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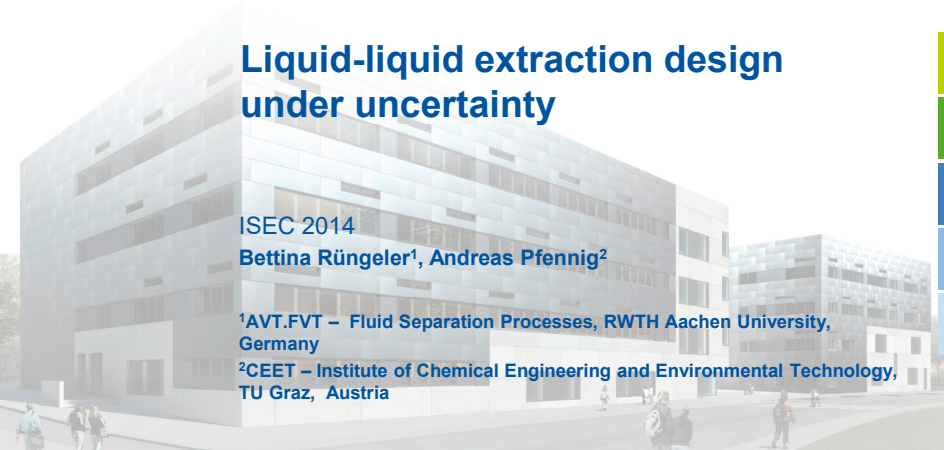
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Liquid-liquid extraction design under uncertainty

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Outline

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- Motivation
- Framework for the design under uncertainty
- Resource allocation
- Cascaded option trees
- Conclusion



Liquid-liquid extraction design under uncertainty

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Motivation



- new solvent extraction processes
 - high-viscous media
 - fermentation broths
 - aqueous two-phase systems
- low expertise in design and scale-up
- high uncertainties in knowledge and data

Goal: Optimal resource allocation in design of common and new solvent extraction processes

Liquid-liquid extraction design under uncertainty

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Uncertainty as supporting information




- uncertainty of input data quantifiable
 - uncertainty reducible by process development steps
- ➡ explicit consideration of uncertainties in all results
- ➡ analysis of sensitivities towards uncertainty levels
- ➡ systematic reduction of uncertainty
- economics as criterion for the selection of best option


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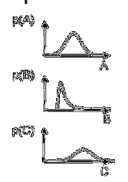
Design under uncertainty



