
Energy efficiency of sludge drying processes

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Wastewater sludge: production and quantities

Sludge's origin

- Urban residual sludges
 - Activated sludge wastewater treatment plant (WWTP)



Oupeye - 446 500 PE

www.aide.be

Structure of a WWTP



Wastewater



Screening



Sand and grease removal



Biological treatment
Activated sludge reactor



Separation between treated water and sludge
Settling tank



Sludge draining and mechanical dewatering



Evacuation of dewatered sludges



Treated water

« Pasty material »
70 to 85% water !!

Structure of a WWTP

- Sludge processing
 - Applied to excess biomass produced by the biological treatment
 - Thickening
 - Stabilisation
 - Liming
 - Digestion (biomethanation)
 - Mechanical dewatering
 - Centrifugation
 - Belt filter
 - Press filter
 - Valorisation

Drying



Quantities

Countries	Sludge Production Volume Tds/a	
	2010 estimate	2020 estimate
USA	7.000.000	10.000.000
Austria	273.000	280.000
UK	1.640.000	1.640.000
Scotland	200.000	200.000
Spain	1.280.000	1.280.000
Sweden	250.000	250.000
France	1.300.000	1.400.000
Germany	2.000.000	2.000.000
Italy	1.500.000	1.500.000
Romania	165.000	520.000
Portugal	420.000	750.000
Poland	520.000	950.000
Hungary	175.000	200.000
EU27	11.500.000	13.500.000

**Europe:
About 50 to 60 million tons
of humid sludge**

Global production globale > 50 million T DS/year

Sludge valorisation

Sludge valorisation

- Valorisation in agriculture
 - Mineral and organic elements
 - Humic value
 - Fertilizer
- Energy valorisation
 - Incineration in a specific furnace
 - Co-incineration with domestic waste
 - Incineration in cement kilns
 - Biomethanation → cogeneration
 - Pyrolysis/gazification → cogeneration
- Land filling
 - Banned

Europe - 2010
Agriculture: 42%
Incineration: 27%
Landfill: 14%
Others: 16%



Sludge drying

Why ? How ? Difficulties ?

Why drying ?

- Energy valorisation
 - Drying \Rightarrow Increase of lower heating value

$30 < DS < 45\%$: self combustibility

\Rightarrow Incineration in a specific furnace

$60 < DS < 90\%$: LHV \cong domestic waste (8400 kJ/kg)

\Rightarrow Co-incineration

$DS > 85\%$

\Rightarrow Pyrolysis or gazification

Sludges, a complex material

- Sludge = rheologically complex material

Transition between liquid-pasty-solid states during drying

Increasing siccidity					
(% MS)	< 10	10 - 40	40 - 60	60 - 90	> 90
State	Liquid	Viscous liquid – pasty	Glue phase ('sticky')	Granular solid	Dry solid

Sludge rheological behaviour and transition between states is extremely variable:

It depends on: sludge chemical and biological nature

treatment conditions (stabilisation, dewatering, ...)

pumping conditions, storage, ...

