

Determination of Moisture Diffusivity during Drying of Mortar Cement: Experimental and Modeling Study

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Abstract The aim of this study is the experimental characterization of the behaviour of a mortar during convective drying. We focalise on mortar that has a rate water-cement of 0.5. The drying tests are developed in a micro-convective dryer that can use samples weighing from 0 to 8g. The advantage of these experiments is to reproduce the natural conditions that can be found during the treatment of the mortar-atmosphere problems. The response of the drying curve or the drying kinetic depends on the applied drying conditions. So, the temperature of the air varies from 60°C to 130°C, the velocity of the air is changed from 2 m.s⁻¹ to 5 m.s⁻¹ and the relative humidity is kept less than 1.7%. The comparison between the experimental results and the proposed analytical solutions of the equation of diffusion represented by Fick's law, applied for a finite shape, allows determination of the values of the diffusion coefficient. It has a value of $1.71 \times 10^{-10} \text{ m}^2 \cdot \text{s}^{-1}$ at 60°C, $13.69 \times 10^{-10} \text{ m}^2 \cdot \text{s}^{-1}$ at 90°C and $16.27 \times 10^{-10} \text{ m}^2 \cdot \text{s}^{-1}$ at 130°C. Calculation of the activation energy and the D_0 constant are also possible.

Keywords Thermal Energy, Convective Drying, Diffusion Coefficient, Operating Conditions

1. Introduction

Materials based on cement, such as mortar, and cement pastes are still widely used in several construction sectors such as buildings and road constructions. This intensive use of mortar cement is due to its good mechanical properties, low cost but also can be reported to its durability which is one of the important parameters. The knowledge of the micro-structural changes and the interaction between water and solid, in particular during drying process, is one of the keys for durability studies of cement products. The application of non-controlled conditions can lead to the appearance of shrinkage, deformations and cracks, as it is reported in many studies[1-4]. So, deep studies dealing with happening transfers during the process could be necessary to have a final marketable material. Several works are focused on studying heat and mass transfer during drying of different materials, such as Gypsum board and wood[5], Bricks, plasters and stones[6] and the effect of the operating conditions[5] with determination of the moisture profile[6] and the drying kinetic changes[7]. The effect of the application of other parameters such as pressure[8], external wind velocity[9] and application of constraint stress[10] are

also studied. For mathematical modeling, two approaches are generally used; the first is by considering the materials as a porous media. In this first approach, heat and mass balances are applied for the different components of the material represented by gas, and solid phases[11-13]. It allows following, for the two phases, the variations of the humidity and the temperature of the media. The second approach consists on the use of the equation of diffusion. Numerous solutions and approximations of this equation are proposed leading to easily have the moisture profile inside the material and its variation with time. Diffusion coefficient is the most important parameter that can be calculated using this approach[14-19].

The objective of this work is the determination, based on experiments, of the moisture evolution during convective drying of a sample of mortar cement, the effect of the operating conditions on this profile and finally the calculation of the diffusion coefficient using analytical solutions of diffusion equation.

2. Materials and Methods

Samples are prepared at the Laboratory of Building Materials of the University of Liege. The samples are kept in a climatic room at 20.1°C and 90% relative humidity (according to the recommendations of CEN[20]), until their utilization.

