

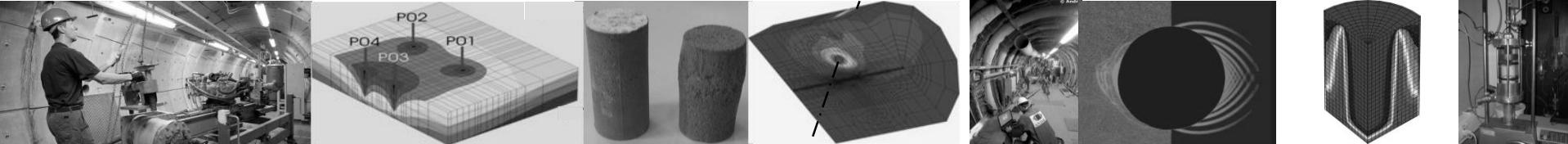
University of Liège – Department ArGENCo

2014 – 2015

Numerical modeling of the long term behavior of Municipal Solid Waste in a landfill

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30th of January 2015
Julien Hubert

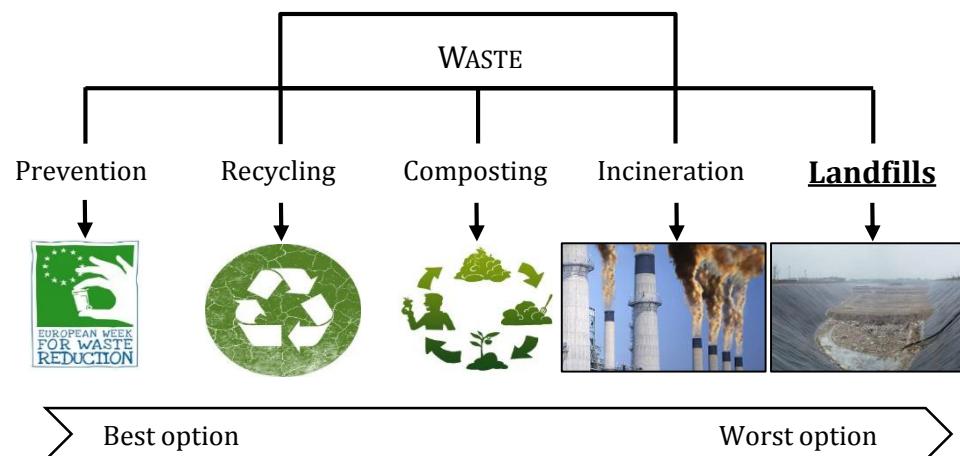


SUMMARY OF THE PRESENTATION

- Introduction to the waste management issue
- THBCM multi-physics model
 - Hydraulic model
 - Bio-chemo model
 - Thermal model
 - Mechanical model
- Test simulation and results
- Conclusion

WASTE MANAGEMENT ISSUE

- Waste production ↑ { Demographic explosion
Over – Consumption
 - It has to be taken care of :



- One of the key point of the waste management issue
 - Objective : optimal post closure management

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HYDRAULIC MODEL

- MSW behave like an unsaturated soil :

$$\frac{\partial(\rho_w n S_{r,w})}{\partial t} + \operatorname{div}(\rho_w \underline{f}_w) = Q$$

f_w is the Darcy's flow given by the following equation:

$$\underline{f}_w = -\frac{k_w(S_{r,w})}{\mu_w} (\operatorname{grad}(p_w) + \rho_w \cdot g \cdot \operatorname{grad}(y))$$

HYDRAULIC MODEL

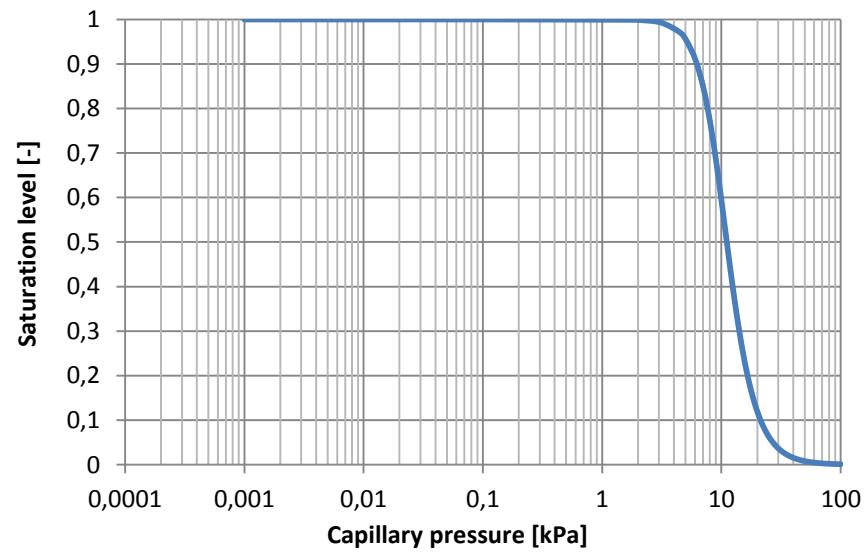
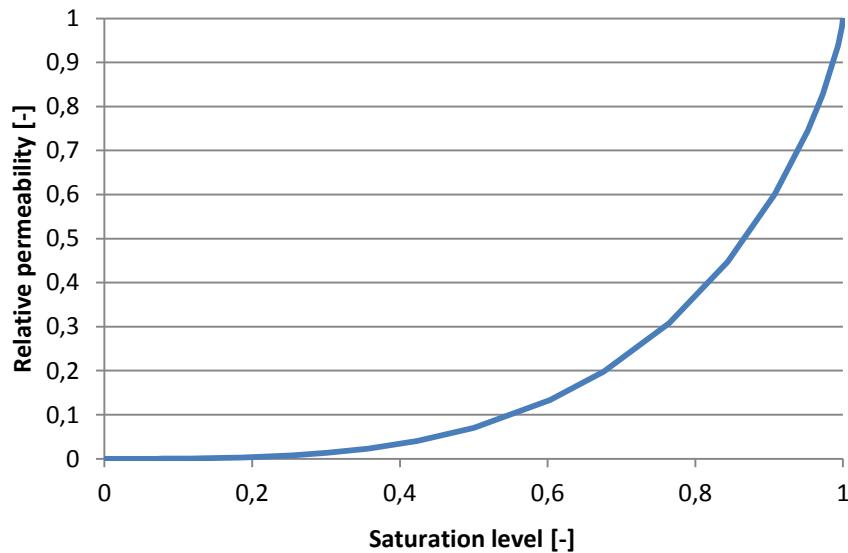
Relative permeability and water retention curves (van Genuchten):