process options

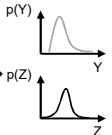


uncertainty in input parameters

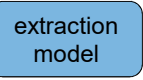


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uncertainty in results




extraction model

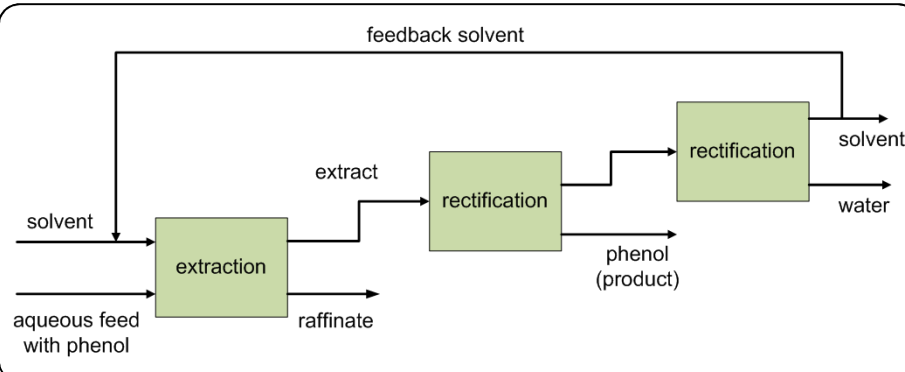


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Example process



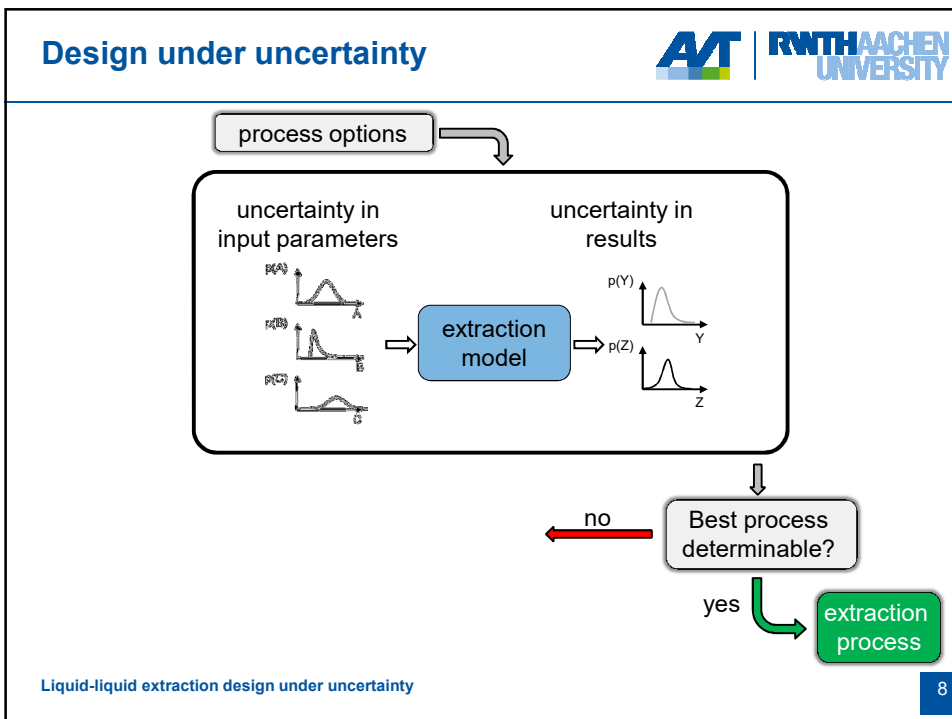
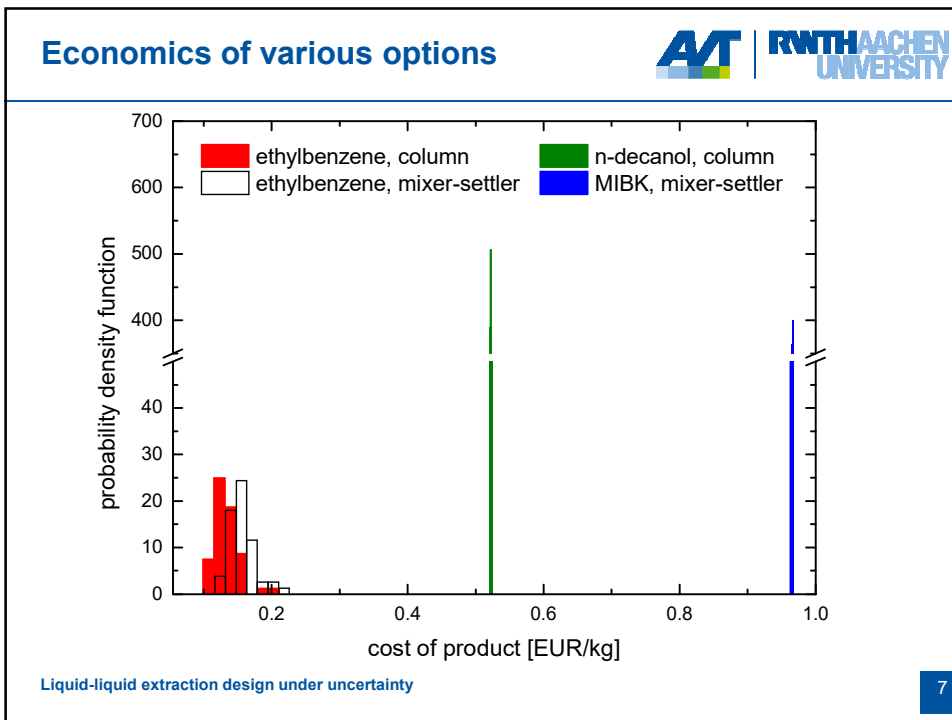


process options:

	solvent	device
	ethylbenzene	mixer-settler
	n-decanol	column
	methyl isobutyl ketone (MIBK)	

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modKL as distinctness measure

