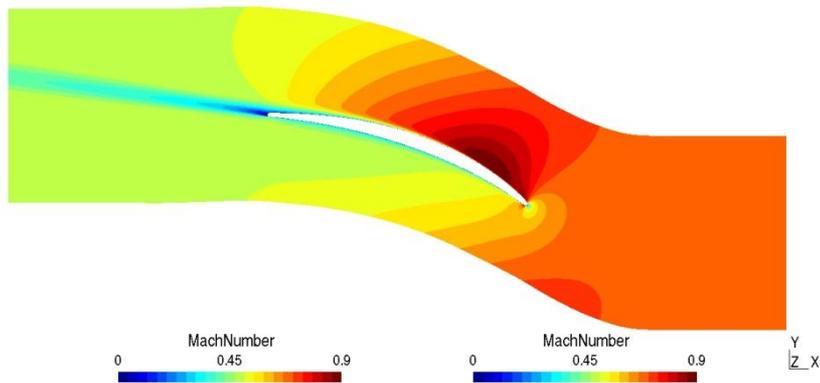


# Application of the discontinuous Galerkin method to 3D compressible RANS simulations of a high lift cascade flow



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- Discontinuous Galerkin method
- Spalart-Allmaras turbulence model
- Stability issues
- Grid convergence: flat plate
- 3D high lift cascade flow

- Convection-diffusion-source equation

$$\frac{\partial u_m}{\partial t} + \mathcal{L}_m(u) = \mathcal{S}_m(u, \nabla u), \quad m = 1 \dots N_v$$

with

$$\mathcal{L}_m(u) = \nabla \cdot \vec{f}_m(u) + \nabla \cdot \vec{d}_m(u, \nabla u)$$

- Variational principle

state function  $\phi_i$   
state variable  $\tilde{u}_m$

$$\begin{aligned} \mathbf{r}_{im} &= (\phi_i, (\mathcal{L}_m(\tilde{u}) - \mathcal{S}_m(\tilde{u}, \nabla \tilde{u})) \\ &= \int_{\Omega} \phi_i \cdot \left( \nabla \cdot \vec{f}_m(\tilde{u}) + \nabla \cdot \vec{d}_m(\tilde{u}, \nabla \tilde{u}) - \vec{S}_m(\tilde{u}, \nabla \tilde{u}) \right) dV. \end{aligned}$$

- Notations

- Jump  $[ ]$  and average  $\langle \rangle$  operator

$$[u] = u^+ \vec{n}^+ + u^- \vec{n}^-$$

$$\langle u \rangle = (u^+ + u^-) / 2$$

- Riemann solver

$$\mathcal{H}(\tilde{u}^-, \tilde{u}^+, \vec{n})$$

- Diffusive flux

$$d_m^k = \sum_{l=1}^d D_{mn}^{kl} \frac{\partial u_n}{\partial x_l}$$

- Interior penalty method

$$\begin{aligned}
 \mathbf{r}_{im} = & - \underbrace{\int_{\mathcal{T}} \nabla \phi_i \cdot \vec{f}_m dV}_{CV} - \underbrace{\int_{\mathcal{T}} \nabla \phi_i \cdot \vec{d}_m dV}_{DV} - \underbrace{\int_{\mathcal{T}} \phi_i \cdot \vec{S}_m dV}_{SV} \\
 & + \underbrace{\oint_{\partial \mathcal{T}} \phi_i \mathcal{H}_m(\tilde{u}^-, \tilde{u}^+, \vec{n}) dS}_{CI} + CBD \\
 & + \underbrace{\oint_{\partial \mathcal{T}} [\phi_i]^k \left\langle D_{mn}^{kl} \cdot \frac{\partial \tilde{u}_n}{\partial x_l} \right\rangle dS}_{DI} + \theta \underbrace{\oint_{\partial \mathcal{T}} [\tilde{u}_n]^k \left\langle D_{nm}^{kl} \cdot \frac{\partial \phi_i}{\partial x_l} \right\rangle dS}_{DT} \\
 & + DBD + DBN \\
 & + \underbrace{\oint_{\partial \mathcal{T}} \sigma[\tilde{u}_m][\phi_i] dS}_{DP} + PBD
 \end{aligned}$$

$\theta = +1$	$\rightarrow$	SIPDG
$\theta = -1$	$\rightarrow$	NIPDG

- Spalart-Allmaras turbulence model
  - One equation model based on empiricism and arguments of dimensional analysis
  - Developed and calibrated for flows like airfoils and wings
  - Working variable  $\tilde{\mu}$  (linear behaviour near the wall)

$$\mu^t = \tilde{\mu} f_{v1}, \quad f_{v1} = \frac{\chi^3}{\chi^3 + c_{v1}^3}, \quad \chi = \frac{\tilde{\mu}}{\mu}$$

$$\frac{\partial \tilde{\mu}}{\partial t} + \frac{\partial(\tilde{\mu} u_j)}{\partial x_j} - \frac{1}{\sigma} \frac{\partial}{\partial x_j} \left[ (\mu + \tilde{\mu}) \frac{\partial(\frac{\tilde{\mu}}{\rho})}{\partial x_j} \right] = Q^{SA}$$

- Source term

$$Q^{SA} = \underbrace{c_{b1}\tilde{\omega}\tilde{\mu}}_{\text{production}} - \underbrace{\rho\left(c_{w1}f_w - \frac{c_{b1}}{c_{\kappa}^2}f_{t2}\right)\left(\frac{\tilde{\mu}}{\rho d}\right)^2}_{\text{destruction}} + \underbrace{\frac{1}{\sigma}\left[\rho c_{b2}\frac{\partial(\frac{\tilde{\mu}}{\rho})}{\partial x_j}\frac{\partial(\frac{\tilde{\mu}}{\rho})}{\partial x_j}\right]}_{\text{diffusion}}$$

$$c_{v1} = 7.1, c_{v2} = 5.0, c_{b1} = 0.1355, c_{b2} = 0.622, \\ c_{w1} = 3.2391, c_{w2} = 0.3, c_{w3} = 2.0, c_{\kappa} = 0.41, \sigma = 2/3$$

- Production term:  $\rho c_{b1}(1 - f_{t2})\tilde{\omega}\tilde{\nu}^*$

Modified vorticity :  $\tilde{\omega} = |\omega| f_{v3} + \frac{\tilde{\nu}^*}{c_{\kappa}^2 d^2} f_{v2}$

$$f_{v2} = \left(1 + \frac{\chi}{c_{v2}}\right)^{-3} \quad f_{v3} = \frac{(1 + \chi f_{v1})(1 - f_{v2})}{\chi}$$

- Destruction term:  $-\rho \left( c_{w1} f_w - \frac{c_{b1}}{c_{\kappa}^2} f_{t2} \right) \left( \frac{\tilde{\nu}^*}{d} \right)^2$