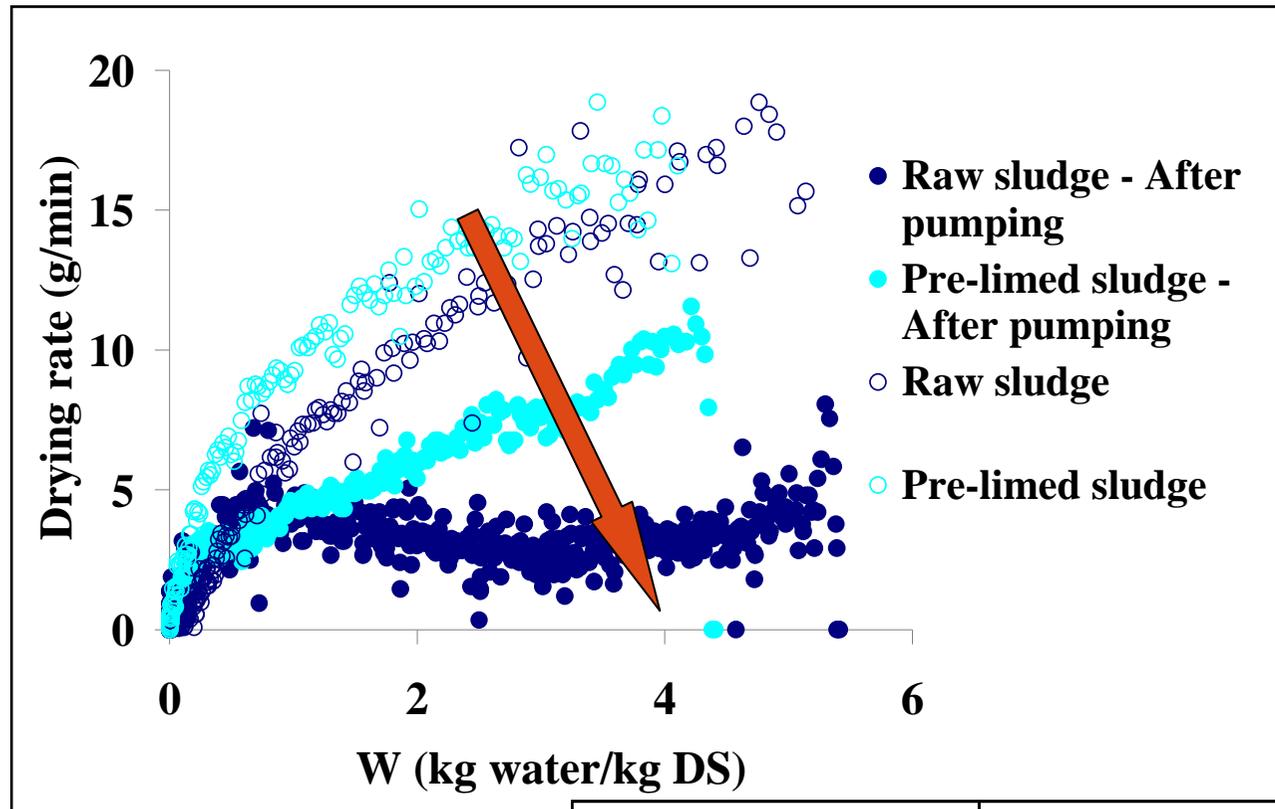
Sludge
«history»

Sludge drying = complex operation

- **Complex process depending on**
 - ❑ sludge origin
 - ❑ rheological properties
 - ❑ composition (organic matter, EPS, fat content, ...)
 - ❑ treatments underwent within the WWTP
 - flocculation
 - mechanical dewatering
 - liming
 - pumping, conveying ...
- **Few specialised manufacturers**
 - ❑ Adaptation of existing technologies
 - ❑ Bad knowledge of the material → design errors
 - ❑ Diffusion of good practices !!