Relative permeability

$$k_{rel} = \sqrt{S_{r,w}} \left[1 - \left(1 - S_{r,w}^{\frac{1}{m_{vG}}} \right)^{m_{vG}} \right]^2$$

Water retention

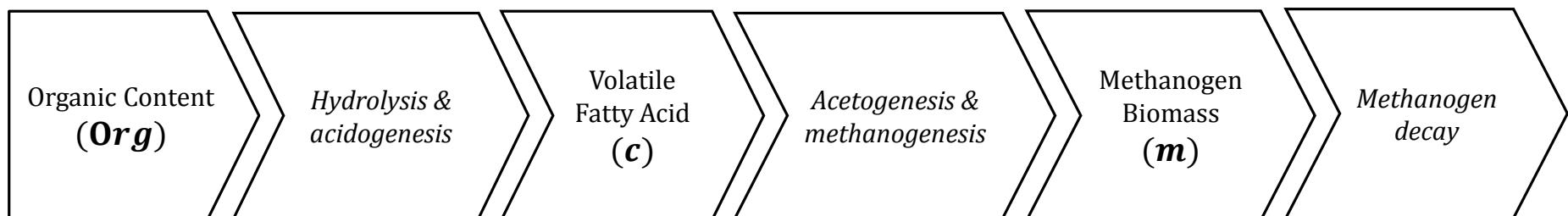
$$S_{r,w} = S_{res} + (S_{sat} - S_{res}) \left[\left(1 + \frac{p_c}{\alpha} \right)^{n_{vG}} \right]^{-m_{vG}}$$



BIO-CHEMICAL MODEL

- Can be split into two main stages :
 - Aerobic stage \Rightarrow neglected
 - Anaerobic stage

It is assumed it can be simplified :



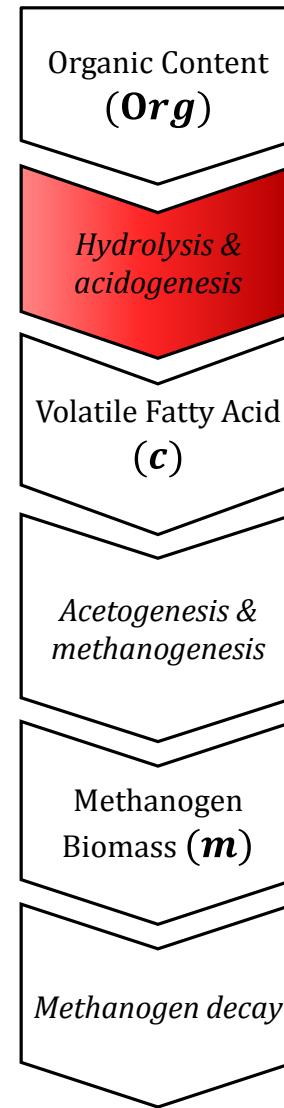
BIO-CHEMICAL MODEL

- McDougall's formulation:
 - Hydrolysis and acidogenesis
 - Acetogenesis and methanogenesis
 - Methanogen decay

$$r_g = b\theta_e \phi P$$

$$r_j = \frac{k_0 c}{k_{MC} + c} m$$

$$r_h = \frac{r_j}{Y}$$



$$r_k = k_2 m$$

BIO-CHEMICAL MODEL

- McDougall's formulation:

- Hydrolysis and acidogenesis

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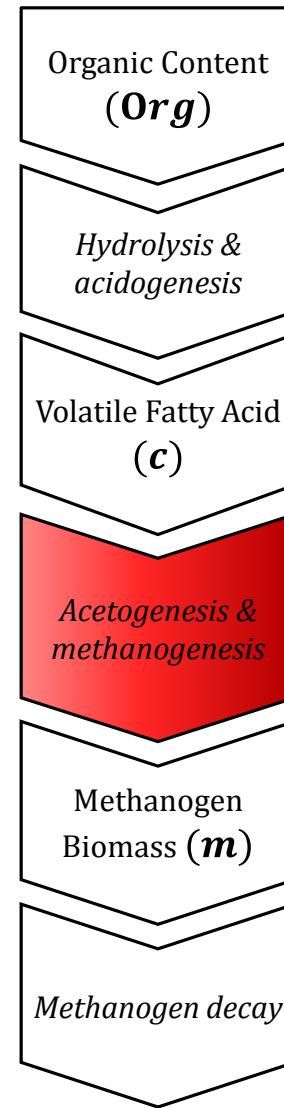
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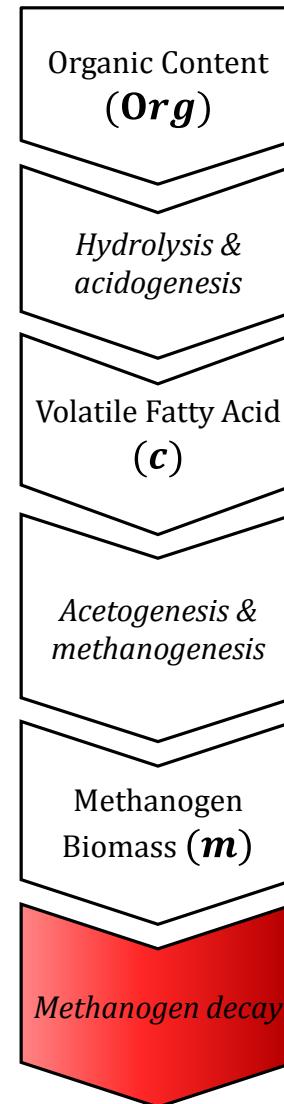
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BIO-CHEMICAL MODEL

