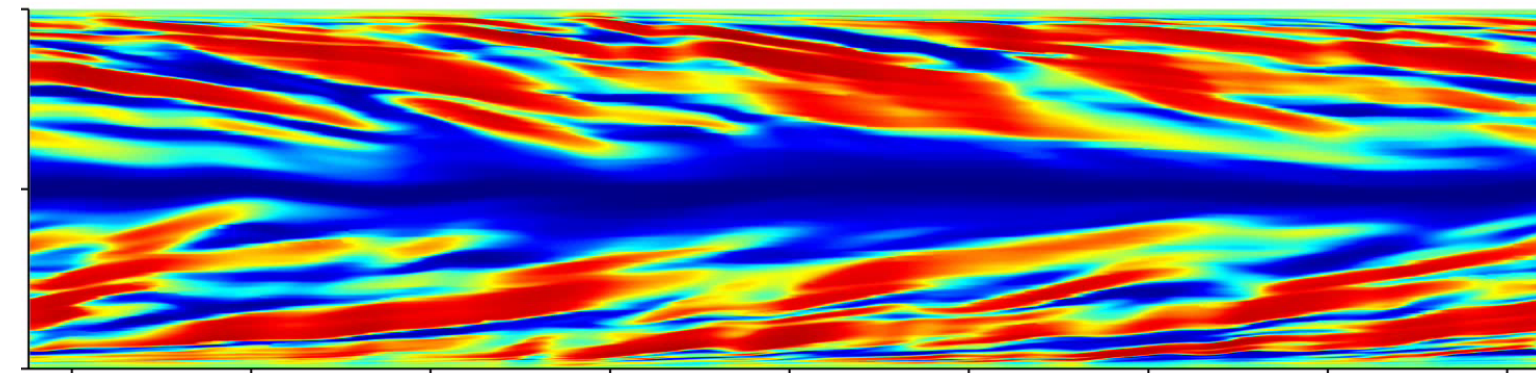
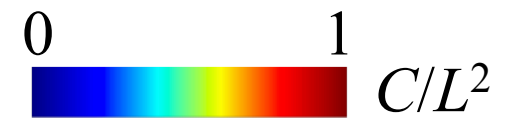
Structures are more 2D due to lower relative contribution of inertia