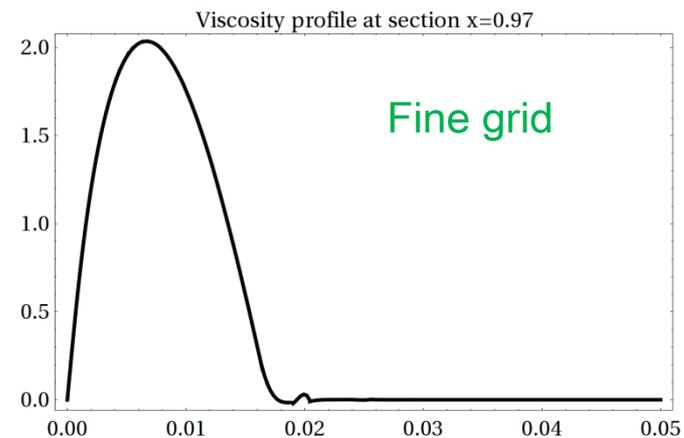
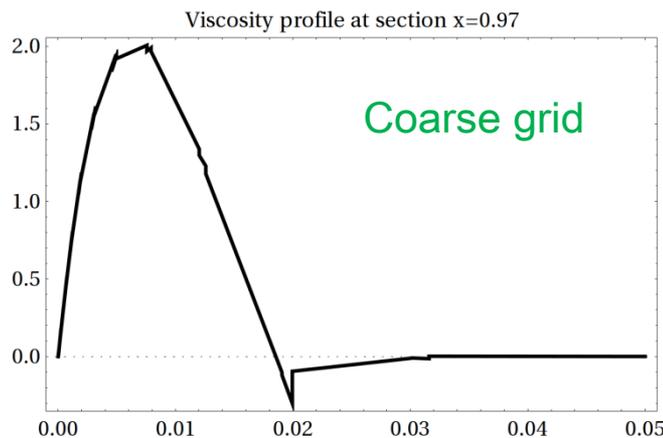
$$f_w = g \left( \frac{1 + c_{w3}^6}{g^6 + c_{w3}^6} \right)^{1/6} \quad g = r + c_{w2}(r^6 - r) \quad r = \frac{\tilde{\nu}^*}{\tilde{\omega} c_{\kappa}^2 d^2}$$

- Given the previous definitions, it is easy to see that the Spalart-Allmaras model becomes **unstable** for negative turbulent viscosities.

$$\lim_{\chi \rightarrow -c_{v1}} f_{v1} = \infty$$

$$\lim_{\chi \rightarrow -c_{v2}} f_{v2} = \infty$$

Latter are frequently observed in the outer boundary layer, if the grid resolution is insufficient.



- Possible solutions :

- Increase the grid resolution

1. Grid refinement
2. Use of high order methods

1. Modification of the turbulence model,...

1. Approximate Jacobian (Spalart & Allmaras '91)
2. Artificial viscosity (Ngyen, Person & Perraire '07)
3. Clipping (Landmann et al '07)
4. Modification of the turbulence model in order to ensure a decrease in time of the negative turbulent energy (Oliver '08)

→ HERE: LOCAL CLIPPING

## 2. Modification of the transpose term

- Original version: breakdown due to negative densities after some iterations
- Likely reason: fast growing of the turbulent variable near the leading edge affects the continuity equation
- Remedy: decouple the SA model and the continuity equation

$$DT_{modif} = \theta \oint_{\Gamma} \left( \begin{array}{ccc} \left\langle n_k D_{11}^{kl} \frac{\partial \phi_i}{\partial x_l} \right\rangle & \cdots & \boxed{0 \quad 0} \\ \vdots & \ddots & \vdots \\ \left\langle n_k D_{1N_v}^{kl} \frac{\partial \phi_i}{\partial x_l} \right\rangle & \cdots & \cdots \left\langle n_k D_{N_v N_v}^{kl} \frac{\partial \phi_i}{\partial x_l} \right\rangle \end{array} \right) \begin{bmatrix} [\rho] \\ \vdots \\ [\tilde{\mu}] \end{bmatrix} dS$$

## 3. Different choices for the penalty coefficient

- Penalty coefficient :

$$\sigma = C_{IP} \frac{\nu}{h}$$

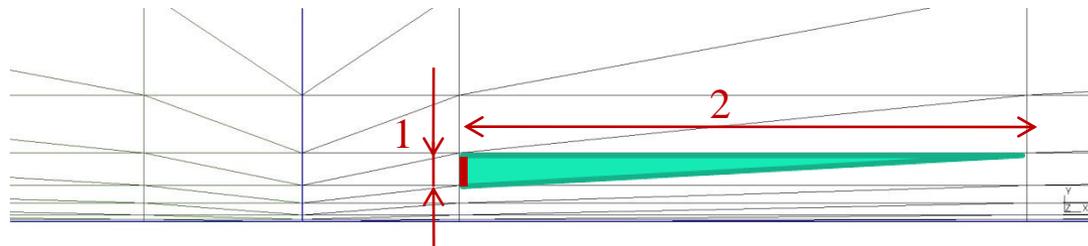
$\nu$  : viscosity

$h$  : element size

- $C_{IP}$  : “constant” depending on the interpolation order  $p$  and the dimension  $d$  ( $\rightarrow$  Shahbazi '05)

$$C_{IP} = \frac{(p + 1) \cdot (p + d)}{d}$$

- Different choices for  $h$  ( $\rightarrow$  K. Hillewaert FEF 2011)



1 : quotient volume/surface  
(Shahbazi)

2 : distance to opposing node

# Test case: Flat plate

- Flat plate

$Re = 5 \times 10^6$   
 $M = 0,2$   
 $L_x = 2$

$$u^+ = U/u_\tau$$
$$y^+ = u_\tau y/\nu$$
$$u_\tau = \sqrt{\tau_w/\rho}$$

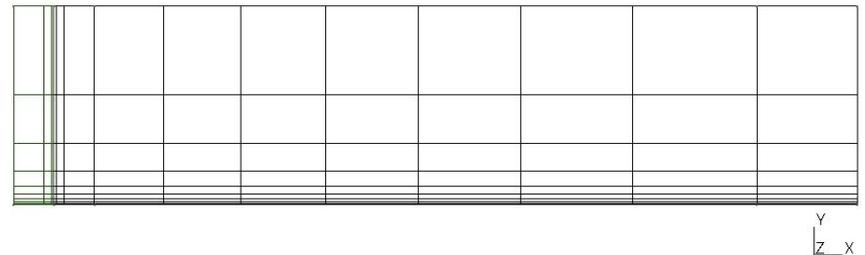
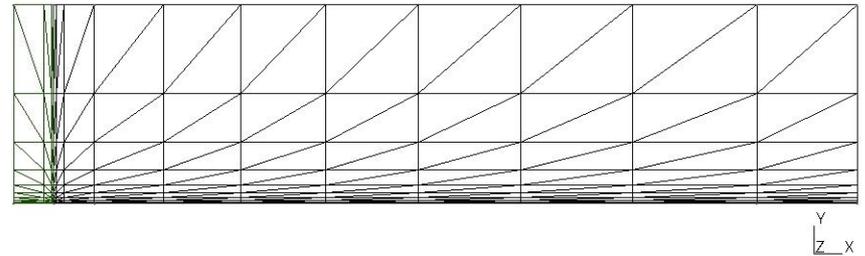
- Grid convergence