- Governing balance equations taking into account transport phenomena:

Variable	Balance equation
Organic Matter (<i>Org</i>):	$-\theta Z r_g = \frac{\partial Org}{\partial t}$
VFA (<i>c</i>):	$div(u.c) - div(D_h \nabla c) + [r_g - r_h] = \frac{\partial c}{\partial t}$
MB (<i>m</i>):	$div(u.m) - div(D_h \nabla m) + [r_j - r_k] = \frac{\partial m}{\partial t}$

Thermal model

- The degradation of the organic matter is an exothermal reaction
- Classical heat storage and diffusion model :

$$\dot{S}_T + \operatorname{div}(V_T) - Q = 0$$

$$V_T = -\Gamma \nabla T + c_{p,w} \rho_w \underline{f_w}(T - T_0)$$

- Heat generation term based on the variation of the organic content :

$$Q = \frac{\Delta Org(t)}{\Delta t} Q_m$$

Mechanical model

- The degradation of the organic matter is going to modify the mechanical properties of the MSW
- Chemo-Hydro-Mechanical model introduced by Liu & *al*

$$\dot{\varepsilon}_{ij} = \dot{\varepsilon}_{ij}^e + \dot{\varepsilon}_{ij}^p$$

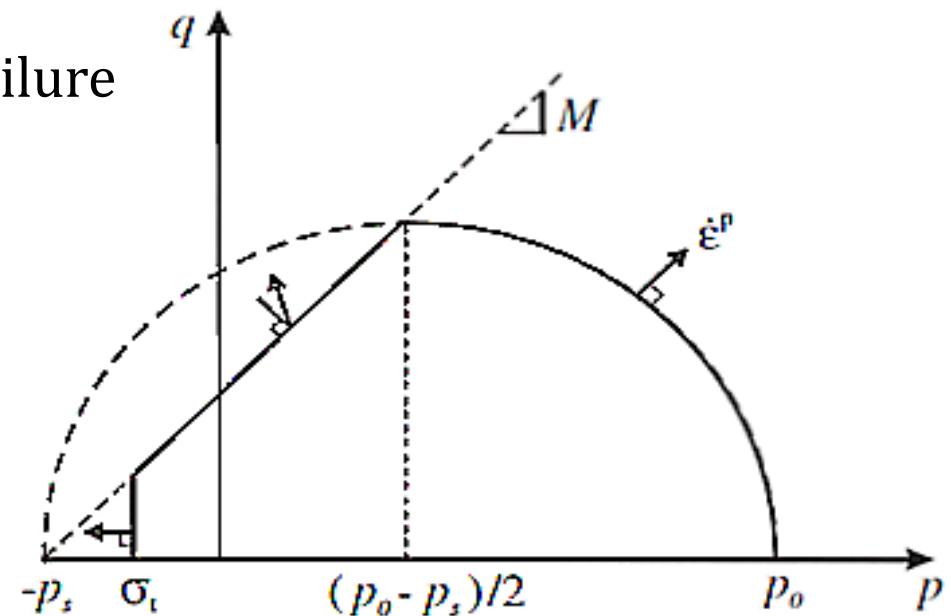
- Classical elastic stress-strain relationship
- The plastic strain rate is defined within the boundaries of the yield criterion:

$$f(\sigma_{ij}, \kappa) \leq 0$$

Mechanical model

- Three plastic yielding mechanisms are implemented into the CHM:

- pore collapse
- frictional-cohesive failure
- tensile failure



Mechanical model

- The degradation of the organic matter induces hardening/softening :

- “Concentration” parameter :

$$\alpha = 1 - \frac{Org}{Org_0}$$

- Effect of the concentration on the yield surface:

$$p_0(\alpha) = p_0^* S(\alpha)$$

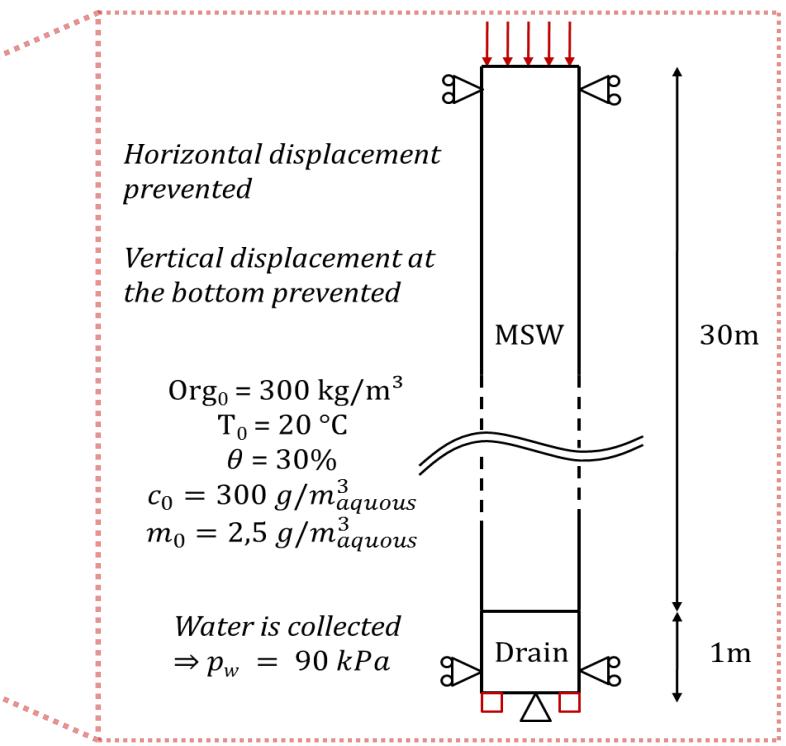
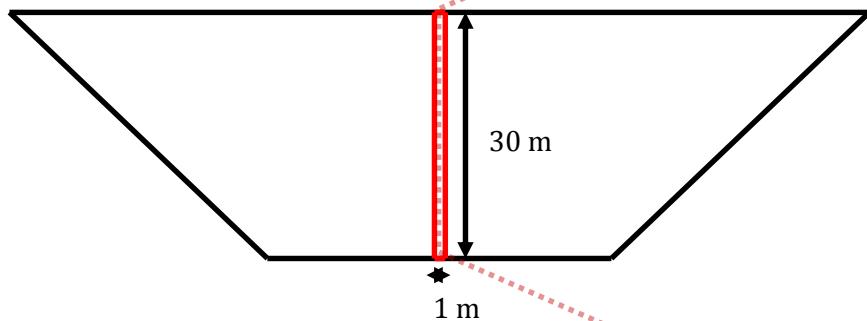
$$p_s = p_s^* + k_{OC} \alpha$$

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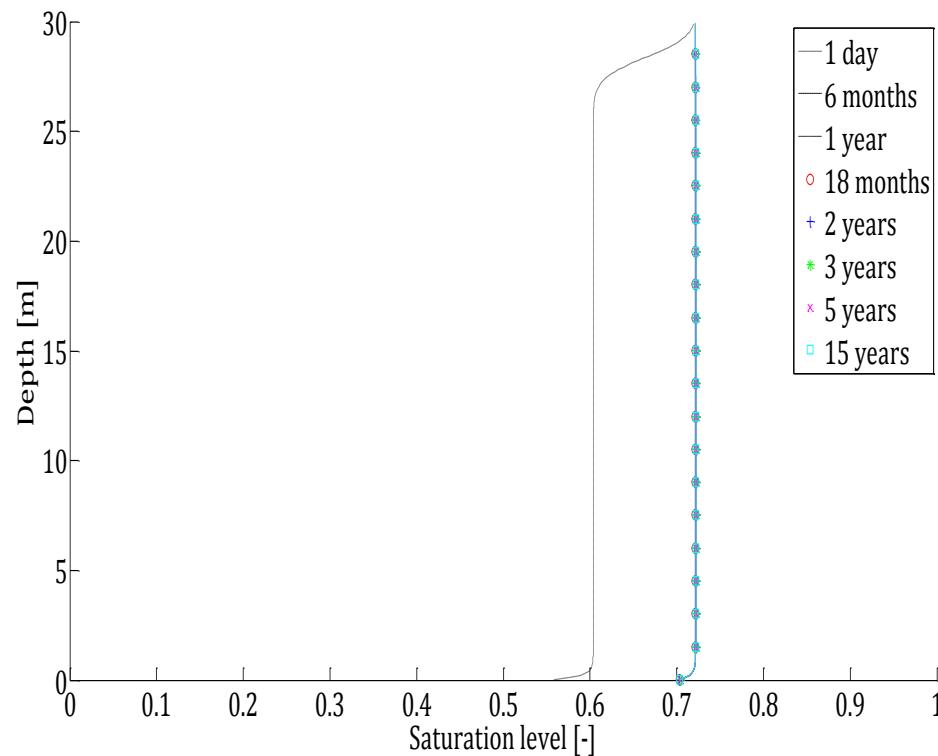
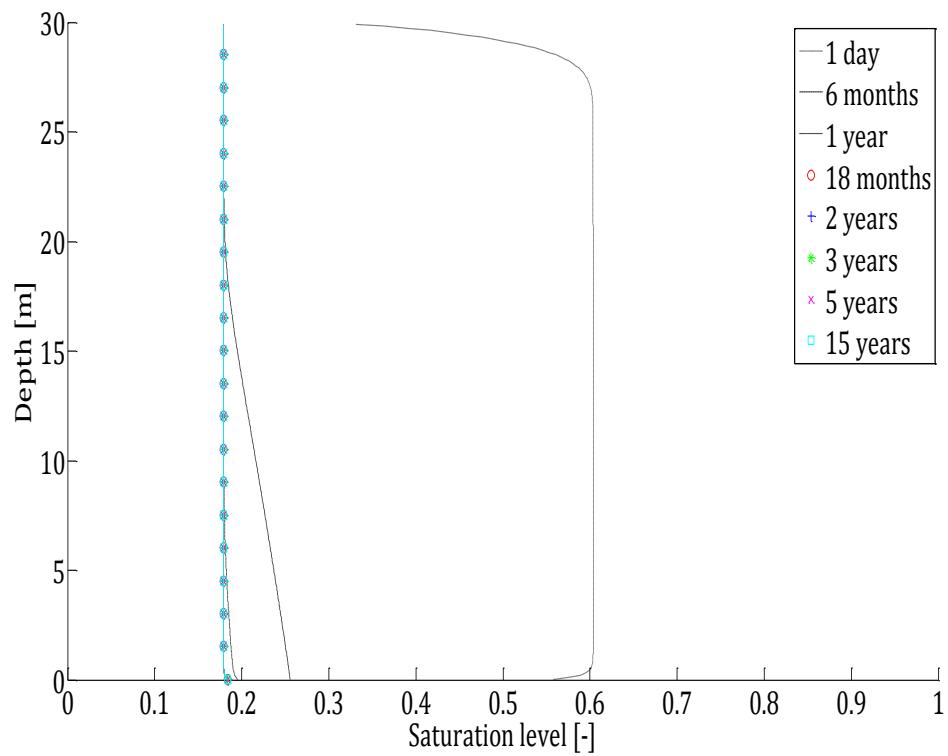
Geometry and initial/boundaries conditions