2D simulation at subcritical Re

Polymer extension

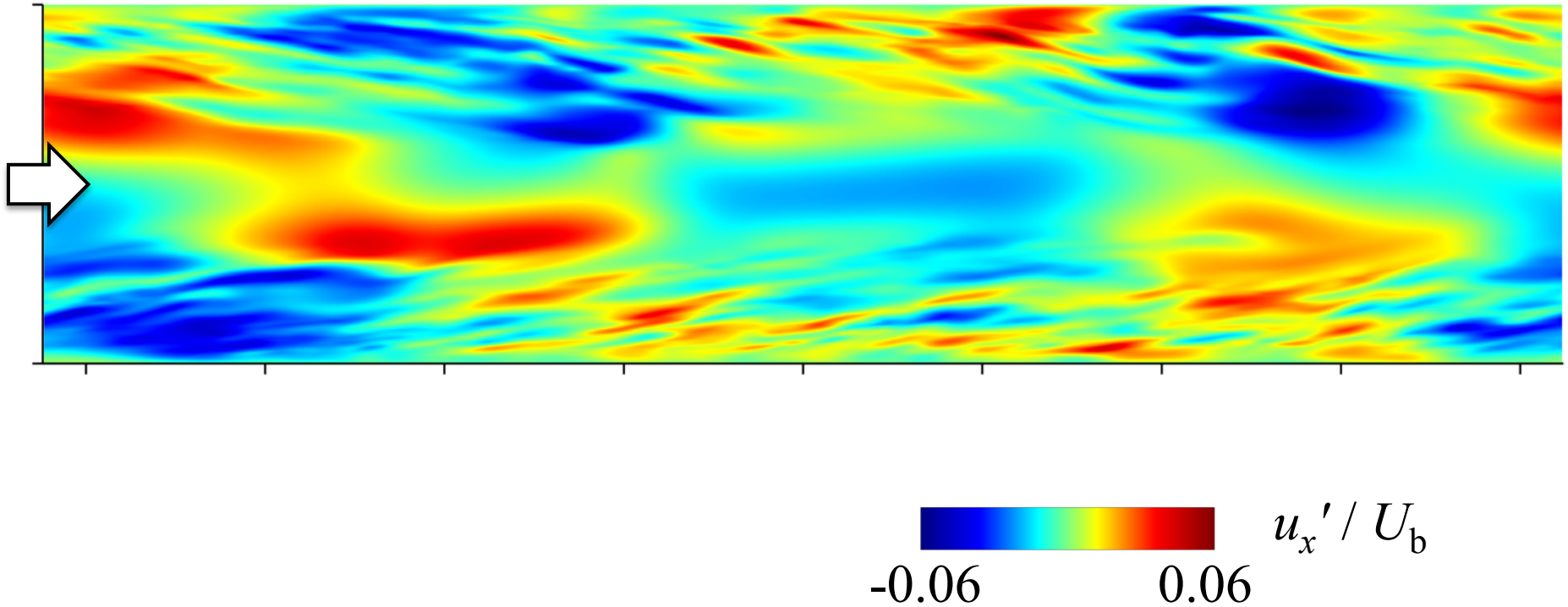


$Wi^+ = 40$



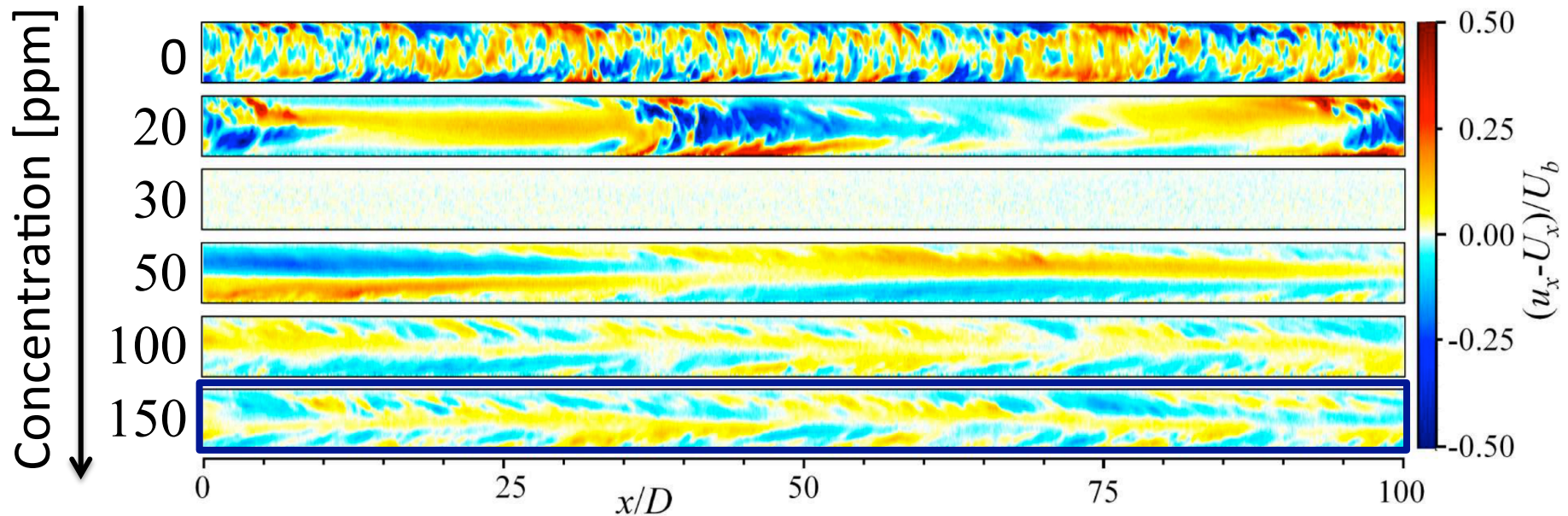
$Wi^+ = 100$

Streamwise velocity fluctuations



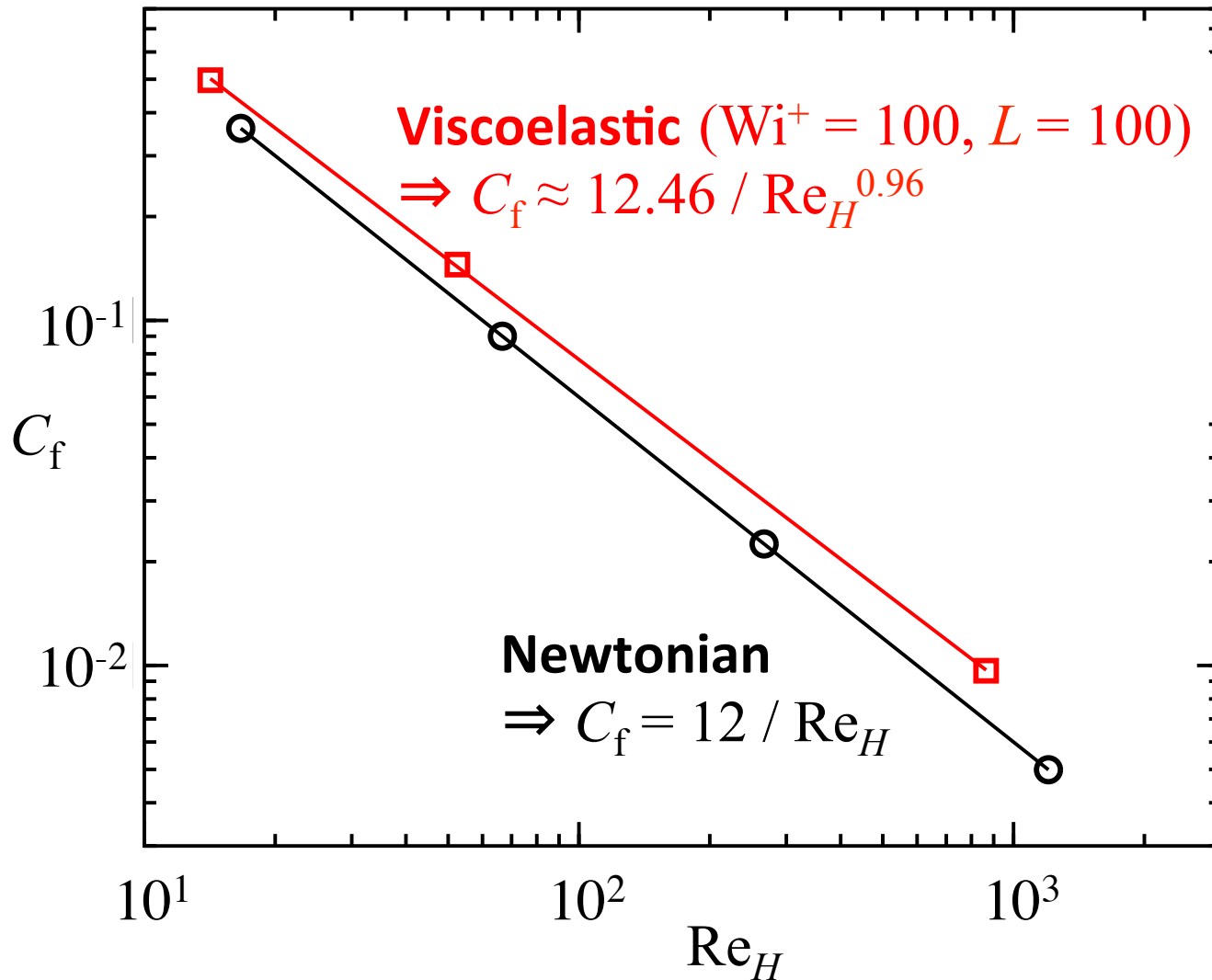
PIV measurements in viscoelastic pipe flow