- 2 types of grids  
(structured triangles/quadrangles)

- Number of elements  
 $y^+=4: (5+16) \times 15$

...  
 $y^+=128: (5+16) \times 8$

- Velocity profile / Friction coefficient / convergence order

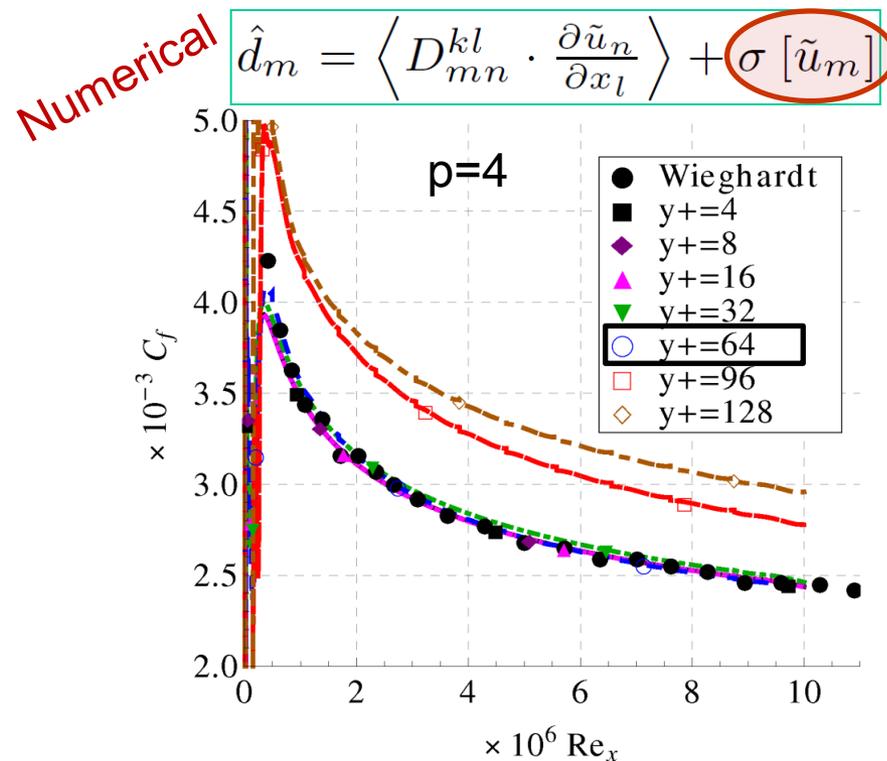
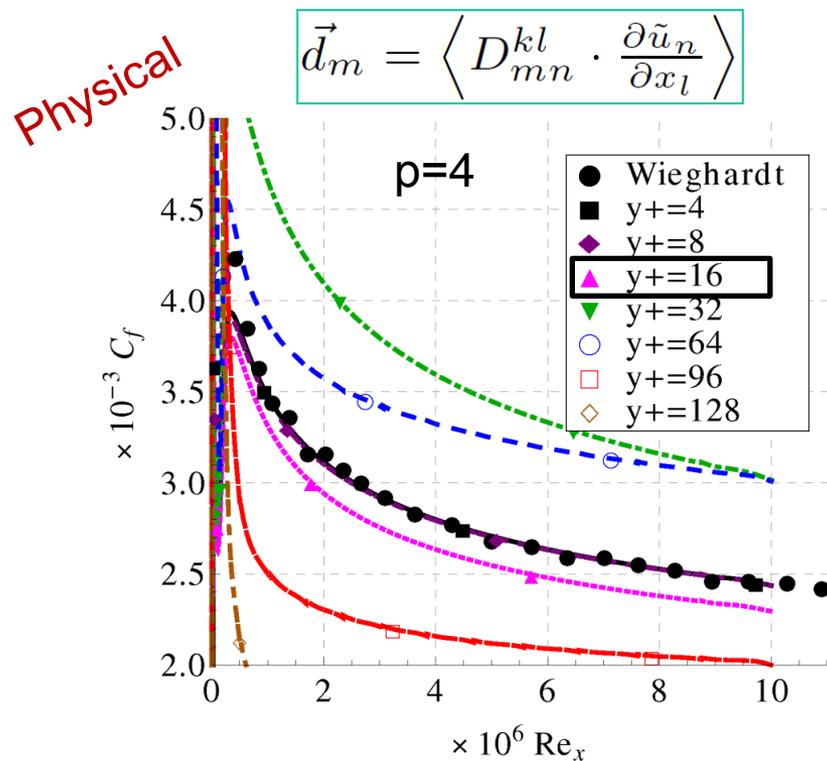


Grid stretching: 1.6

*For the visualization, the grids have been scaled by a factor 10 in y direction.*

# Computed friction (structured quads)

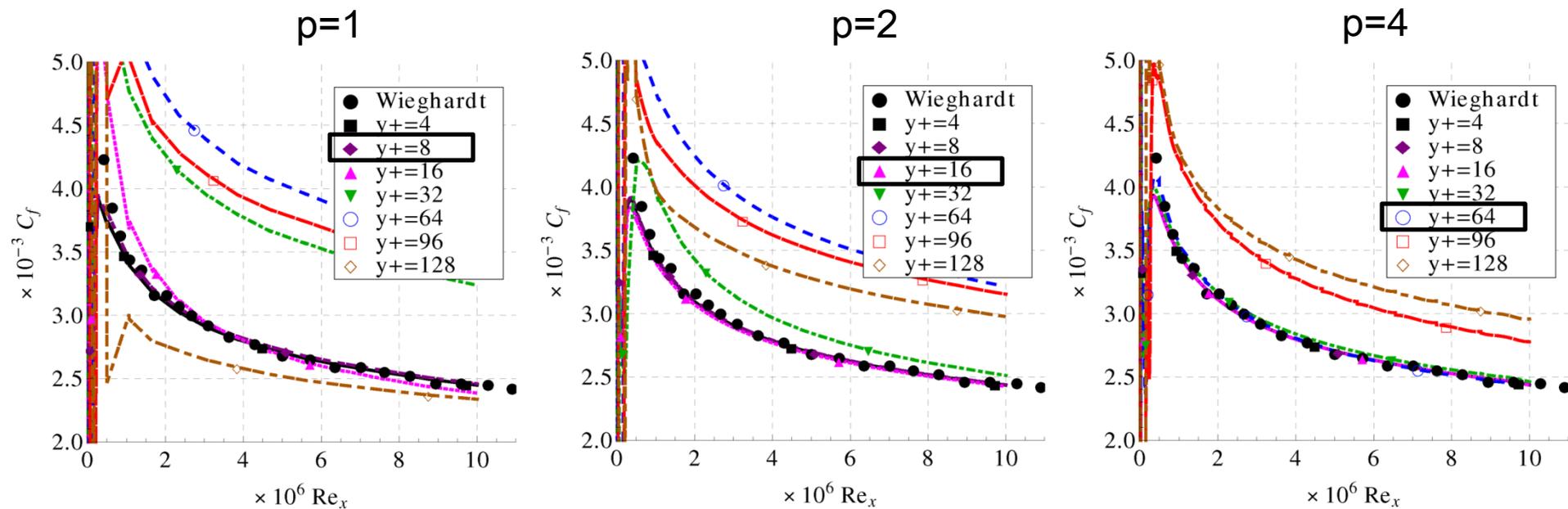
- Physical (consistent) vs numerical skin friction
  - Important improvement of the skin friction  $C_f$  by taking into account the penalty term