- modified Kullback-Leibler distance
- modification for symmetry: $\text{modKL}_{12} = \text{modKL}_{21}$
- comparison of distribution $p(x)$ and $q(x)$:

$$m(x) = \frac{1}{2}(p(x) + q(x))$$

$$\text{modKL} = \int_{-\infty}^{\infty} \frac{1}{2} p(x) \ln \frac{2p(x)}{p(x) + q(x)} dx + \int_{-\infty}^{\infty} \frac{1}{2} q(x) \ln \frac{2q(x)}{p(x) + q(x)} dx$$

$p(x) = q(x)$:
modKL = 0

$p(x) \neq q(x)$:
modKL = $\ln 2 \approx 0.69$

value of modKL	distinctness
0	identical
modKL < 0.65	slightly different
≥ 0.65	strongly different
0.69	totally different

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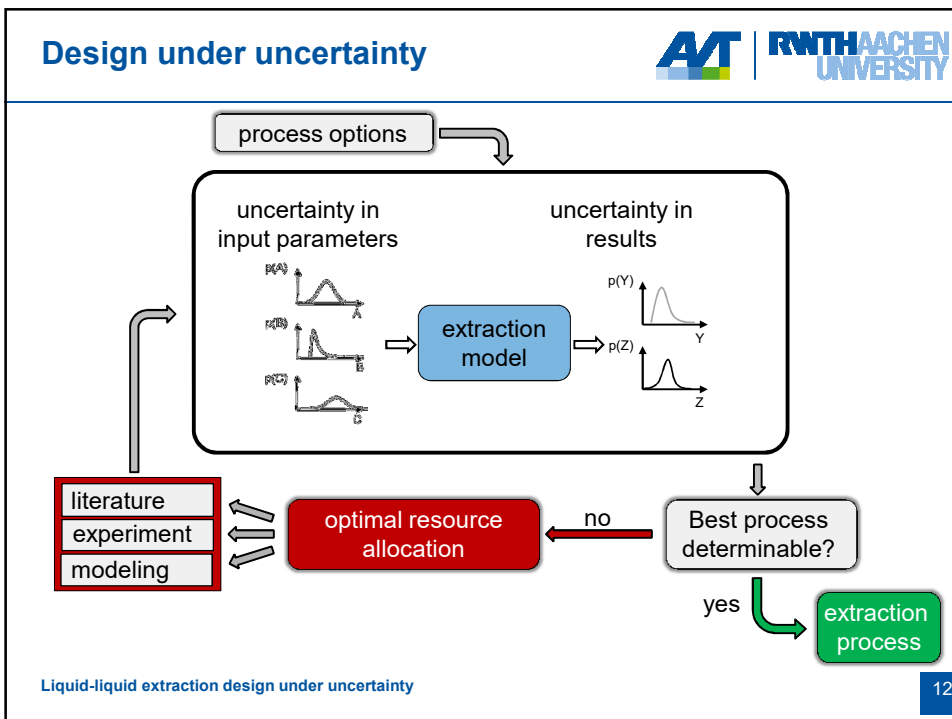
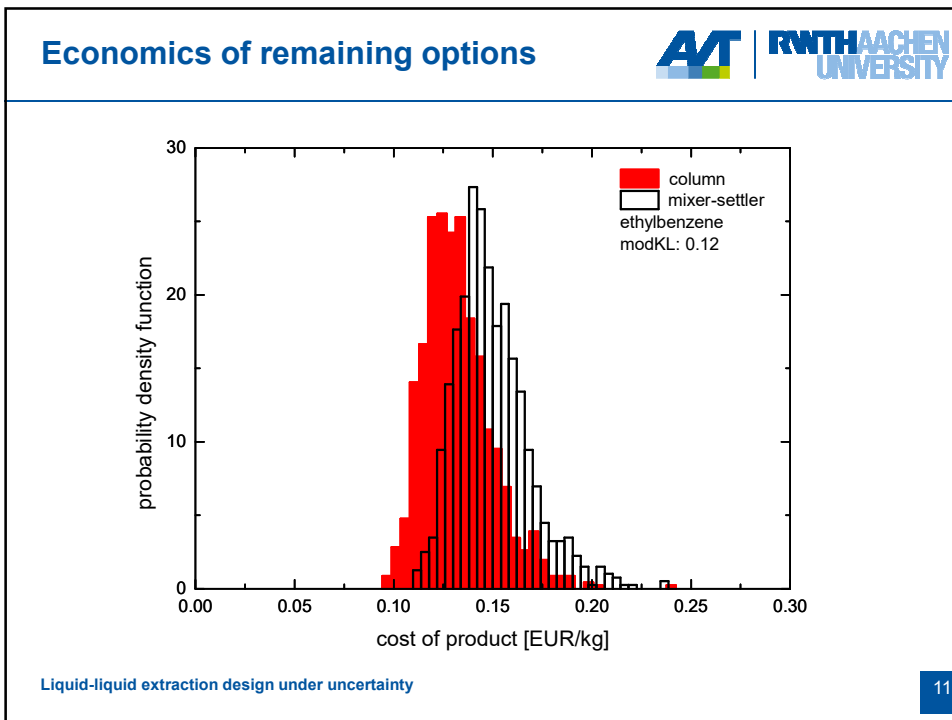
Berkelmans, I., 2010: *Development and Application of a Framework for Technology and Model Selection Under Uncertainty*. Massachusetts Institute of Technology