Streamwise velocity fluctuations at $Re_D = 3150$



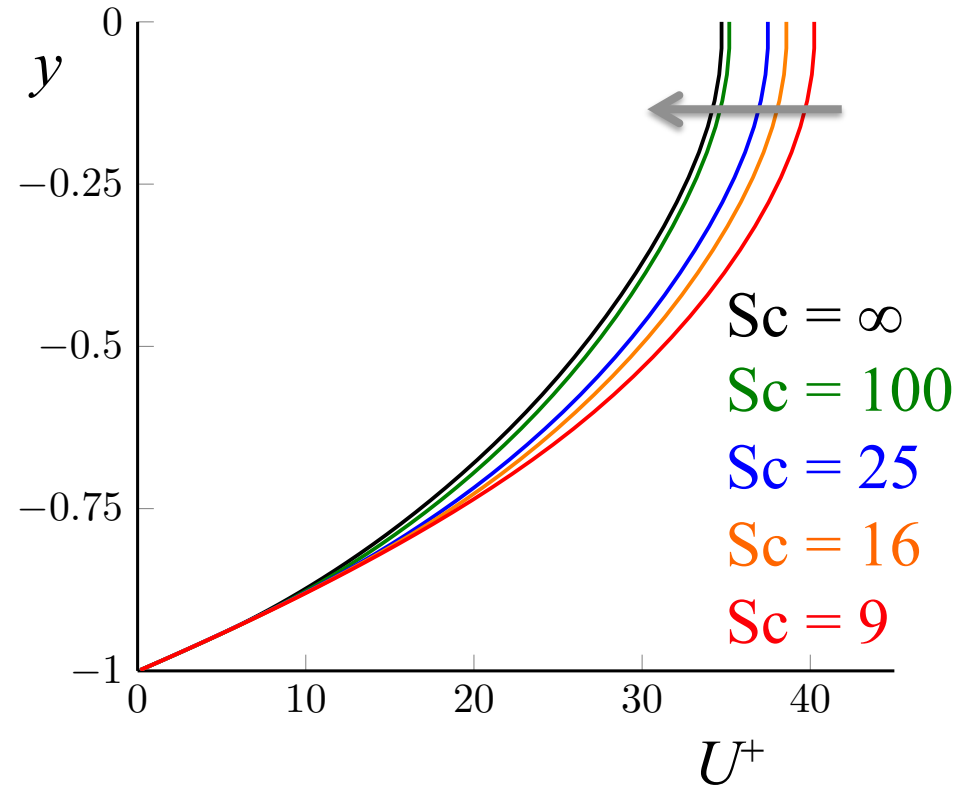
2D simulation at subcritical Re

Friction coefficient

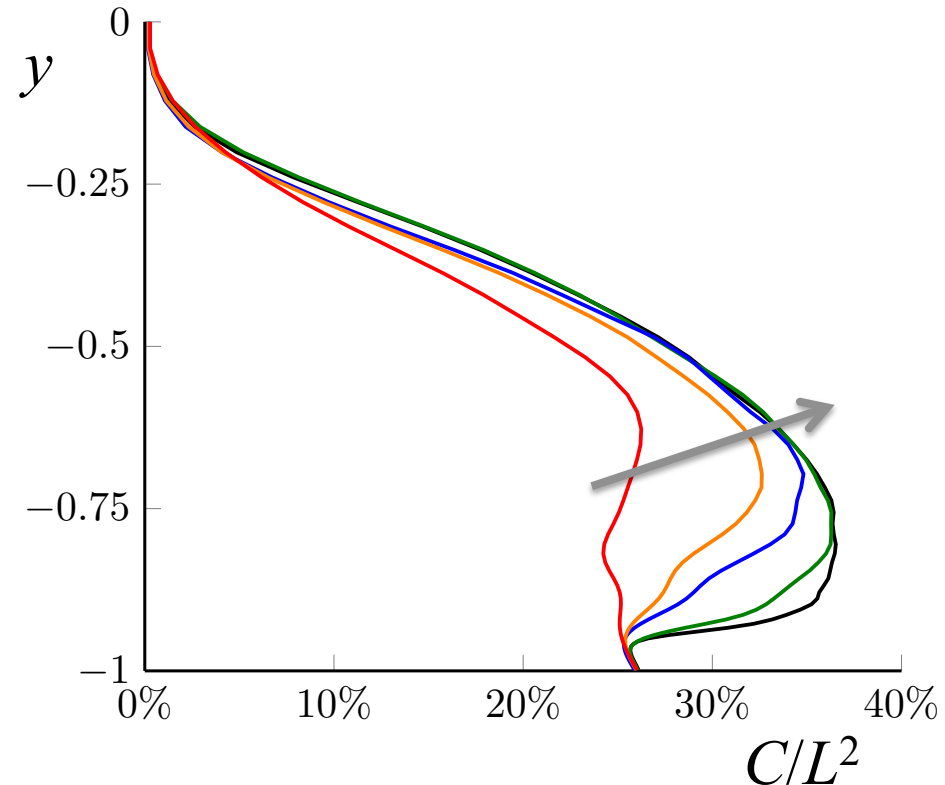


Departure from laminar flow similar to 3D

Mean velocity

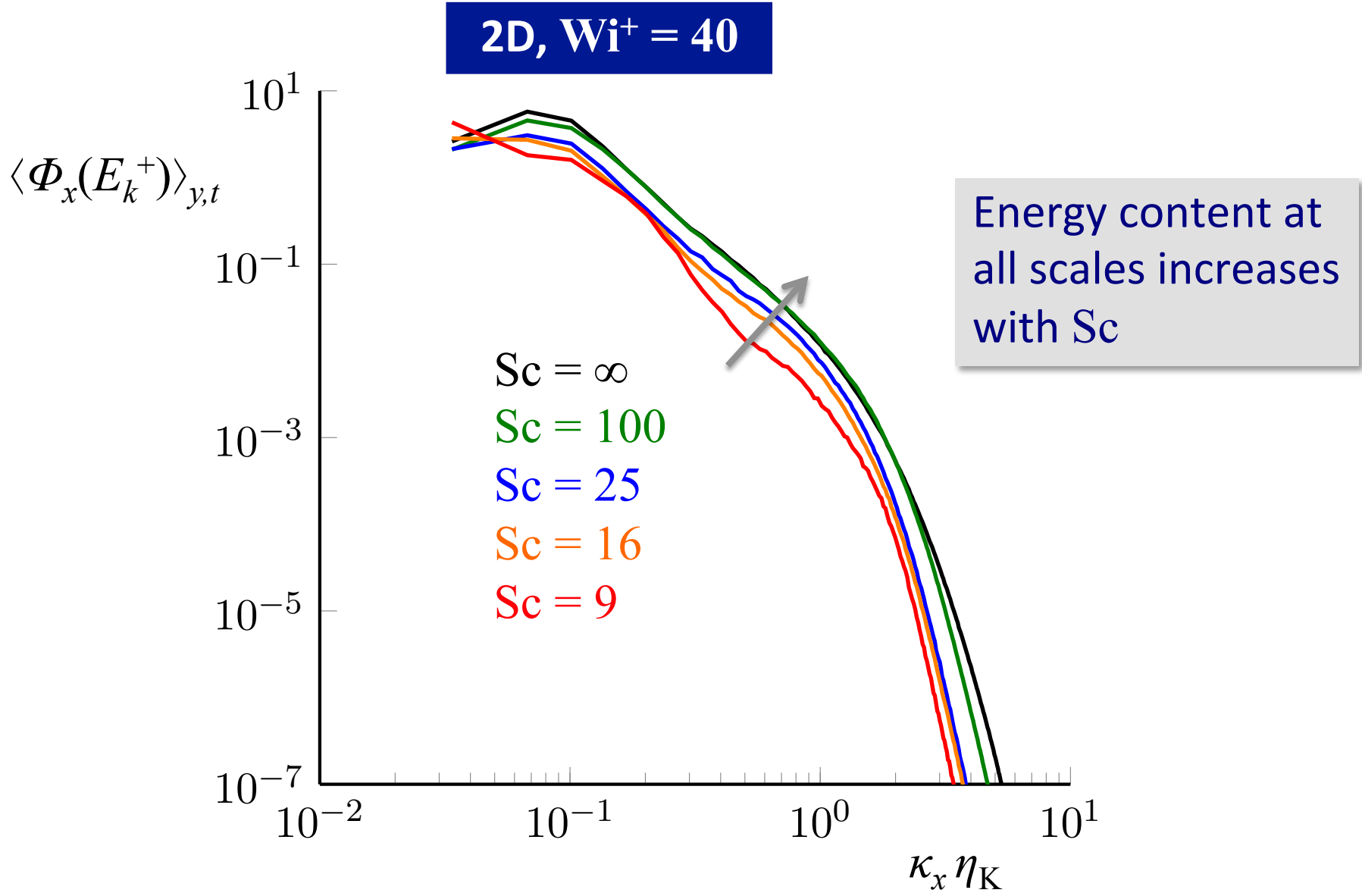


Mean polymer extension



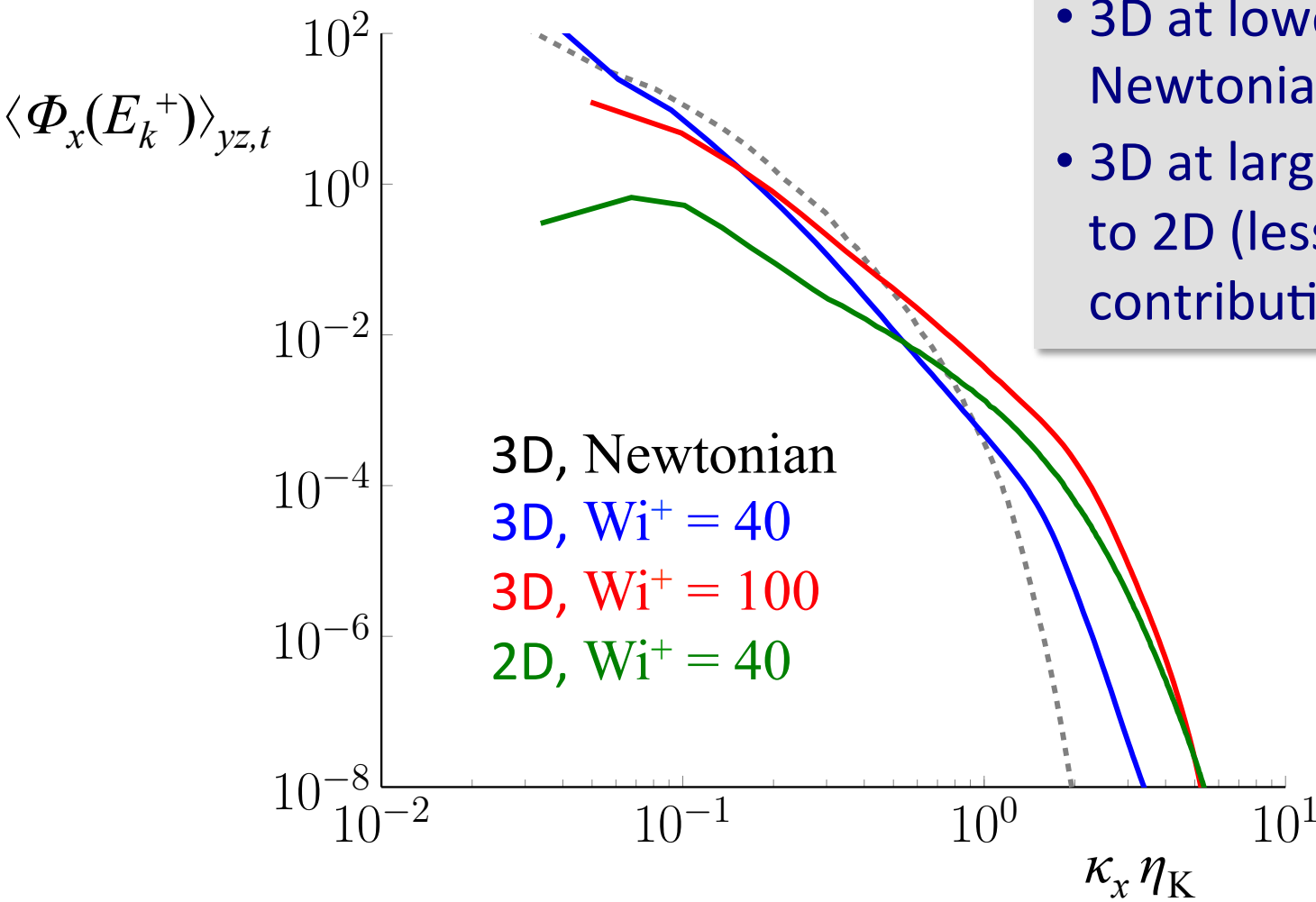
- $Sc \sim < 9$ lead to laminarization!
- Drag and polymer extension increase with Sc