- Goal : Assess the performance and validity of the model
- Very simple 1D geometry



Hydraulic results

$$\nearrow Q = 2,5 * 10^{-8} m^3/s \quad \text{Injected water flux} \quad Q = 2,5 * 10^{-6} m^3/s$$



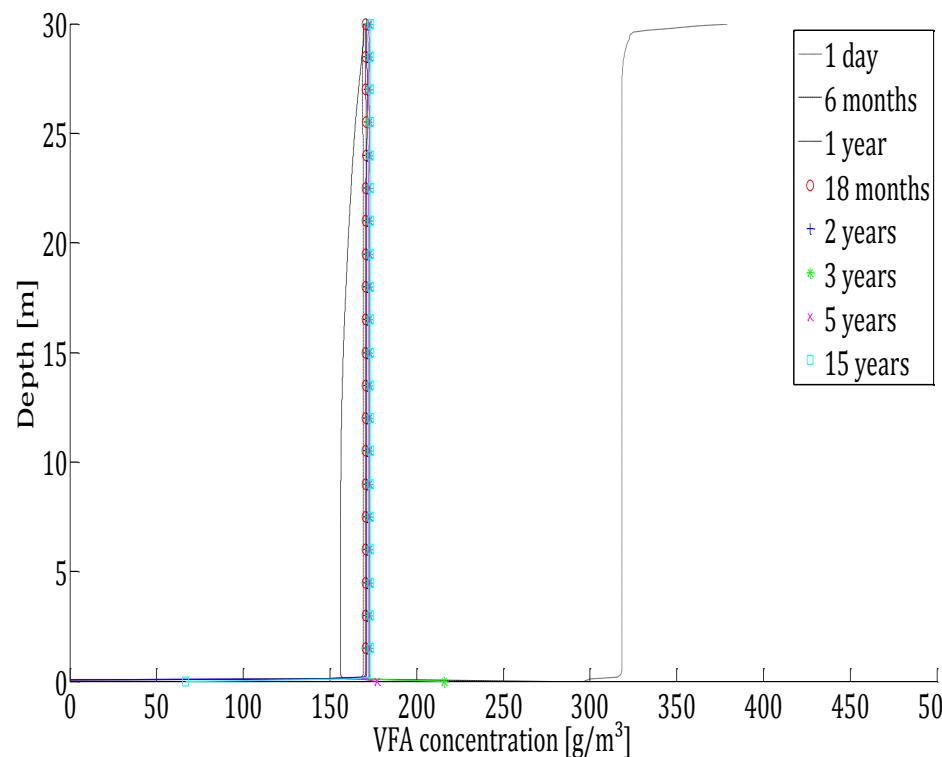
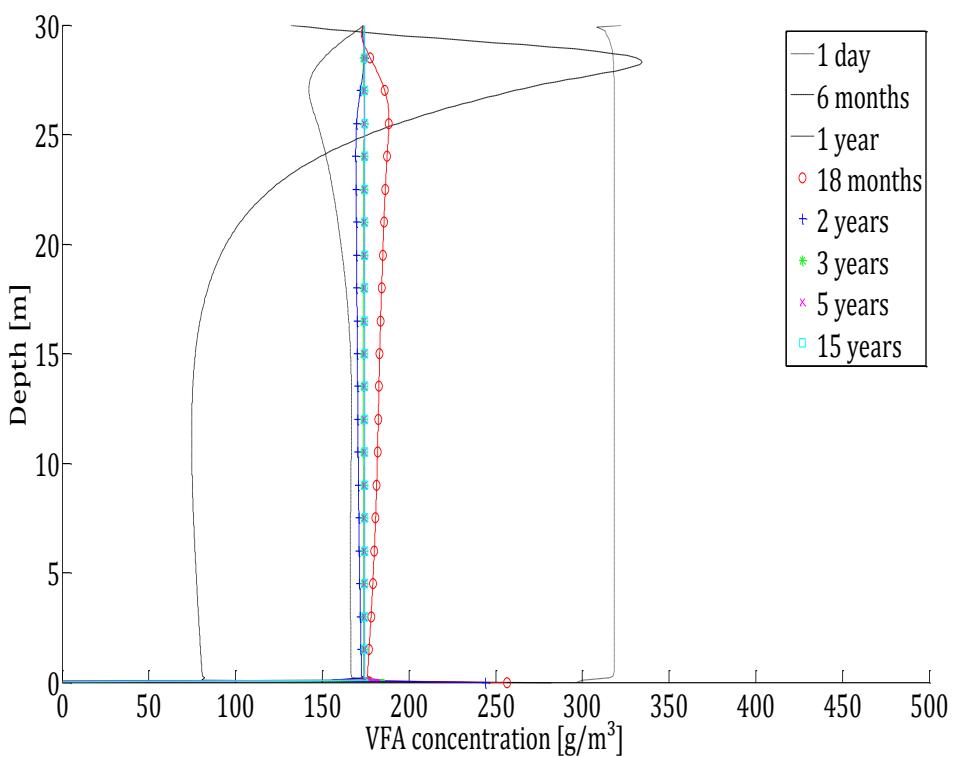
Hydraulic parameters based on *Manassero & al (1996)*; *Olivier & al (2007)*; *Staub & al (2009)* and *Feng & al (2014)*