Comparison of processes


Process Comparison	modKL Value
ethylbenzene column vs. ethylbenzene mixer-settler	~0.12
ethylbenzene column vs. n-decanol column	~0.68
ethylbenzene column vs. MIBK mixer-settler	~0.68

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Definition of design steps



- methods for uncertainty reduction

literature
experiment
modeling

- reduce uncertainty for input parameters

distribution coefficient

density phase 1

density phase 2

interfacial tension

settling time

viscosity phase 1

viscosity phase 2

...

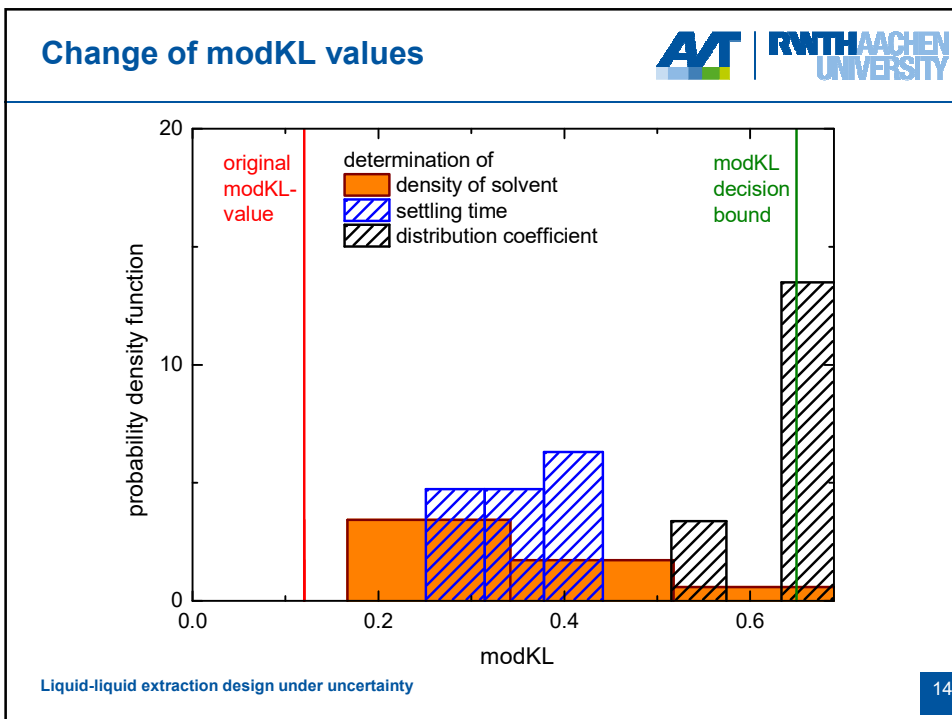
- associated data

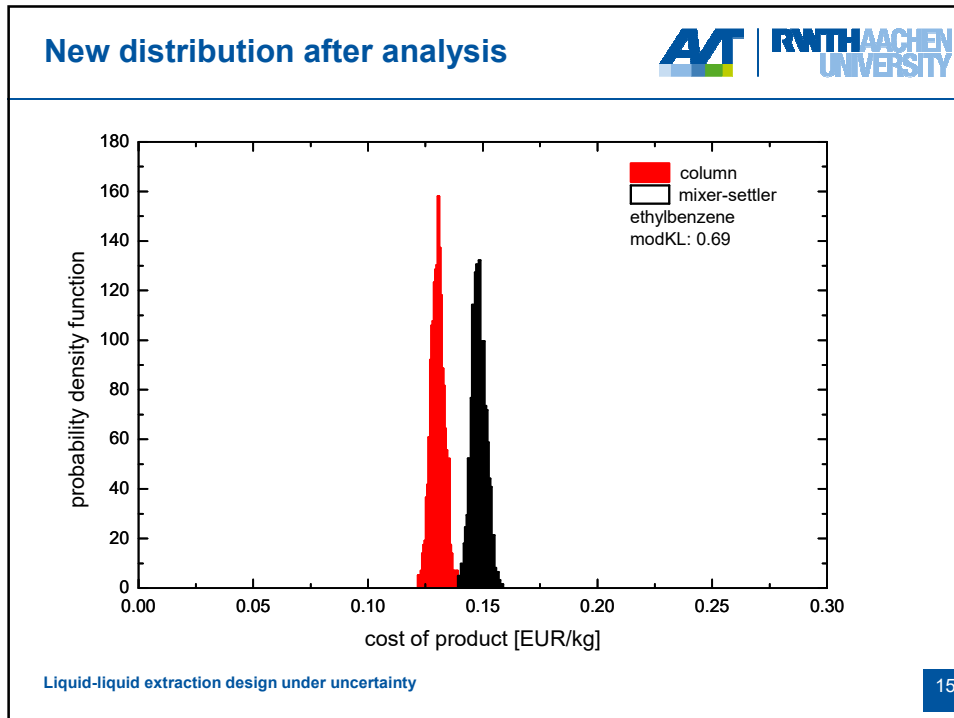
new uncertainty level

analysis costs

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Resource allocation

- How to choose next design step?
cost – benefit analysis
- cost:
 - cost for research (work and material)
- benefit:
 - reduced uncertainty
 - less risk for decision on best process

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Clear summary of design steps



- cascaded option tree

performance

	not tested
	good
	acceptable
	inadmissible

in order of resource allocation

overall performance