Integrated streamwise spectrum of kinetic energy



Integrated streamwise spectrum of kinetic energy

$Re^+ = 85, Sc = \infty$



- 3D at lower Wi shows Newtonian features
- 3D at larger Wi similar to 2D (less inertial contribution)

3D, Newtonian
3D, $Wi^+ = 40$
3D, $Wi^+ = 100$
2D, $Wi^+ = 40$

Conclusions

- EIT is mostly 2D
- Small scales are critical
- Need to respect physics (high Schmidt number)



Open questions

- EIT = elastic turbulence?
- EIT = ultimate MDR state?
- Theory (predictions, shape of spectra, ...)

Acknowledgement



Questions



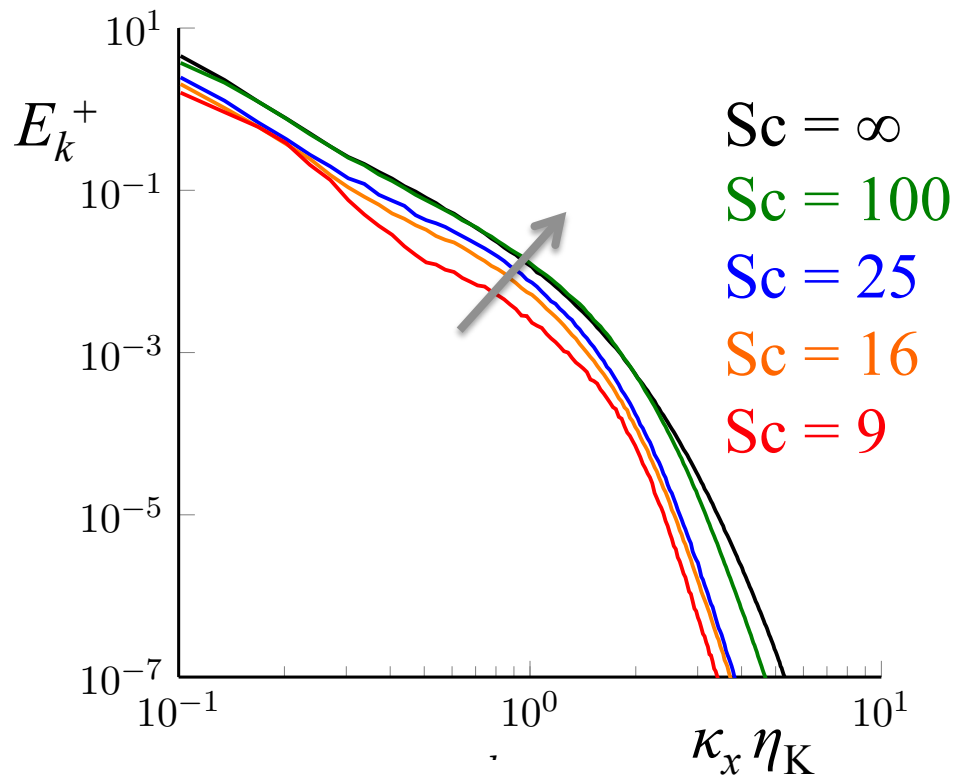
BACKUP

Schmidt number effect

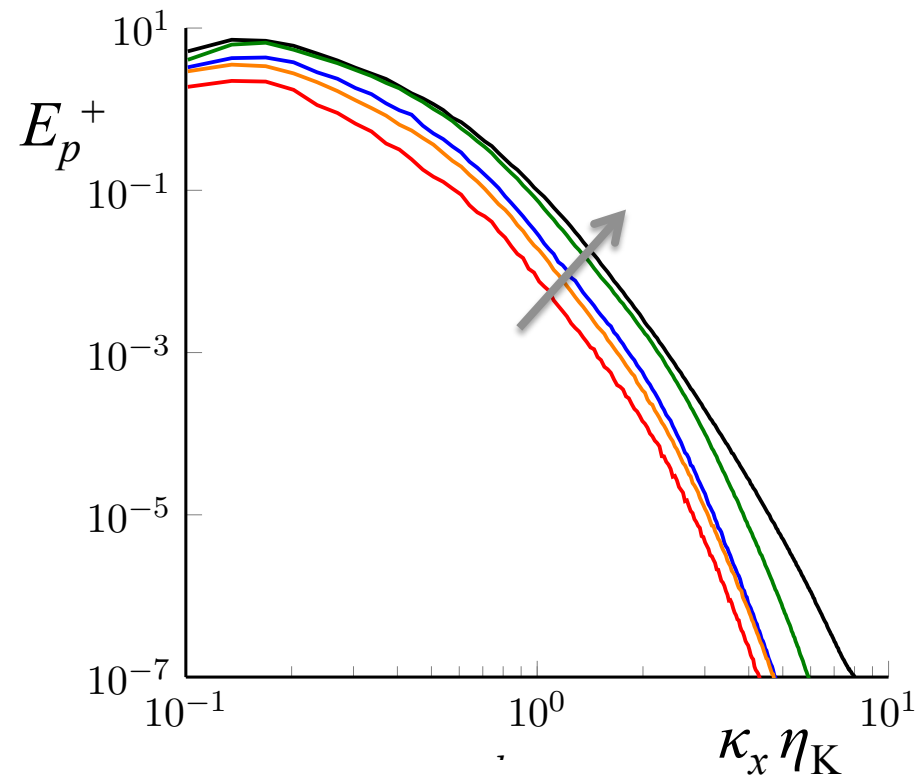
$Wi^+ = 40$

Time-averaged streamwise spectra

Kinetic energy



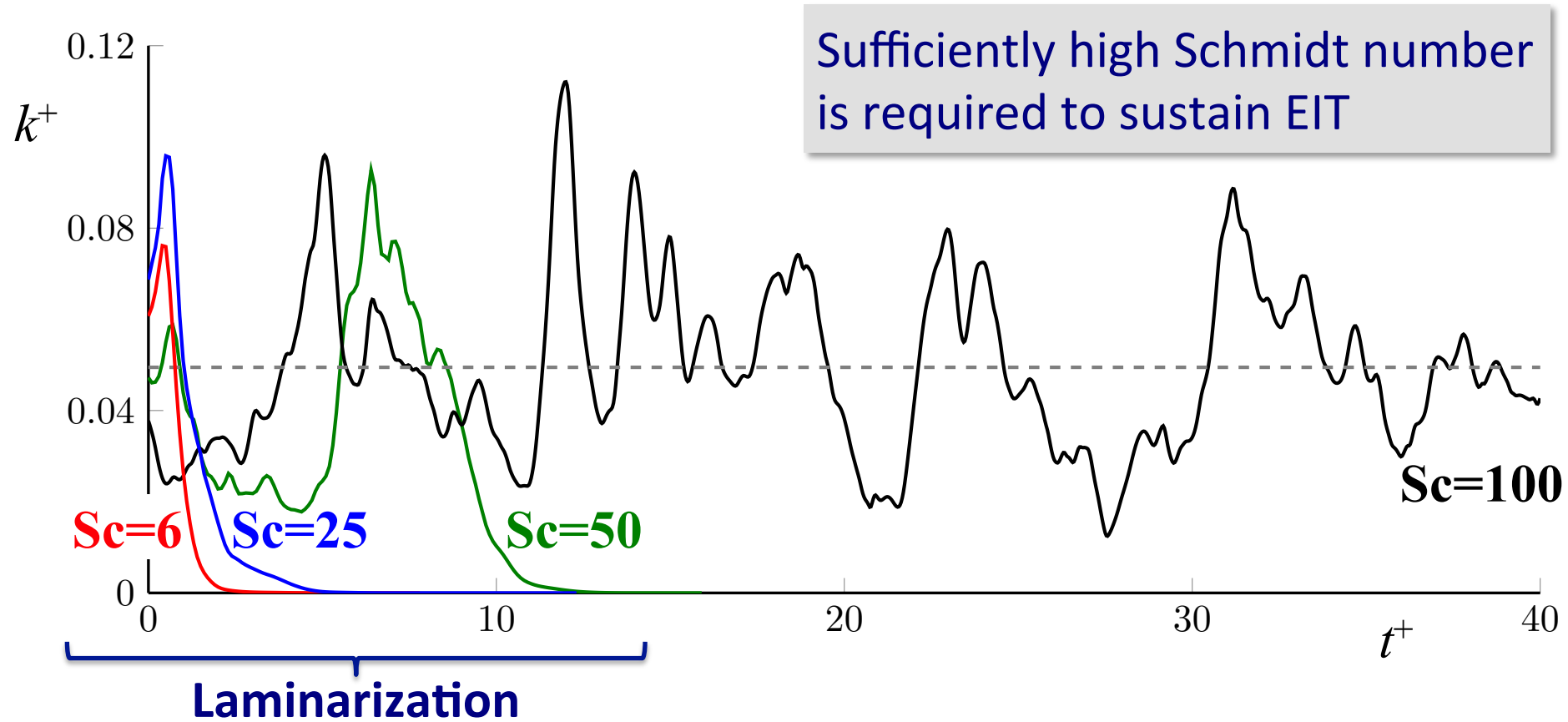
Elastic energy



Small scales are critical!

Schmidt number effect

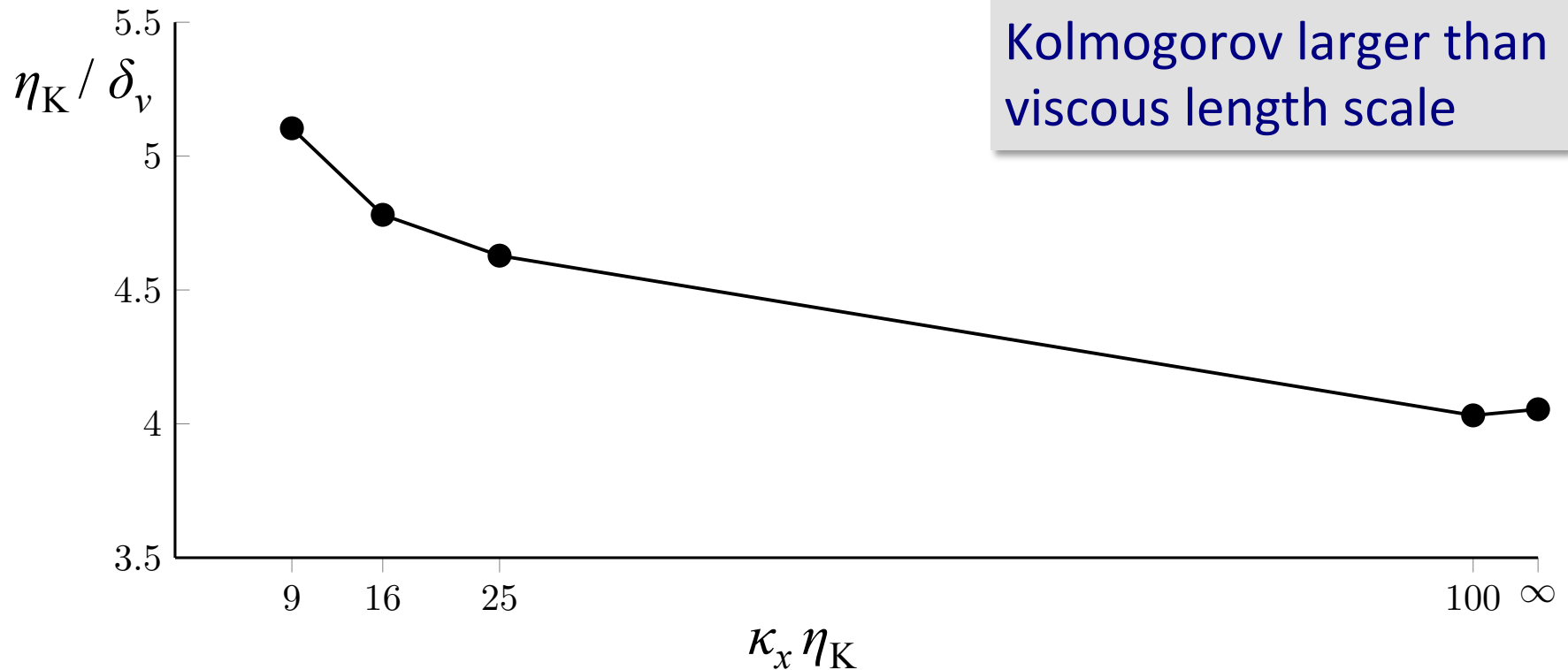
Turbulent kinetic energy



$$Wi^+ = 310, Re^+ = 40, \beta = 0.97, L = 70.9, GAD$$

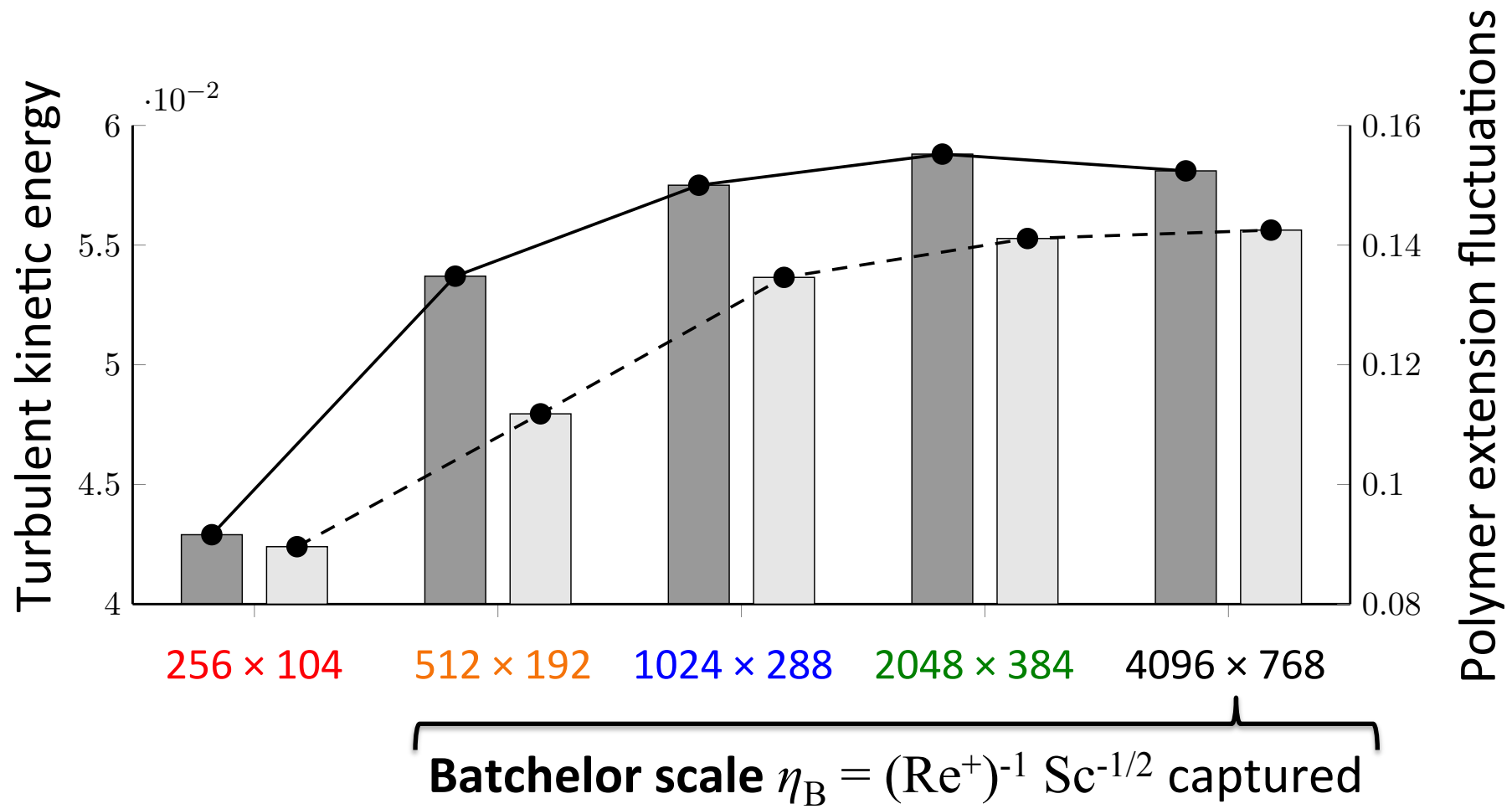
Schmidt number effect

Ratio of Kolmogorov $(\nu^3/\varepsilon)^{1/4}$ to viscous length scale (ν/u_τ)