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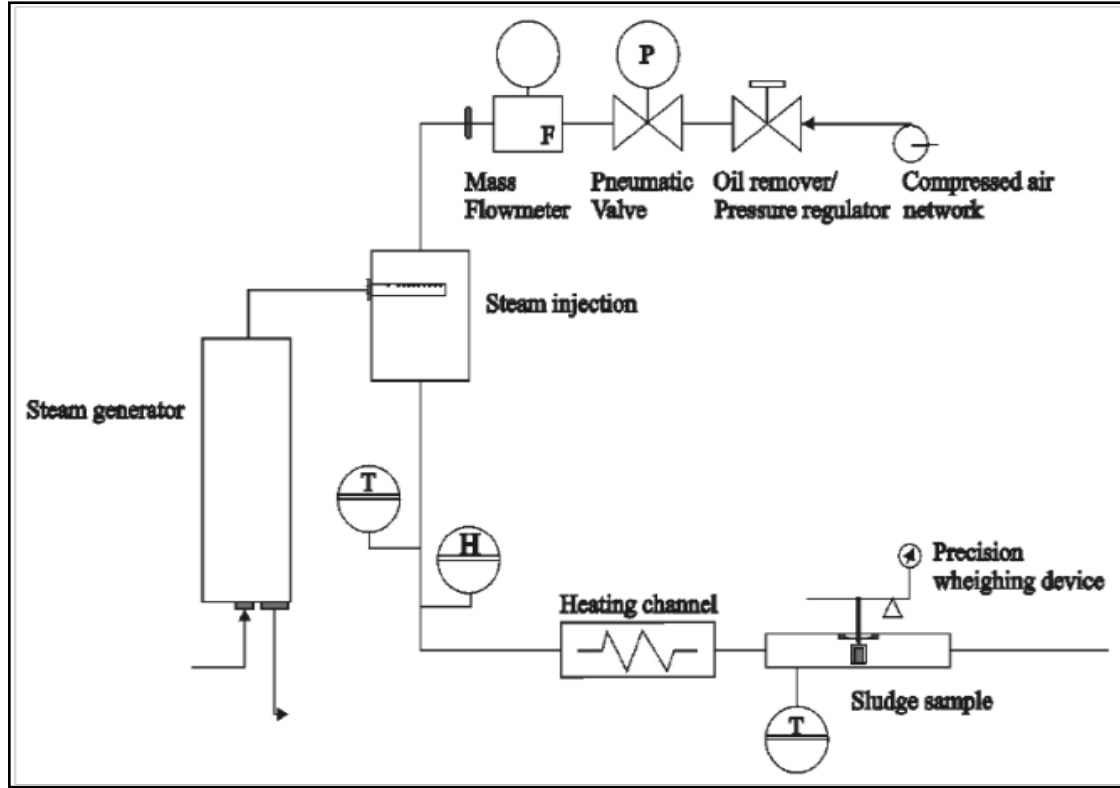


Figure 1. Detailed scheme of the convective dryer[22]

The mortar is constituted of three components: one part of Ordinary Portland Cement, three parts of normalized sand that contains 98% of silica and a half part of water. The Water to Cement ratio is 0.5. The mix portions are presented in Table 1.

The samples have a cylindrical shape with a diameter of 13mm and a height of 17mm.

Table 1. Mix portions of the mortar

Component	Reference	Weight (g)
Sand	EN 196	1350.5
Cement	CEM I 52.5 R HES	450.2
Water	Tap water	225.1
Water/Cement ratio = 0.5		

2.1. Presentation of the Drying System

Drying tests are realized in a micro-convective dryer that can dry small samples whose weight cannot exceed 8g. The micro-dryer was initially developed to undertake samples of wastewater sludge[21]. A representative schema of the convective dryer is shown in Figure 1. The micro-dryer is divided into two parts: the air conditioning and feeding system and the drying chamber. Air is fed from the laboratory compressed air network. A pneumatic valve connected to a mass flowmeter controls the flow rate. The air can be humidified or heated by passing through respectively the steam generation zone or the heating channel. Then the air is directed to the drying chamber. So, the air humidity, temperature and flowrate are continuously controlled. Inside the drying chamber, the sample is linked to a precision weighing device (BP 150 from Sartorius, accuracy: 0.001 g)

connected to a PC that records the mass of the sample. The micro-dryer can operate between 20°C and 180°C and from 0.3 m.s⁻¹ to 5 m.s⁻¹.

3. Mathematical Modeling

As exposed previously, moisture profile of a building material during drying can be well described using Fick's law represented by the equation of diffusion written under the following form, for an unsteady state and one dimensional case:

$$\frac{\partial X}{\partial t} = D_{eff} \left(\frac{1}{y^n} \right) \left(\frac{\partial}{\partial y} \right) \left[y^n \frac{\partial X(y,t)}{\partial y} \right] \quad (1)$$

"n" takes the value of "0" for a plate, "1" for a cylinder and "2" for a sphere. Crank[23] proposed analytical solutions of this equation for various applied conditions and for multiple dimensional studies. But due to the complexity of the proposed solutions some simplifications are generally used, such as considering the sample having an infinite shape.