Bio-chemical results

$$\nearrow Q = 2,5 * 10^{-8} m^3/s$$

Injected water flux

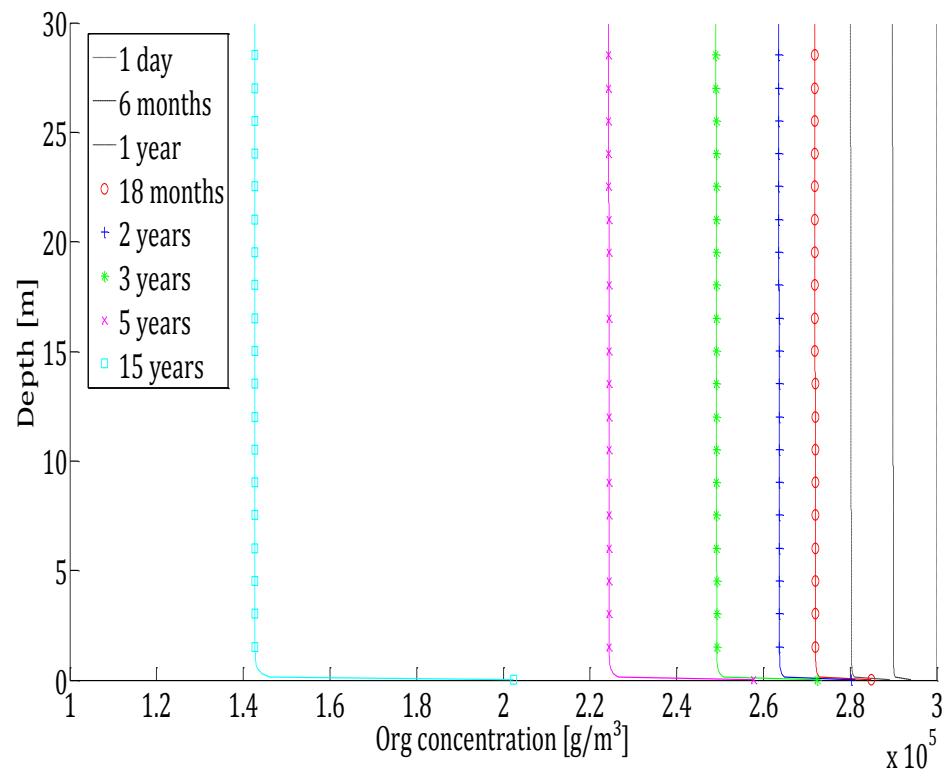
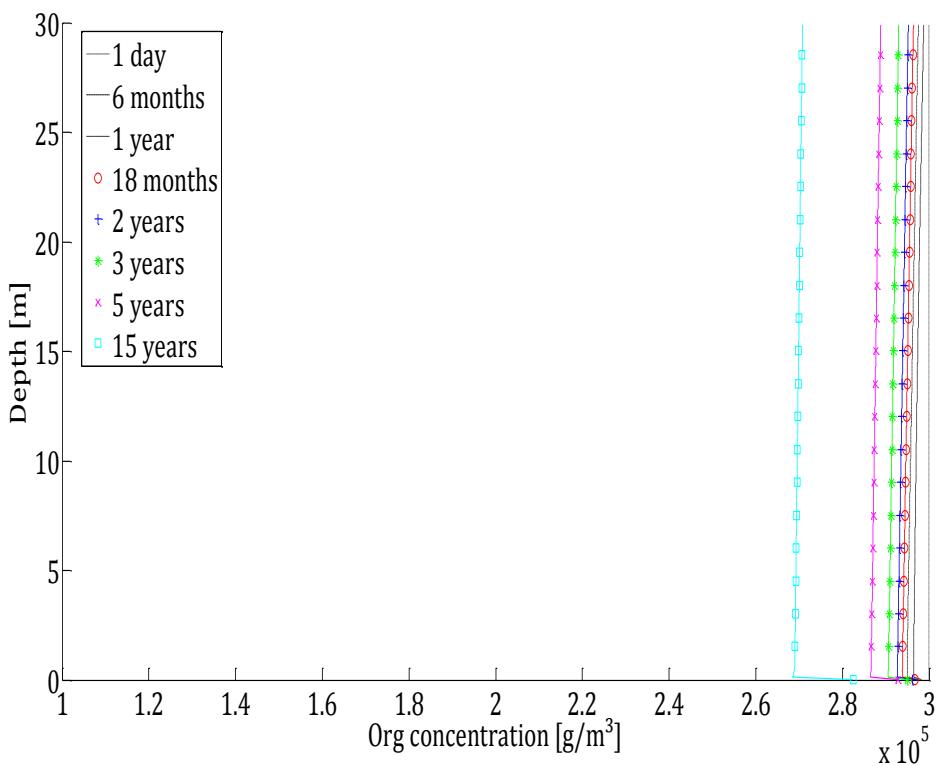
$$Q = 2,5 * 10^{-6} m^3/s$$