$Wi^+ = 40, Re^+ = 85, \beta = 0.97, L = 70.9, LAD$

Sc=100 - Influence of the mesh

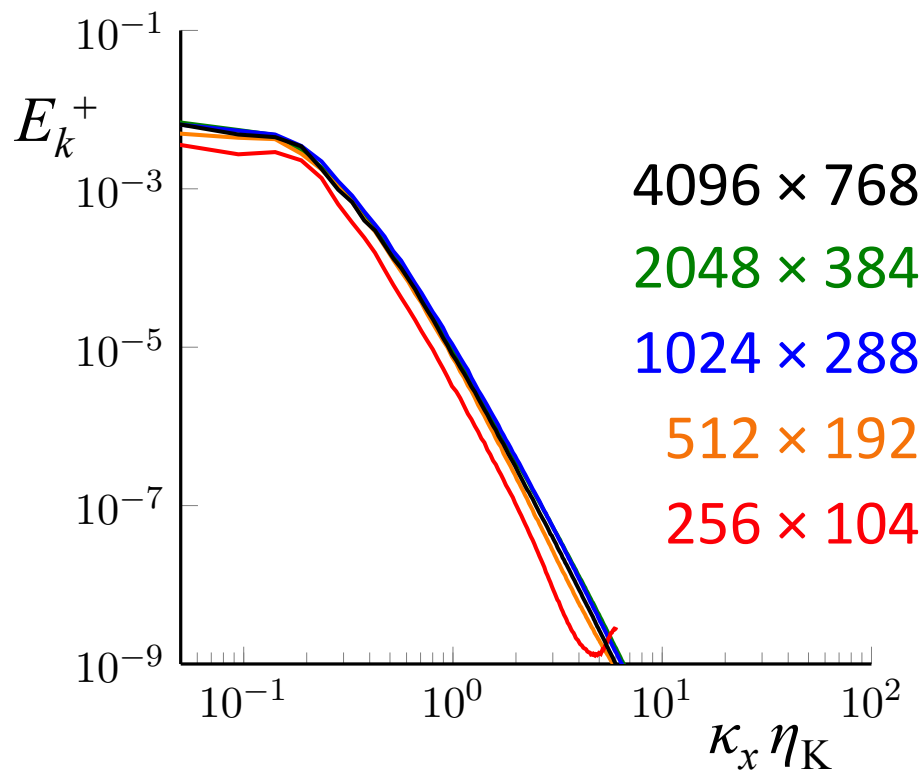


$Wi^+ = 310, \text{Re}^+ = 40, \beta = 0.97, L = 70.9, \text{GAD}$

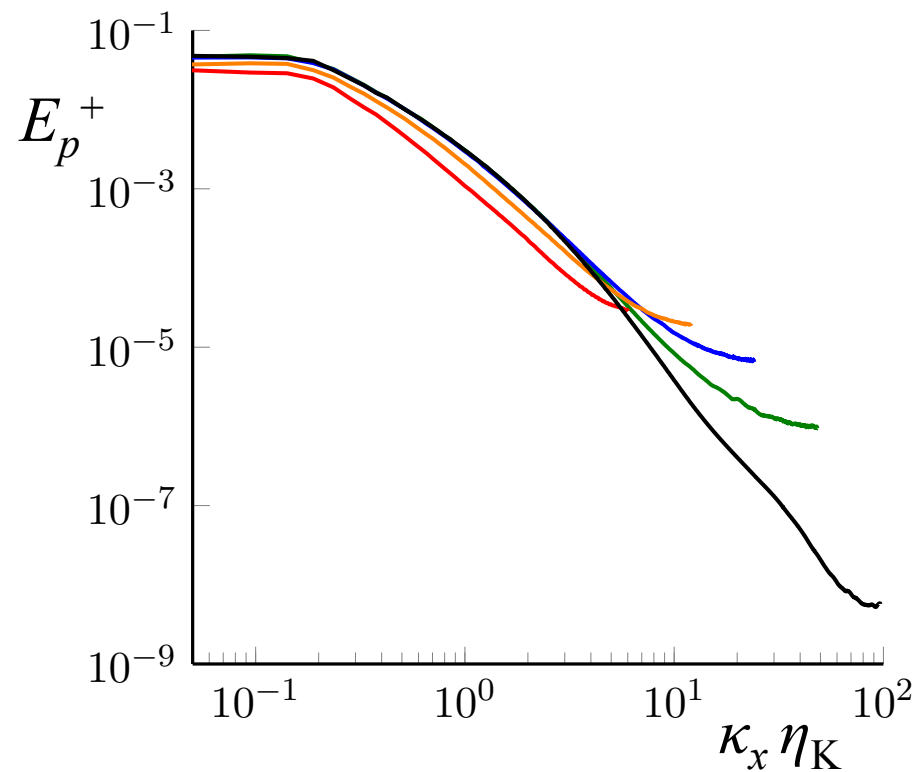
Sc=100 – Influence of the mesh

Time-averaged streamwise spectra

Kinetic energy



Elastic energy