For convective conditions, the solution for an infinite plate is written:

$$X^* = \sum_{n=1}^{\infty} \frac{2 \sin^2 \lambda_n}{\lambda_n (\lambda_n + \sin \lambda_n \cos \lambda_n)} \exp(-\lambda_n^2 Fo) \quad (2)$$

Where λ is given by:

$$Bi = \lambda_i \tan \lambda_i \quad (3)$$

"Fo" is Fourier dimensional number

For an infinite cylinder and convective drying conditions, the solution of the diffusion equation is written:

$$X^* = \sum_{n=1}^{\infty} \frac{4 J_1^2(\lambda_n)}{J_0^2(\lambda_n) + J_1^2(\lambda_n)} J_0 \left(\lambda_n \frac{r}{R} \right) \exp(-\lambda_n^2 Fo) \quad (4)$$

With:

$$Bi = \lambda \frac{J_1(\lambda)}{J_0(\lambda)} \tag{5}$$

In our case, it is clear that the value of the diameter of the sample is almost equal to its height. So, we cannot consider the sample as an infinite cylinder or as an infinite plate. One of the proposed approaches to study finite dimensions is the method called super-imposition technique[24-27]. It considers the solution for a finite cylinder as the product of the infinite slab and the infinite cylinder.

Crank[23] has proposed another solution of the diffusion equation, this solution is reported and use by other authors[28-29]. The solution can be written:

$$X^* = \frac{X}{X_0} = \frac{8r^2}{l^2} \sum_{i=1}^n \sum_{j=1}^n \frac{1}{\lambda_i^2 \beta_j^2} \exp[-(\lambda_i^2 + \beta_j^2)] \frac{D_{eff}}{r^2} t \tag{6}$$

With:

$$\beta_j = \frac{(2j-1)}{2l} \pi r \tag{7}$$

λ_i is the root of the Bessel function.

For long drying times ($X^* < 0.6$) only the first term of the series solution is taken into account and it gives:

$$X^* = \frac{32}{\lambda_1^2 \pi^2} \exp[-(\lambda_1^2 + \beta_1^2)] \frac{D_{eff}}{r^2} t \tag{8}$$

The plot of the experimental results in term on $-\ln(X^*)$ versus drying time gives a straight line with a slope:

$$slope = (5.7831 + \beta_1^2) \frac{D_{eff}}{r^2} \tag{9}$$

4. Results and Discussion

The experiments are realized under temperatures of 60°C, 90°C and 130°C. Increased velocities of 2 m.s⁻¹, 3 m.s⁻¹ and 5

m.s⁻¹ are also used. The relative humidity of the air is less than 1.7%.

Drying process is well represented by the drying curve that gives information about the variation of the moisture content inside the product with time. Figure 2 shows the general trend of the curves with the influence of the operating conditions.

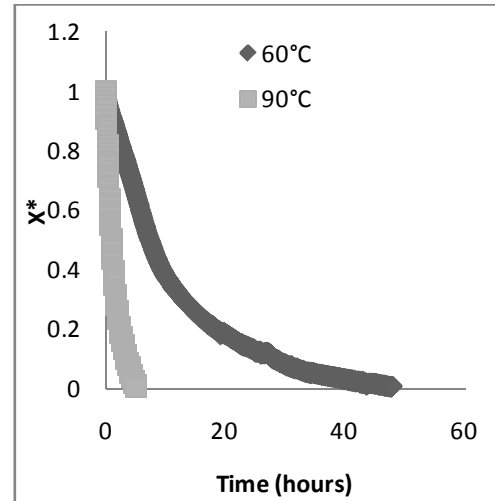


Figure 2. Drying curves during drying of mortar cement

X^* is the dimensionless moisture. It is equal to the ratio of the actual moisture content to the initial moisture content.

As shown in the figure, the quantity of water existing in the product decreases with time. On the other hand, increasing energy (represented by air temperature increase) is considerably reducing drying time.