# Convergence study – structured quads

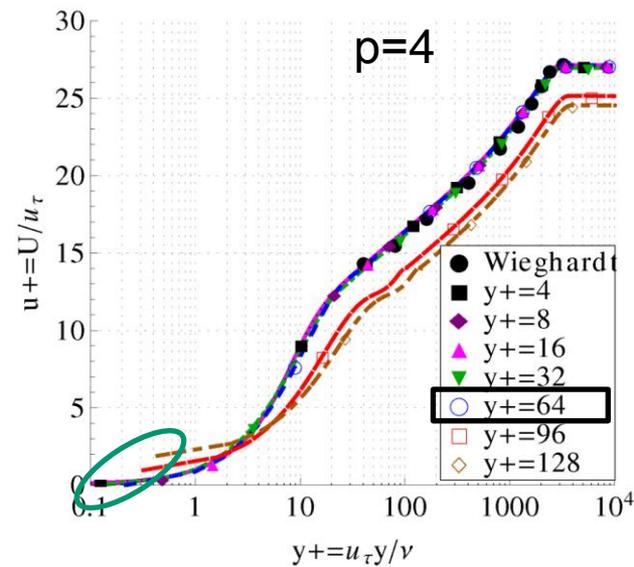
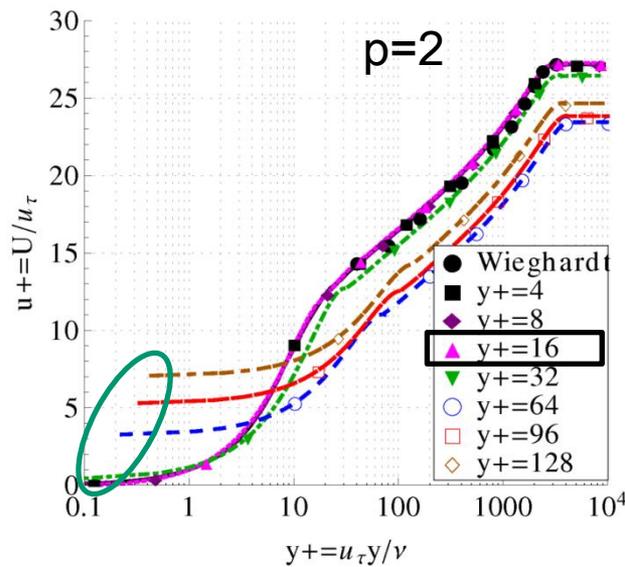
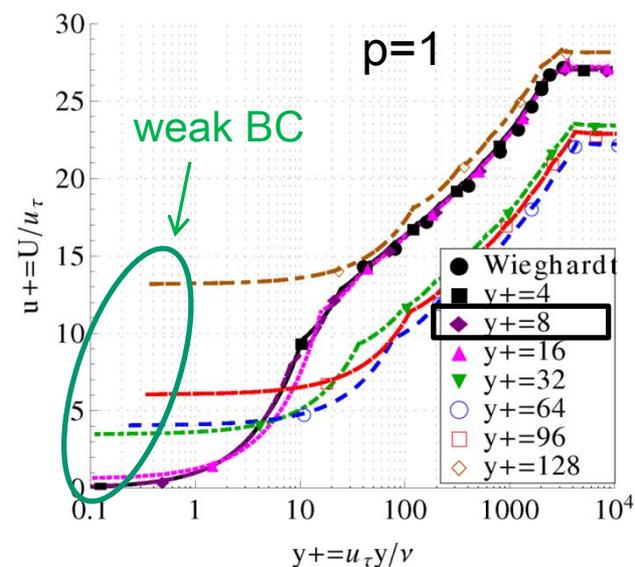
- Friction coefficient  $C_f$  (numerical)

- $p=1 \rightarrow y^+ \approx 8$
- $p=2 \rightarrow y^+ \approx 16$
- $p=4 \rightarrow y^+ \approx 64$



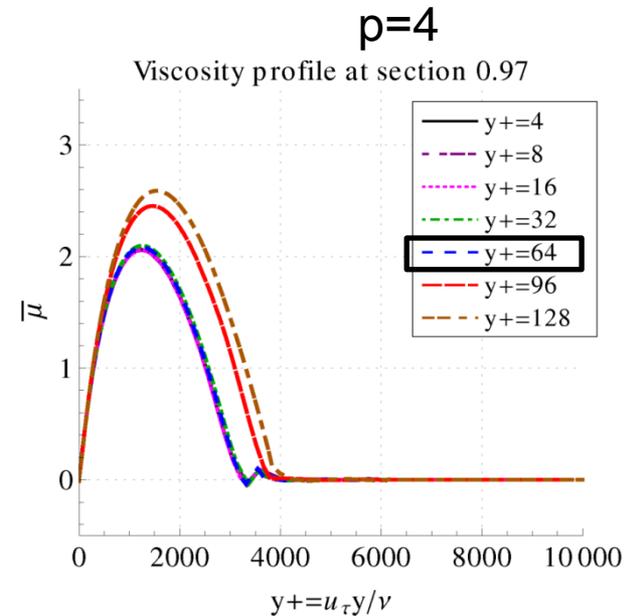
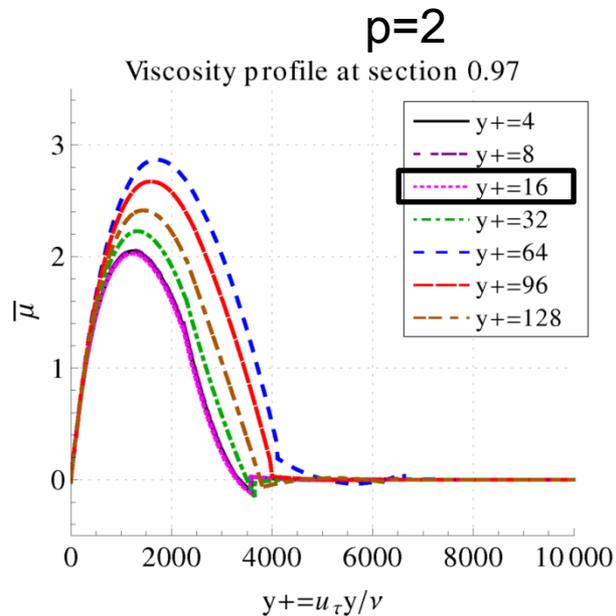
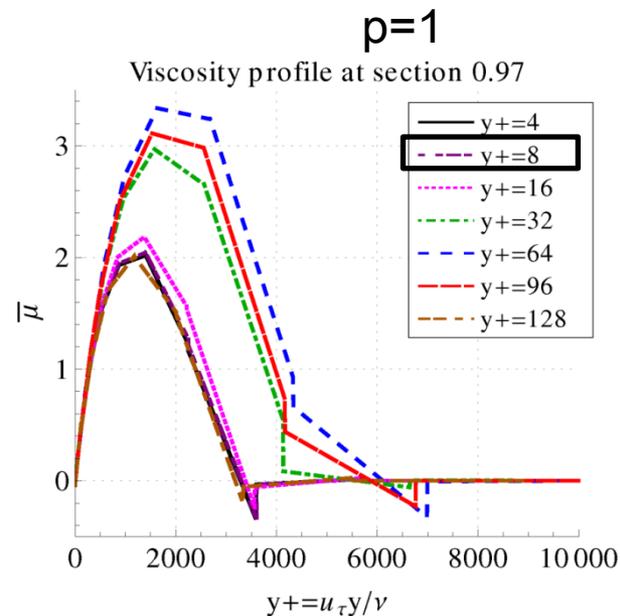
# Convergence study – structured quads