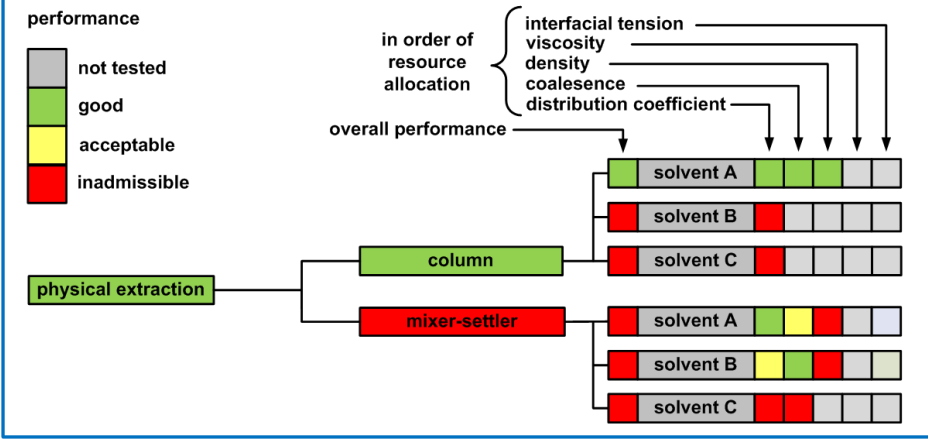
interfacial tension

viscosity

density

coalescence


distribution coefficient



Bednarz, A., Rüngeler, B., Pfennig, A., 2014: Use of Cascaded Option Trees in Chemical-Engineering Process Development, Chemie Ingenieur Technik 86 (5)

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Conclusion



- use of uncertainties as additional information to process
- support for process engineer by systematic resource allocation
- remaining uncertainties at each step of process development visible
- framework for design of solvent extraction under uncertainties

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Thank you for your attention.

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- Berkelmans, I., 2010: *Development and Application of a Framework for Technology and Model Selection Under Uncertainty*. Dissertation, Massachusetts Institute of Technology.
- Biegler, L. T., Grossmann, I. E., Westerberg, A. W., 1997: *Systematic methods of chemical process design*. Upper Saddle River, N.J. Prentice Hall PTR.
- Guthrie, K. M., 1969: *Capital cost estimating*. *Chemical Engineering* (March 24), 114–142.