Transport parameters based on Domenico & al (1998) and Cooke & al (2008). Biodegradation parameters based on McDougall (2007)

Bio-chemical results

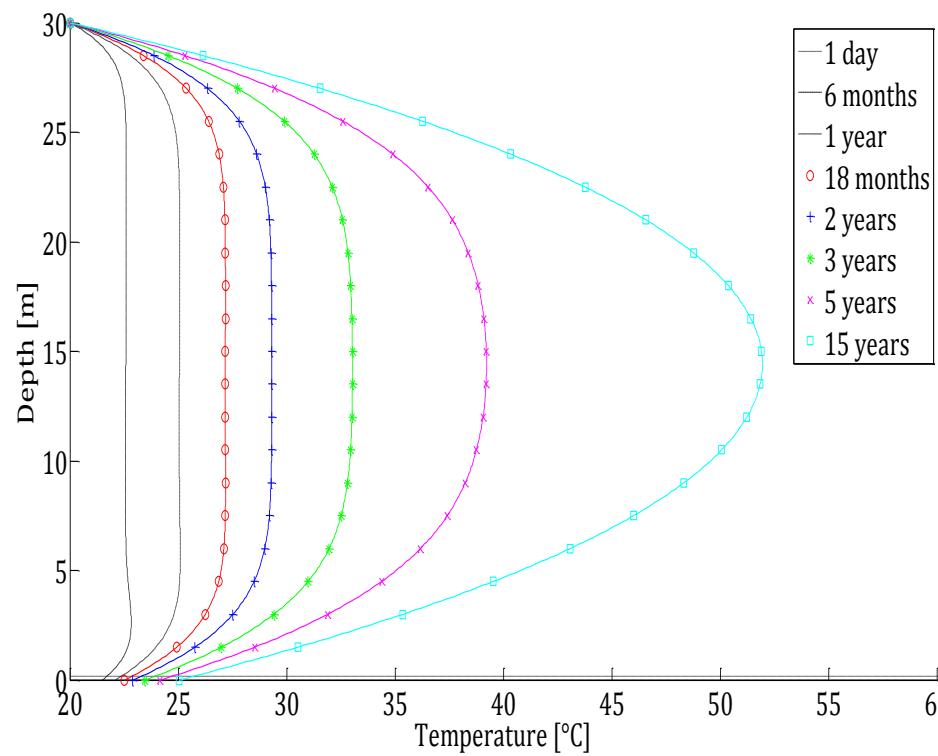
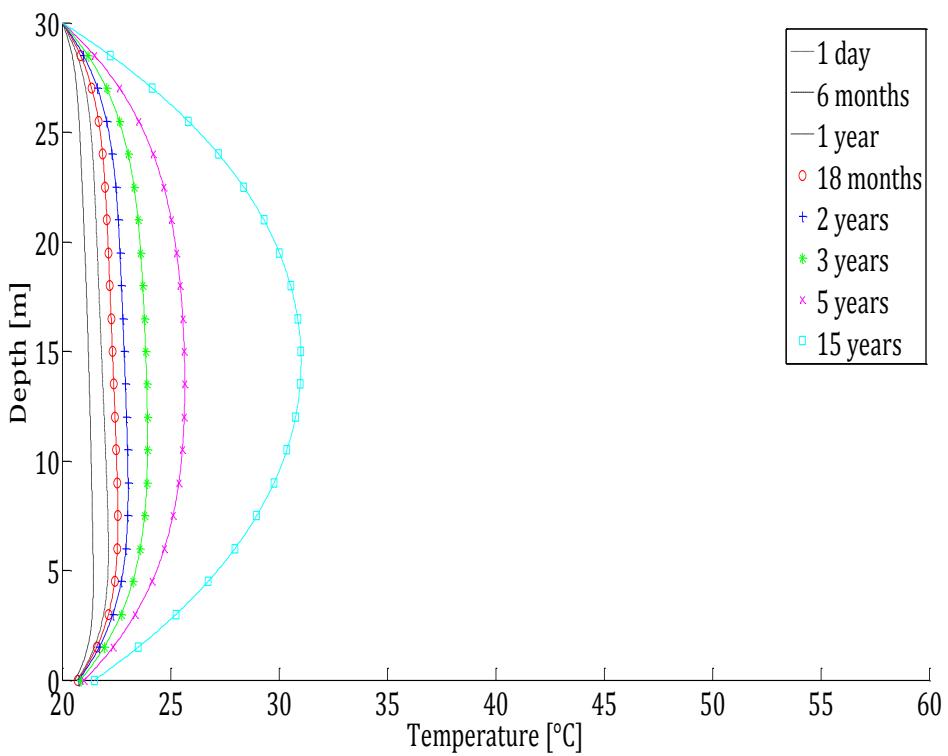
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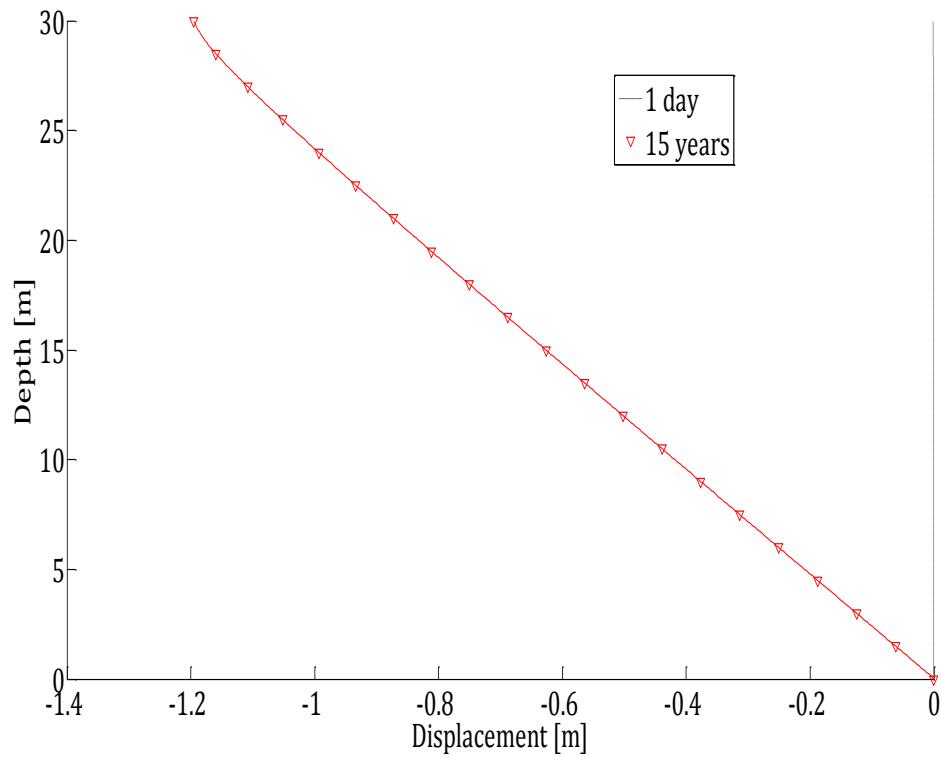
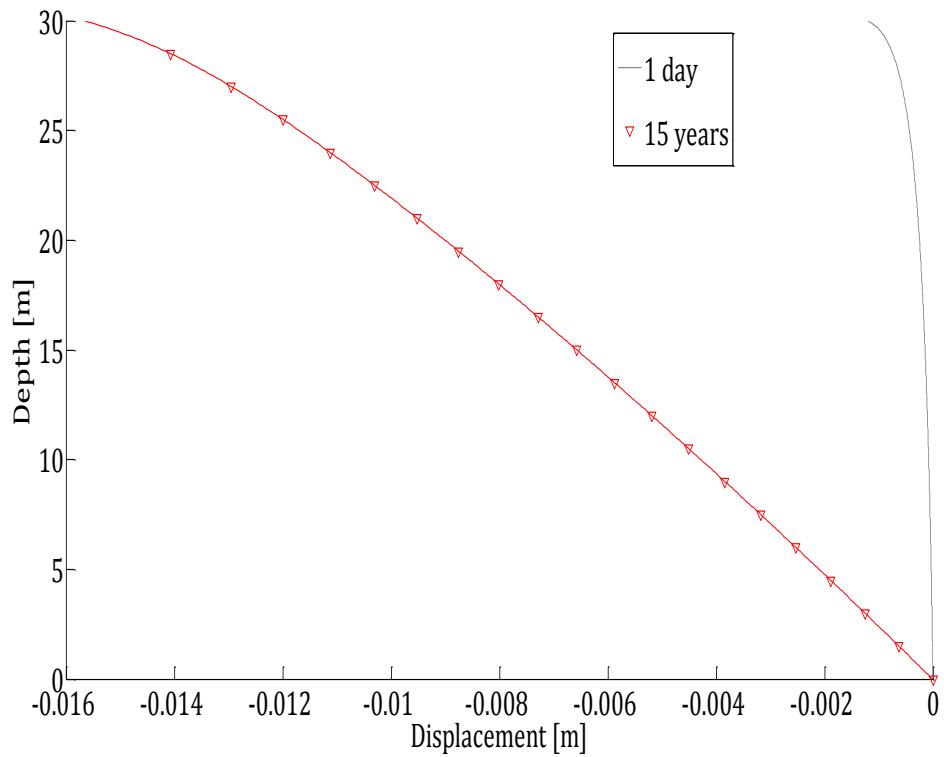
$$\nearrow Q = 2,5 * 10^{-8} m^3/s \quad \text{Injected water flux} \quad Q = 2,5 * 10^{-6} m^3/s$$