- Velocity profiles  $u^+(y^+)$ 
  - Boundary conditions (BC) are imposed weakly
  - Similar mesh resolutions as those based on the numerical friction
  - A very strict compliance with the no-slip BC is not required



# Convergence study – structured quads

- Turbulent viscosity profiles:  $\bar{\mu} = \tilde{\mu}/(100\mu)$ 
  - Close to the wall: - no difference between P<sup>1</sup>, P<sup>2</sup> and P<sup>4</sup>-elements
  - In the log-layer: - larger spread of → *artificial thickening*  
- important undershoot → *stability*



# Comparison – quads vs triangles

- Skin friction

- Smoother skin friction with quads

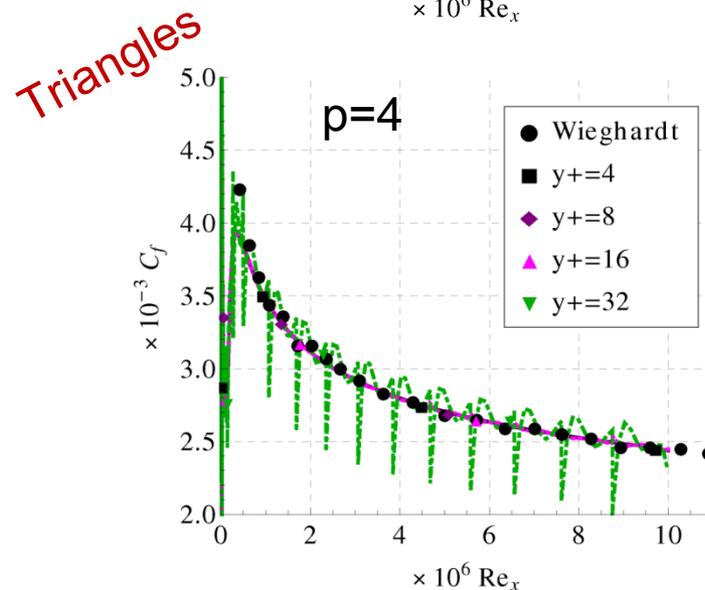
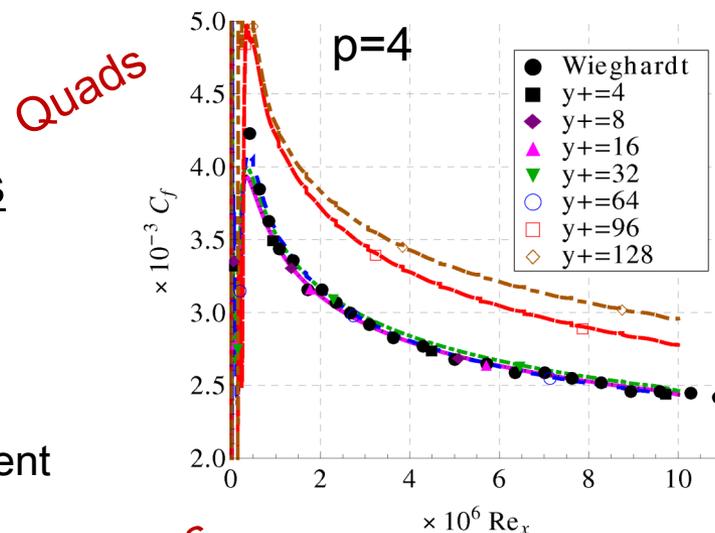
- Reasons:

1.  $C_f$  is proportional to  $\partial u / \partial y$   
⇒ one order higher for quads
2. No jump penalization between adjacent triangles that share only one node