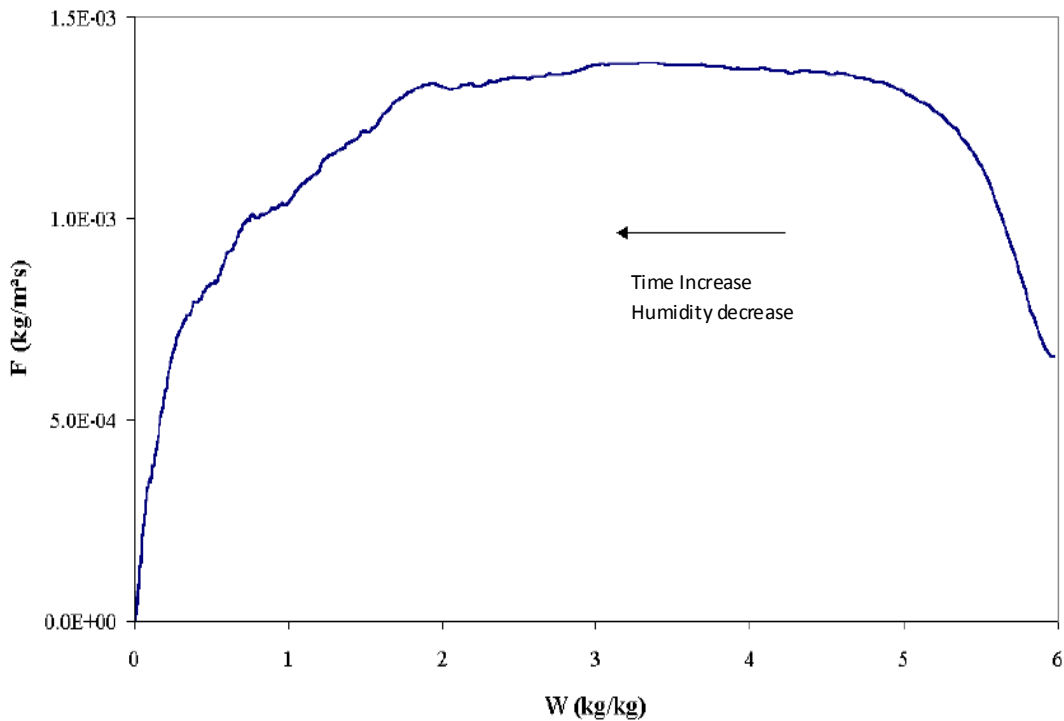


Figure 3. Krisher's curve[21]

Generally, convective drying process passes by several phases, commonly divided into 3 phases. The first phase; is a short period called adaptation period. During this phase, the product adapts its comportment to the new applied conditions. The second period is also called constant drying rate period, provided no shrinkage occurs. During this period the supplied heat serves essentially to the evaporation of the product water. The operation is done at constant surface product temperature. The last phase is the falling drying rate period. In this last period, the energy serves both to evaporate the product water and to increase its temperature. The best representation allowing illustrating the different drying phases is the so-called Krisher's curve, i.e. the drying rate, or flux, versus the product water content. Figure 3 gives Krisher's representation in the case of wastewater sludge drying[21].

Determining the influent parameters that affect drying plays an important role to have an optimum procedure. According to previous studies done for food stuffs[31-32], wastewater sludge[30] and some building materials[19]; temperature of the air and its velocity are found as the most influent parameters. Figures 4 and 5 show the influence of respectively the temperature of the heated air and its velocity on the drying kinetics for mortar samples. The experimental results of figure 4 are obtained at a velocity of 2 m.s⁻¹. Those of figure 5 are obtained at a temperature of 130°C.