Sludge drying = complex operation

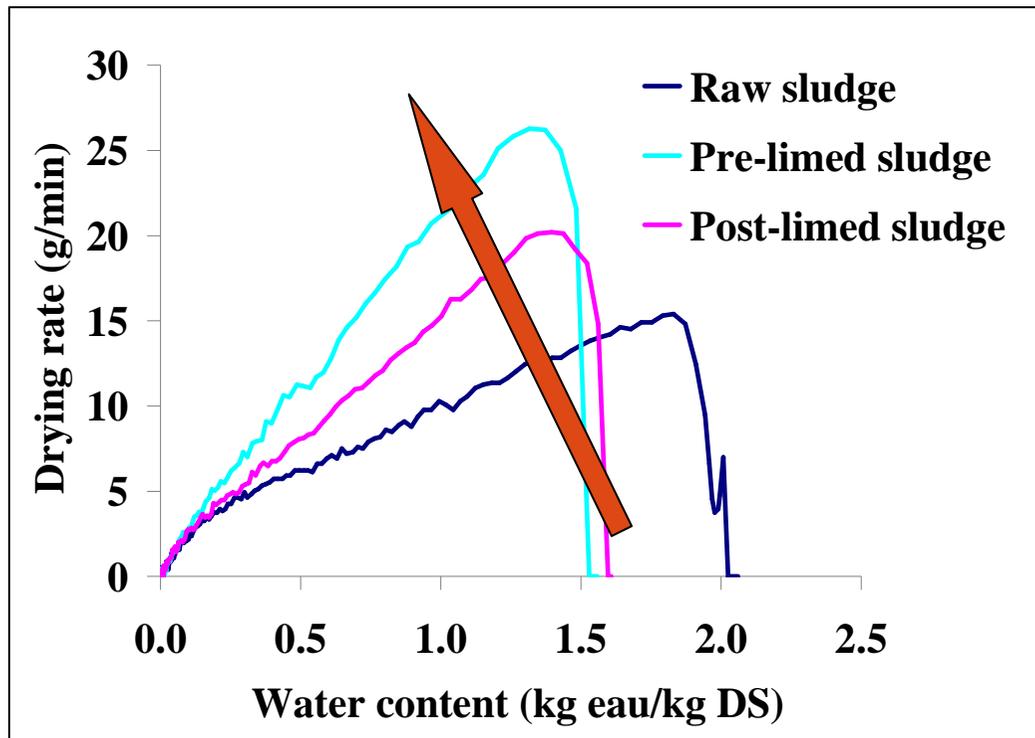
■ Influence of pumping



	Specific evaporation capacity (kg/m ² h)
Raw sludge	21.4
Pumped sludge	9.9

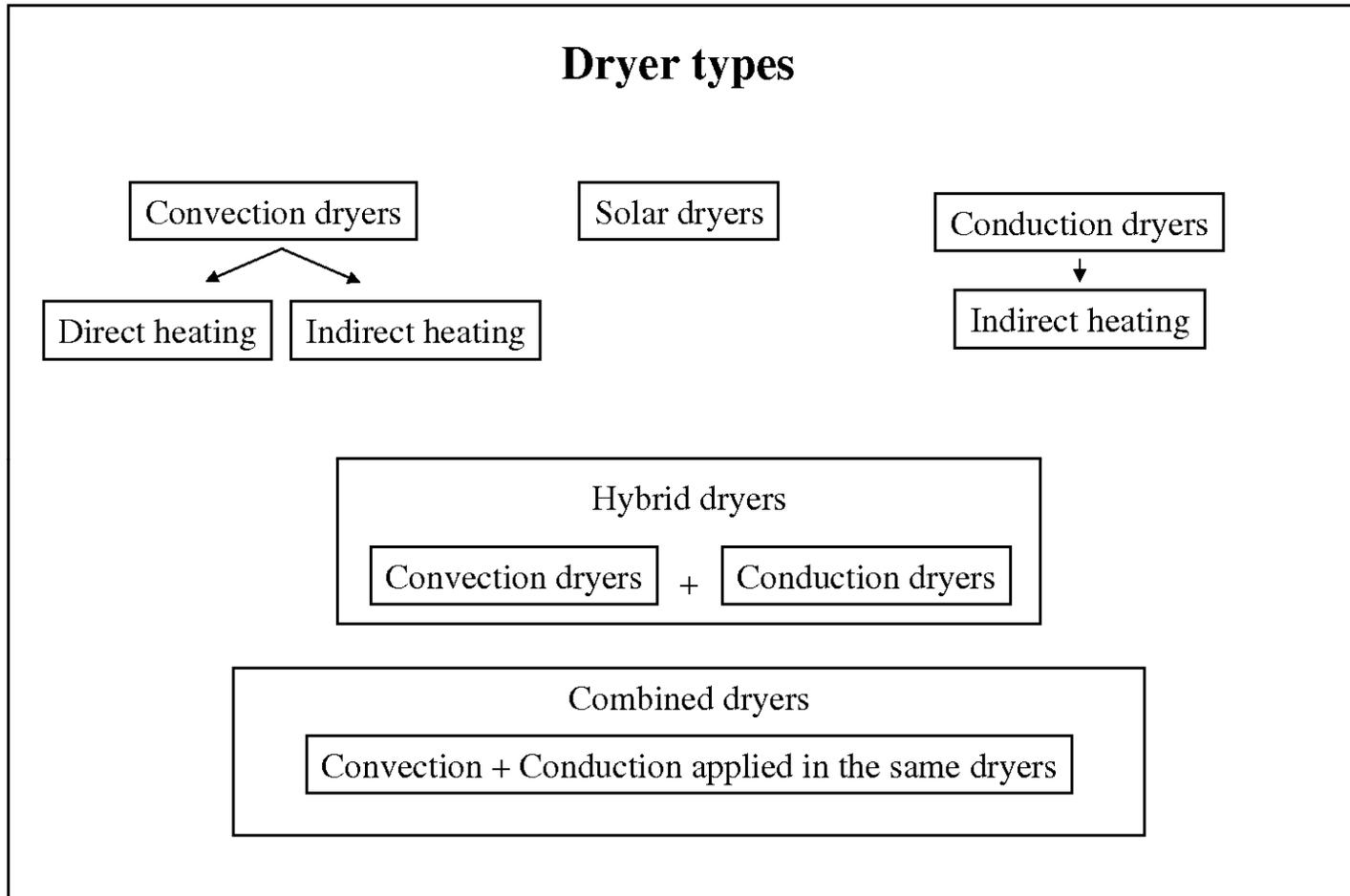
Sludge drying = complex operation

■ Influence of liming



	Specific evaporation capacity (kg/m ² h)