- Velocity profiles

- No significant difference between quads and triangles

- The no-slip condition is slightly better respected with triangles

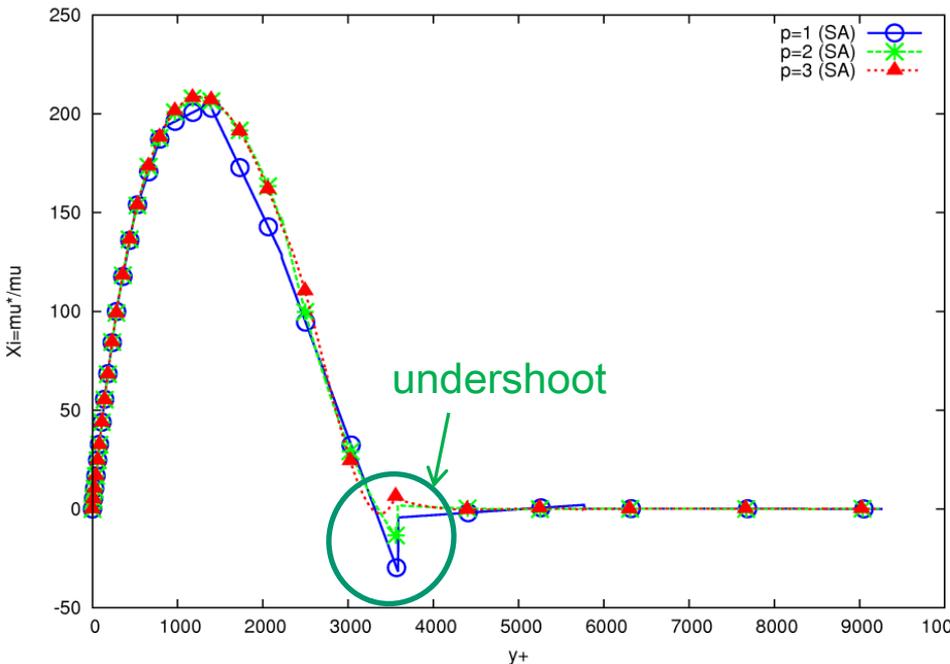


# High-order turbulent viscosity???

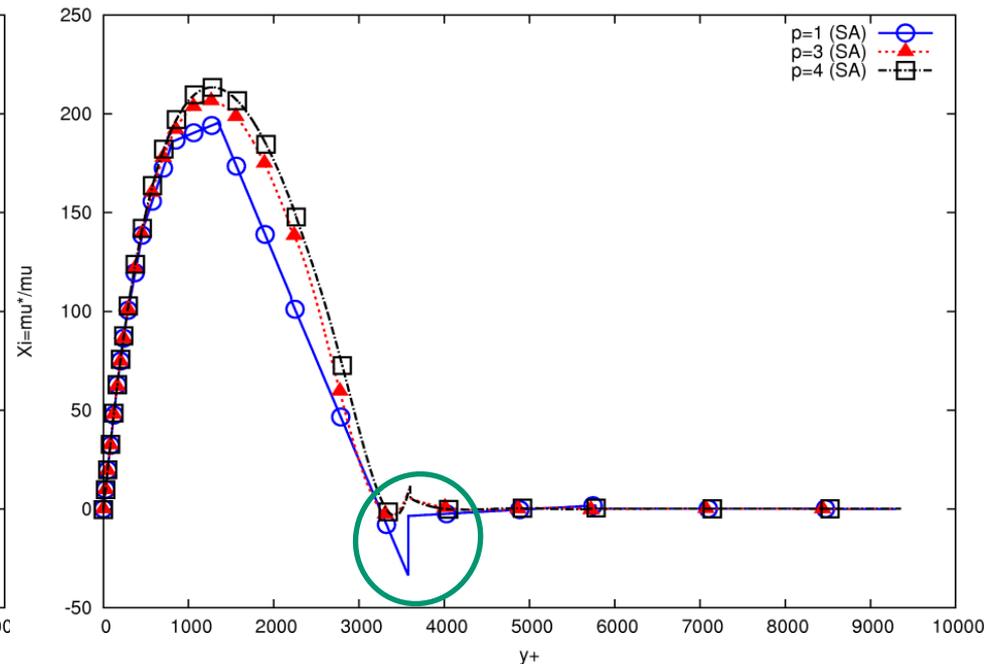
- Necessity of high-order polynomials to discretize the turbulence model?

## 1. Turbulent viscosity profiles (x=0.97)

p=3 ( $y^+=32$ )



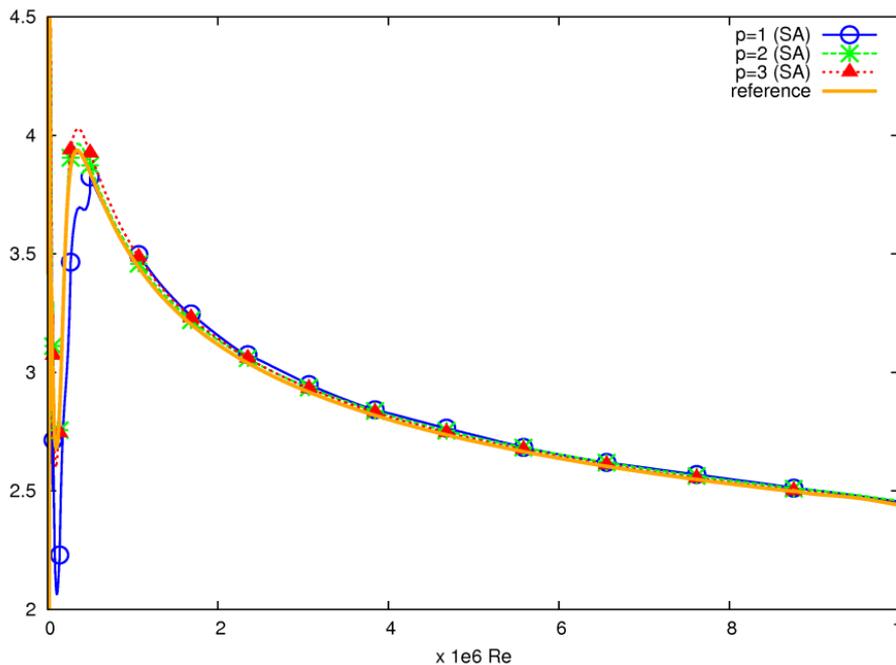
p=4 ( $y^+=64$ )



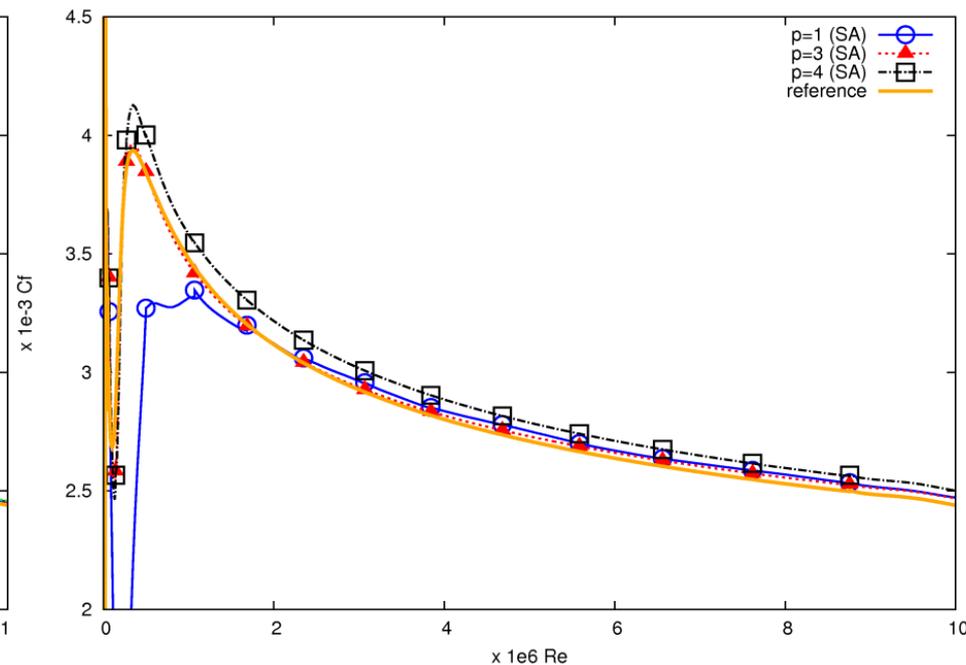
# High-order turbulent viscosity???

## 2. Skin friction

p=3 ( $y^+=32$ )