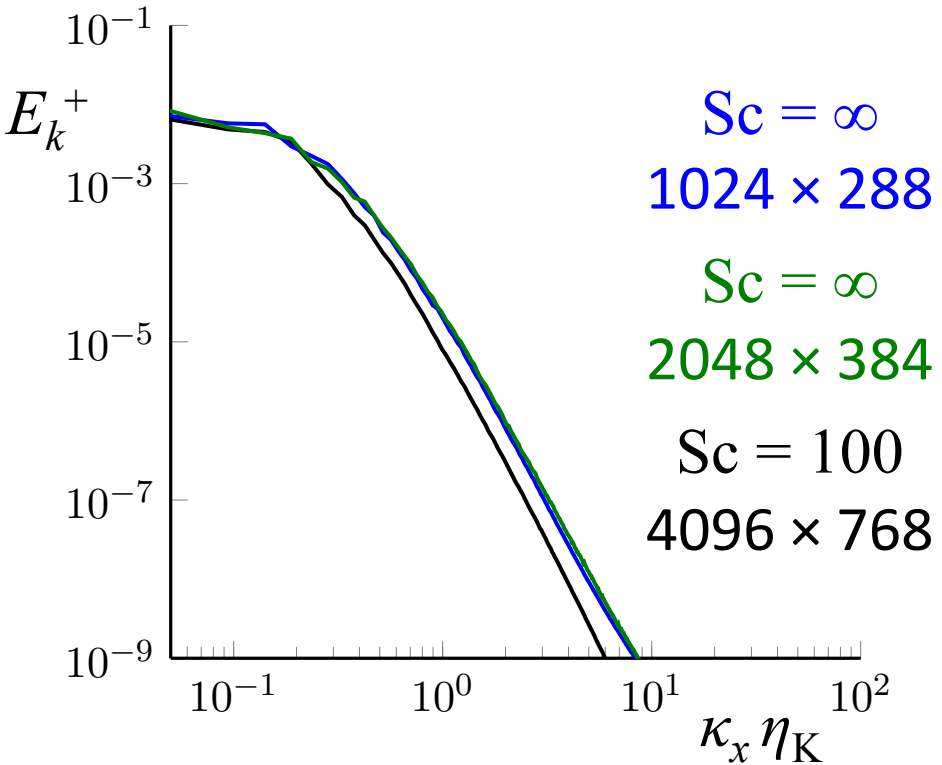


$Wi^+ = 310, Re^+ = 40, \beta = 0.97, L = 70.9, GAD$

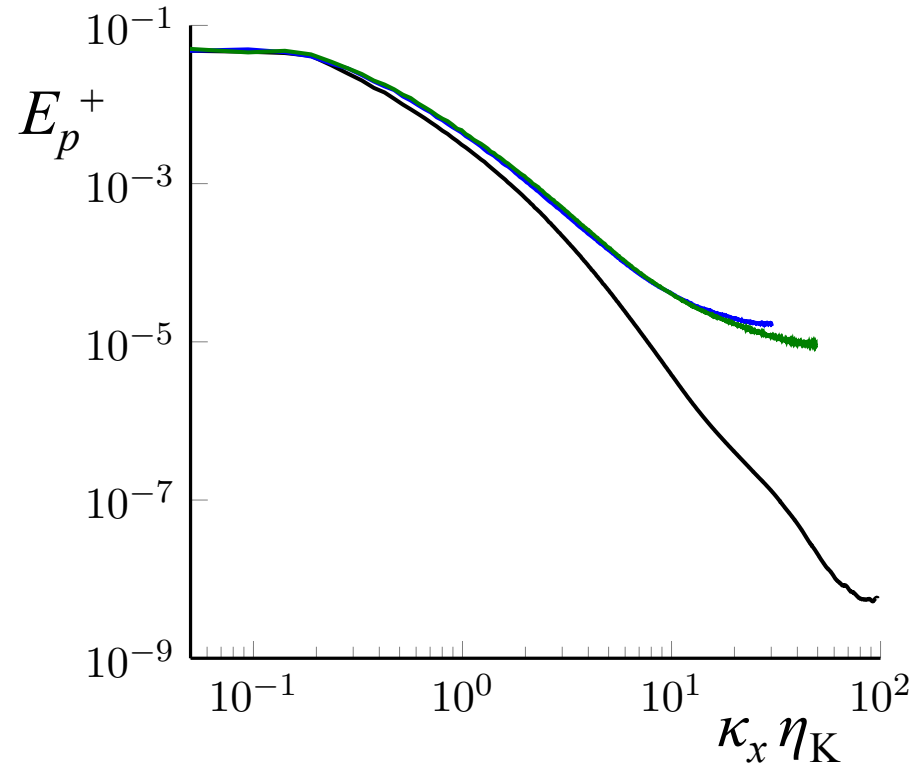
GAD vs. LAD

Time-averaged streamwise spectra

Kinetic energy

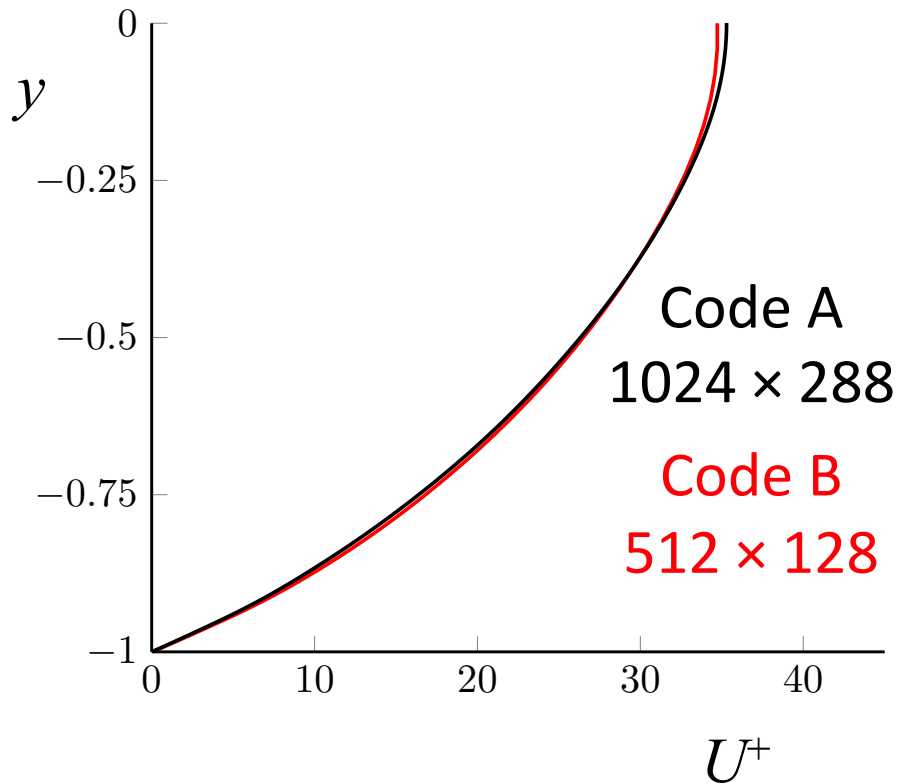


Elastic energy

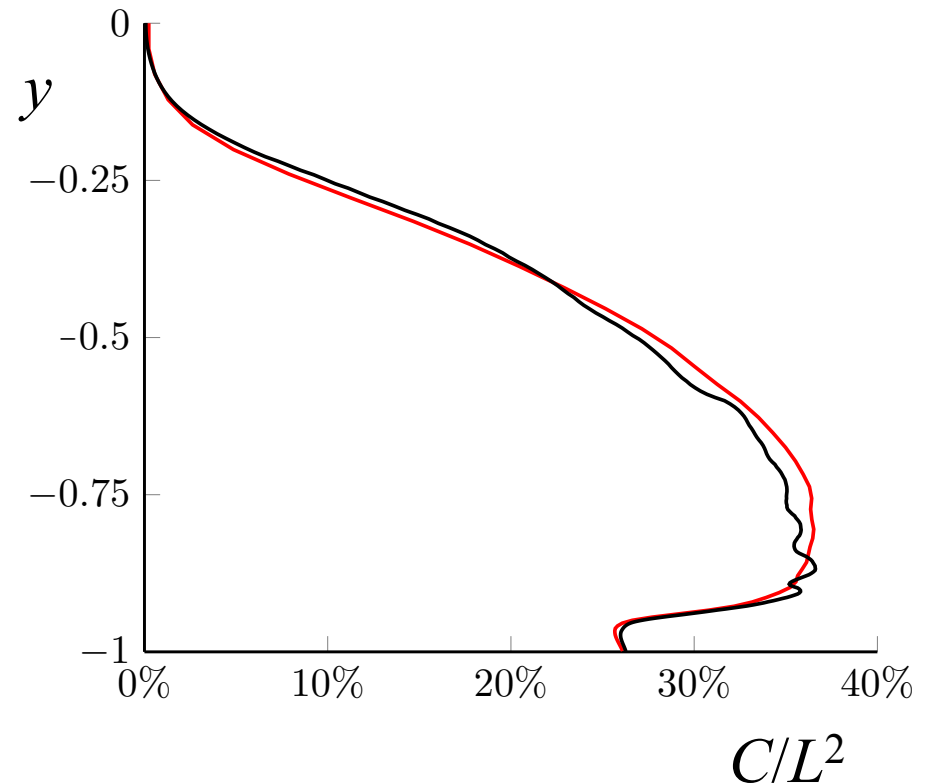


Code comparison

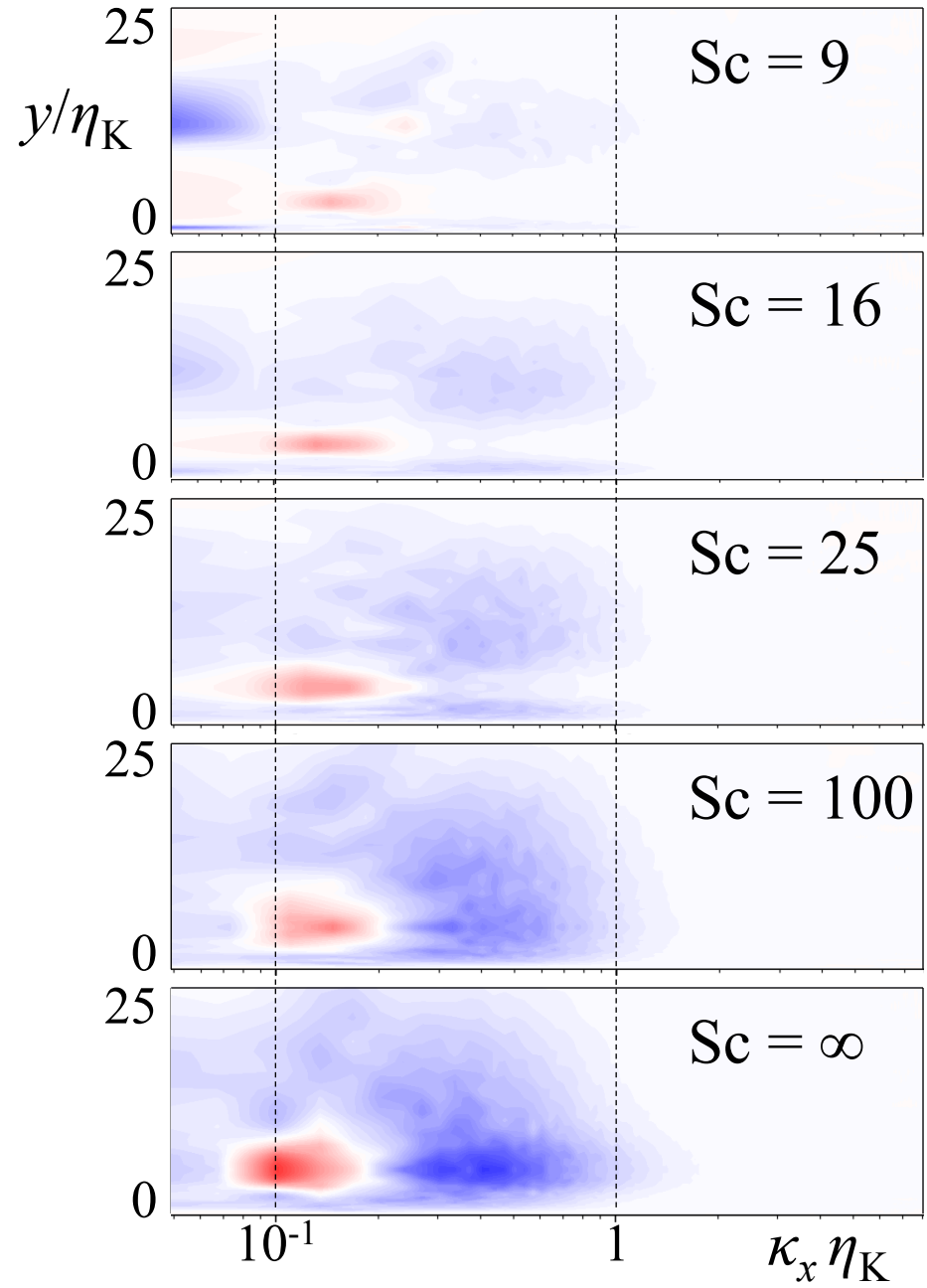
Mean velocity