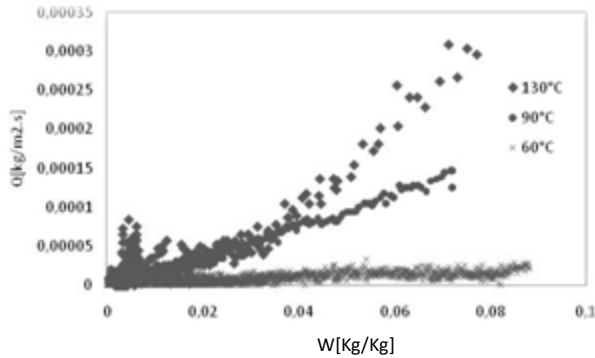


Figure 4. Influence of the air temperature on the total evaporated water

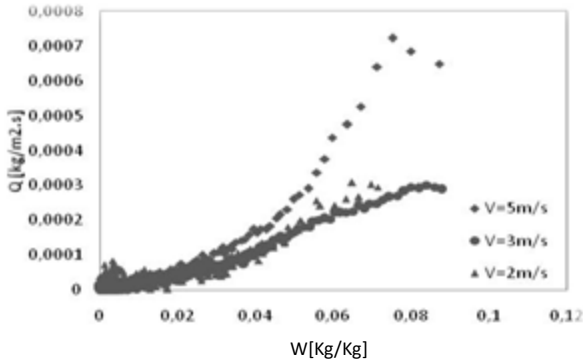
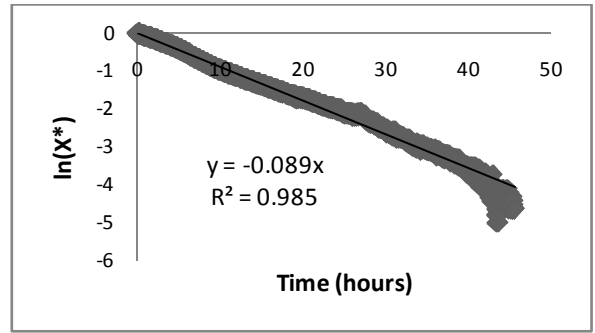


Figure 5. Influence of the air velocity on the total evaporated water

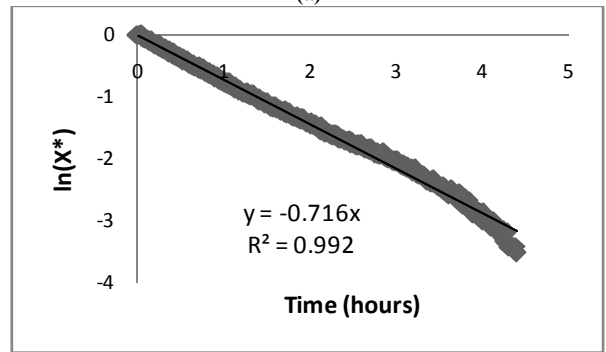
The two figures show the existence of the adaptation phase, the short constant drying rate period and a dominant falling drying rate phase. It is clear that increasing the temperature or the velocity of the air increases transfer and in

consequence the increase of the quantity of the evaporated water. For the same drying time, the quantities have been doubled values when the temperature increased from 90°C to 130°C and also when the velocity was increased from 3 m.s⁻¹ to 5 m.s⁻¹. It is important to note that surface change was followed using microtomography and it was found that it remained constant; i.e. no shrinkage was observed.

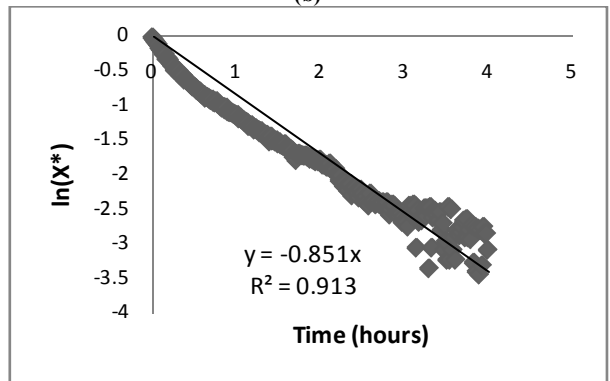
4.1. Determination of the Diffusion Coefficient



(a)



(b)



(c)

Figure 6. Variation of the moisture with time for different temperatures. (a):60°C, (b): 90°C, (c)=130°C

The plots of the experimental results as ln(X*) vs. time, for different temperatures, are shown in Figure 6.