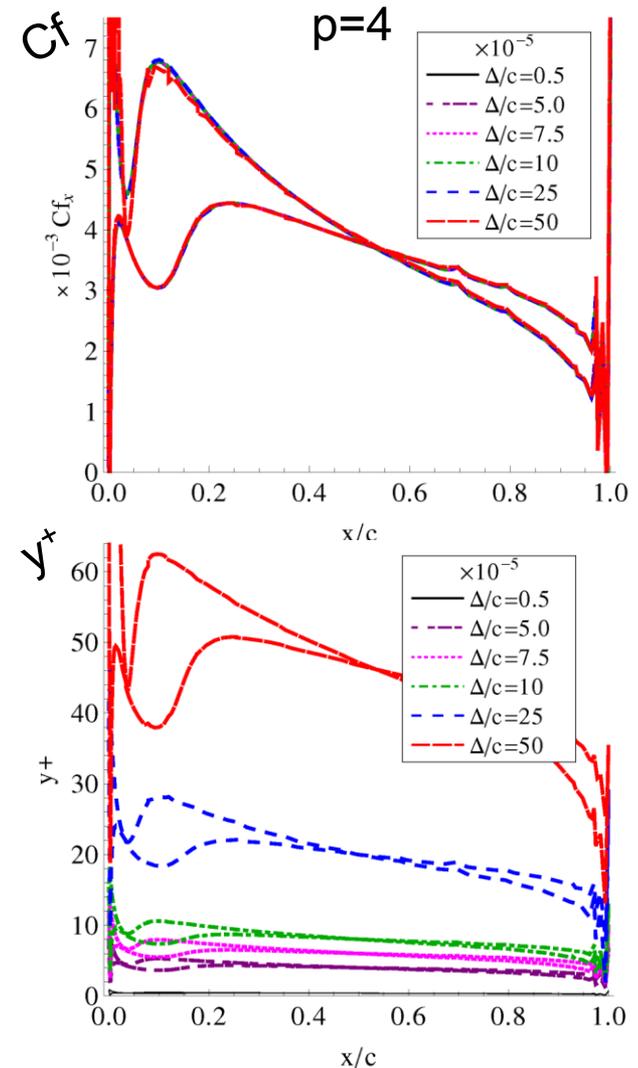
p=4 ( $y^+=64$ )



⇒ No significant impact

# Effect of grid curvature – NACA 0012

- NACA 0012 ( $\alpha=3.59^\circ$ )
  - $Re=1.86 \times 10^6$ ,  $M_\infty=0.3$
  - 4<sup>th</sup> order geometry
  - 19 elements along the chord (2500 to 4800 elements)
- Observations
  - Good results for similar grid resolutions as in the case of straight elements, i.e.  $y^+ \approx 50$  to 60 ( $p=4$ )
  - Accuracy of low-order polynomials decreases with increasing curvature