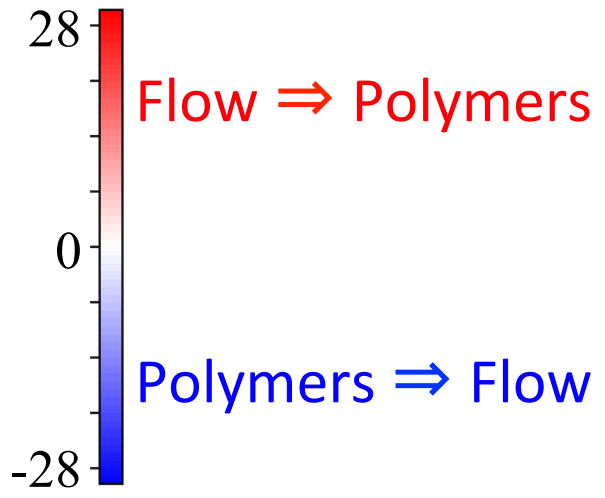
Mean polymer extension



Transfer from kinetic to elastic energy

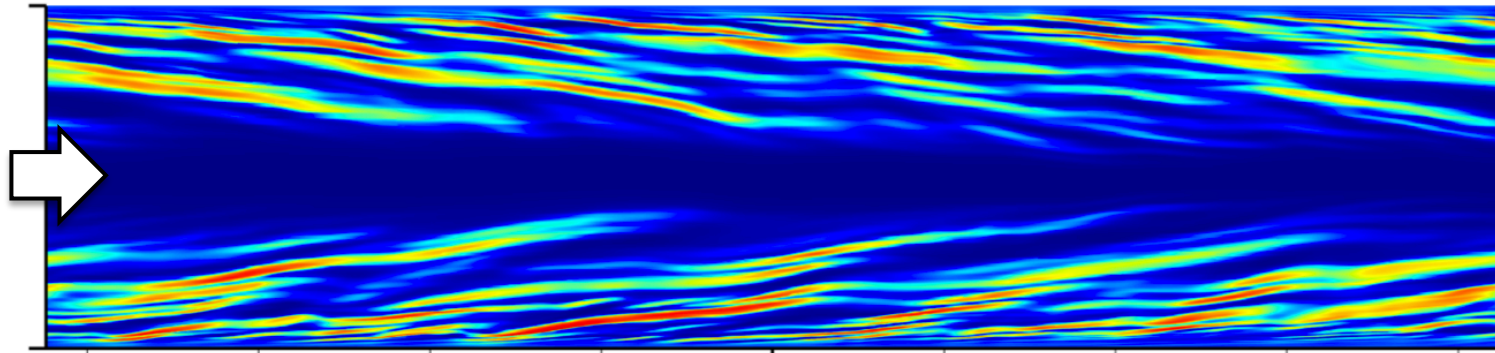


Streamwise spectrum $\Phi \left(\frac{1-\beta}{Re} T_{ij} S_{ij} \right)$

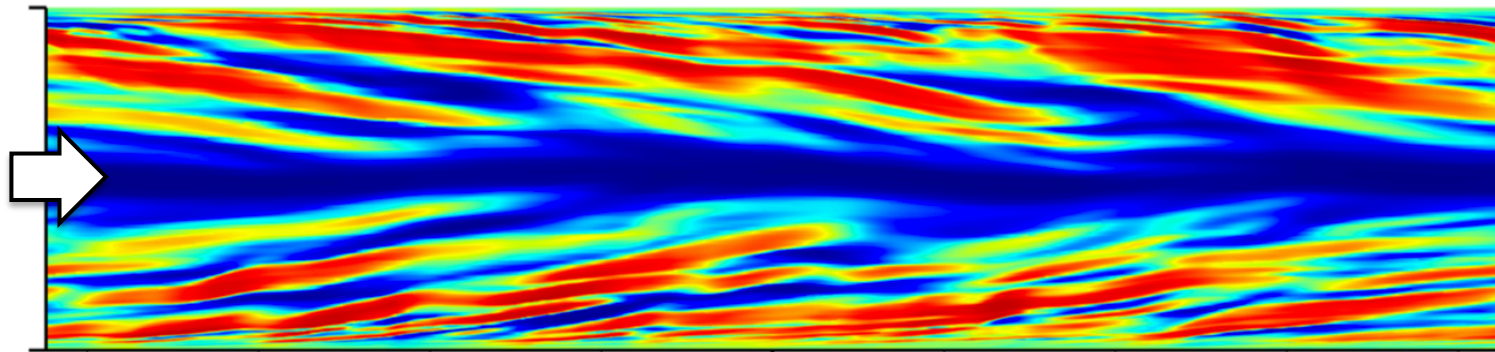


2D simulation at subcritical Re

Polymer extension



$Wi^+ = 40$



$Wi^+ = 100$