Heat transfert parameters based on *Yoshida & al* (1999) and heat production parameters based on *Boukpeti & al* (2004)

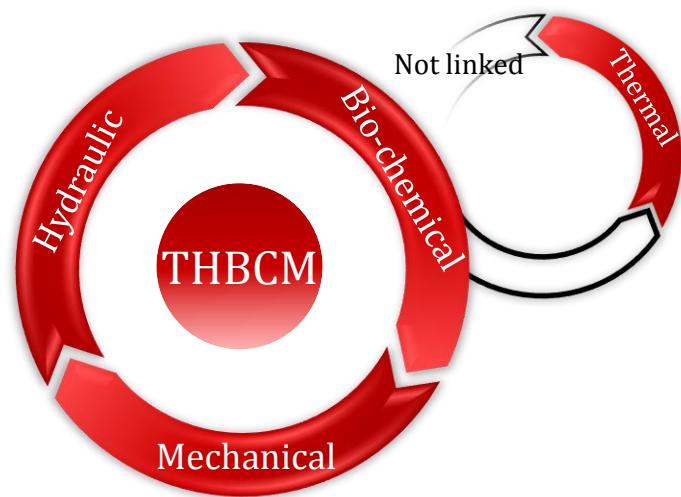
Mechanical results

$\sum Q = 2,5 * 10^{-8} m^3/s$ Injected water flux $Q = 2,5 * 10^{-6} m^3/s$



Conclusion

- Results linked to the hydraulic equilibrium reached
- Can work on any given geometry
- Thermal model not fully linked



- Effective to assess settlements
- Effective tool for pollution potential evaluation

Questions