# Test case: 3D high-lift cascade flow

- Description

$Re = 8.4 \times 10^5$

$M_\infty \approx 0,6$

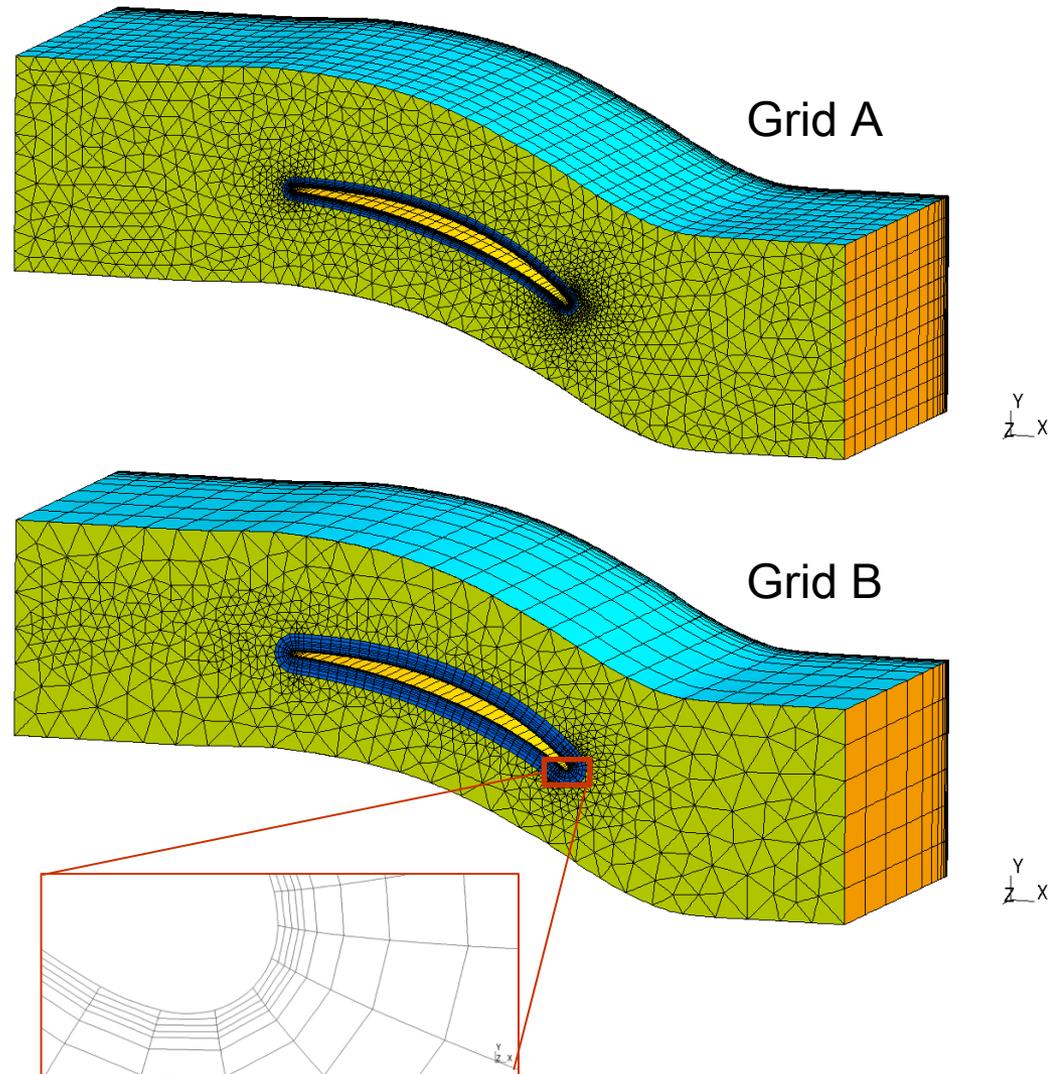
- Grid specifications

- Grid A

- 42 000 hex
- 52 800 prisms
- 22 layers

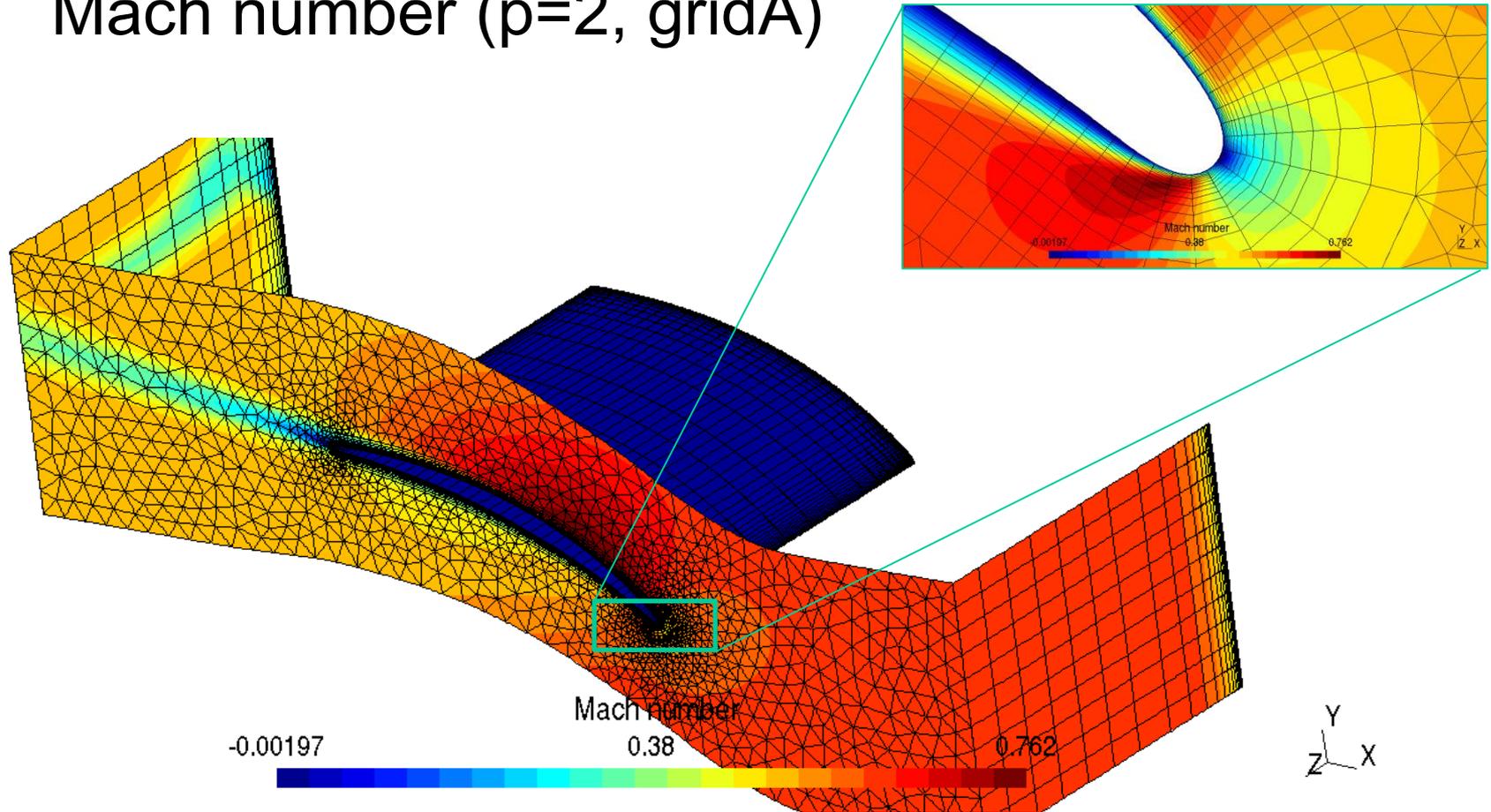
- Grid B

- 17 800 hex
- 19 400 prisms
- 15 layers



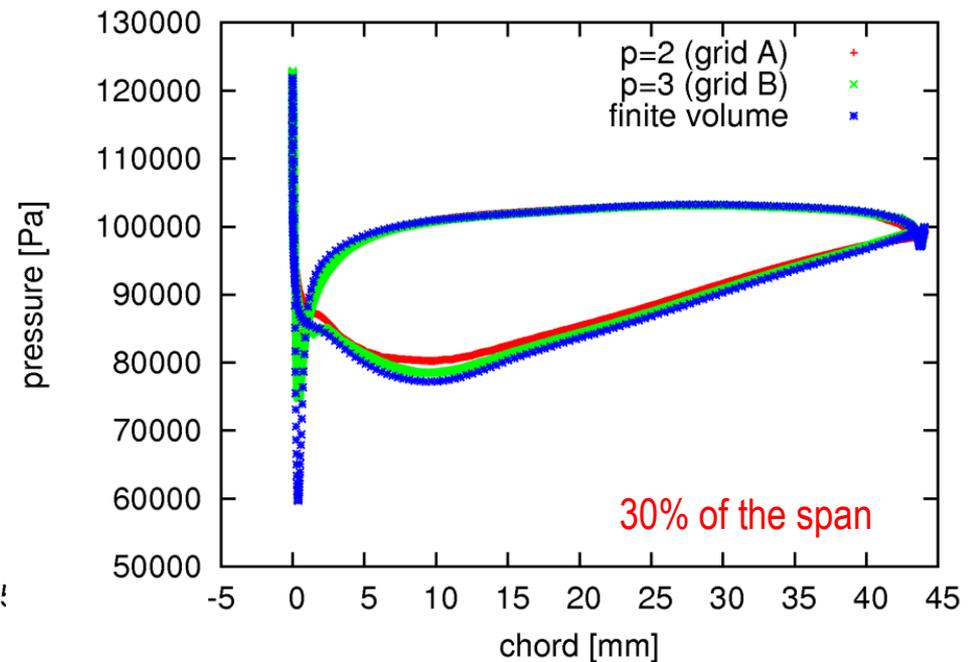
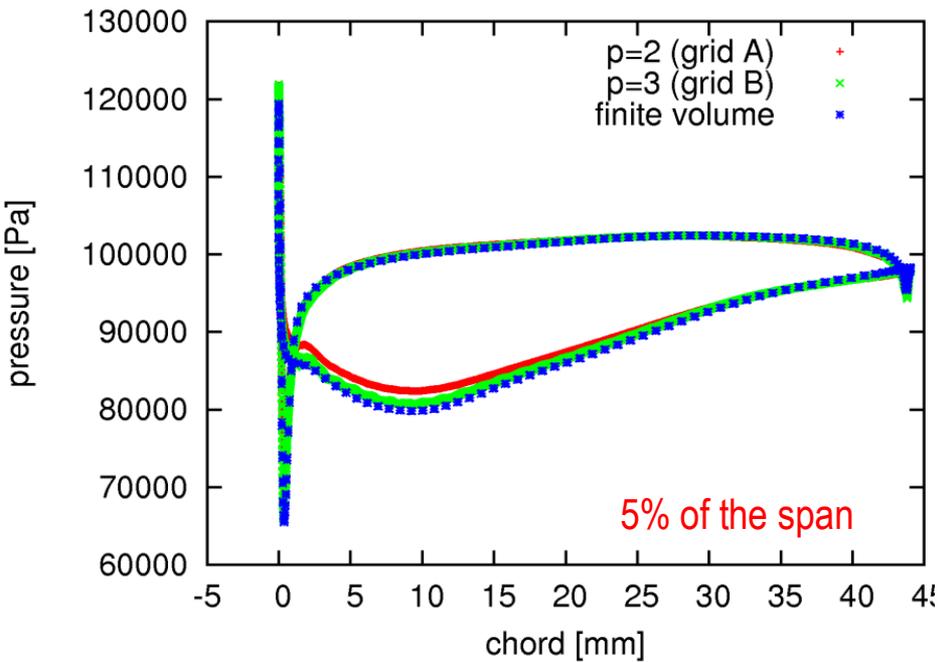
# Test case: 3D high-lift cascade flow

- Mach number (p=2, gridA)



# Test case: 3D high-lift cascade flow

## Pressure



- Presented results
  - Adaptation of the SIPDG method to RANS computations
  - Grid resolution for turbulent boundary layers
  - Impact of lower order approximation of the turbulent viscosity
  - 3D high-lift cascade flows
- Future work
  - Improvement of the linear solver
  - Reduction of the memory consumption in 3D
  - Grid adaptation