The results of the comparison of the experimental results and equation 9 give the values of the diffusion coefficient for different temperatures summarized in table 2:

Table 2. Influence of the temperature on diffusion coefficient

Temperature (°C)	60	90	130
D _{eff} (m ² .s ⁻¹)*10 ¹⁰	1.71	13.69	16.27

The relation is written under the following form:

$$D_{eff} = D_0 \exp\left(-\frac{E}{RT}\right) \quad (10)$$

R is the perfect gas constant, it is equal to 8.314 J/ K..mol).

The plot of $\ln(D_{eff})$ vs. the inverse of the temperature is illustrated in figure 7.

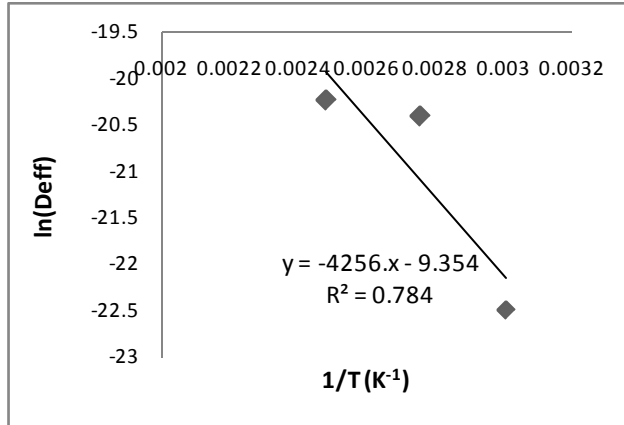


Figure 7. Determination of the coefficient diffusion parameters

An activation energy of about 35.39 kJ.mol⁻¹ is then obtained and the value of the constant D₀ is ln(D₀) = -9.3546

Table 3 presents the results of the diffusion coefficient calculus presented by other works and for several building materials.

Table 3. Values of diffusion coefficient for different materials

Material	D _{eff} (m ² /s)	Reference
Hemp concrete	0.82 *10 ⁻⁹	[33]
Cellular concrete	4.5*10 ⁻⁹ – 6.7*10 ⁻⁹	[12]
Lime binder	2.0*10 ⁻⁹ – 3.5*10 ⁻⁹	[12]
Clay Brick	2.0*10 ⁻¹⁰ – 3.0*10 ⁻¹⁰	[14]
Brick	18.75*10 ⁻⁹ – 7.16*10 ⁻⁹	[19]

The studied product shows a diffusion coefficient higher than hemp concrete and clay brick and lower than cellular concrete, lime binder and brick.

5. Conclusions

The experiments permit to have more information about drying of cement mortar with study of the influence of the operating conditions which are commonly, the temperature and the velocity of the air. During application of drying to cement mortar three phases can be identifiable by using Krisher's curve. The use of the microtomography shows that no changes are happening to the samples and a constant surface is registered in all studied cases. It is evident to find that increasing temperature or velocity of the air conducts to the increase of the evaporated quantity of water. The maximum value reached at 60°C is 0.00015 kg.m⁻².s⁻¹, this value increases to 0.00030 kg.m⁻².s⁻¹ at 130°C. On the other side, the increase of the air velocity from 1 m.s⁻¹ to 5 m.s⁻¹ causes an increase of the maximum value from 0.00030 to 0.00070 kg.m⁻².s⁻¹. The modelling part of this work allows calculation of the diffusion coefficient. The value of this coefficient increases with temperature from 1.71 ×10⁻¹⁰

m².s⁻¹ at 60°C to 16.27 ×10⁻¹⁰ m².s⁻¹ at 130°C. The constant coefficient and the activation energy are then easily calculated. The activation energy is equal to 35.39 kJ.mol⁻¹.

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Nomenclature

- Bi Biot dimensionless number
- D diffusion coefficient (m²/s)
- E activation energy (J/mol)
- Fo Fourier dimensionless number
- R perfect gas constant (=8.314 J/K..mol)
- r radius (m)
- Q or F evaporation flux (kg/m².s)
- T temperature (°C or K)
- t time (hours)
- X or W moisture content (kg/kg dry basis)
- X₀ initial moisture content (kg/kg dry basis)
- X* dimensionless moisture content
- y dimension (m)

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