Raw sludge	24.3
Post-liming	28.9
Pre-liming	37.0

Drying technologies



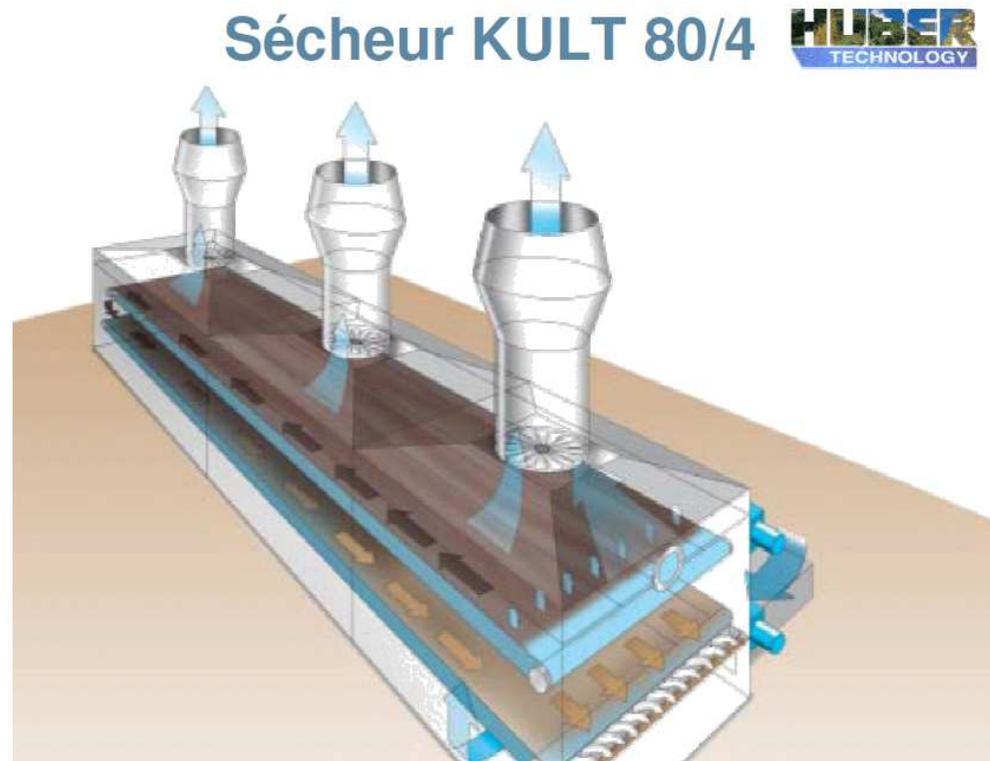
Drying technologies

■ Convective dryers

Dryer type	Operating range (in terms of water content X , expressed on a dry basis)	Specific drying rate ($\text{kg m}^{-2} \text{h}^{-1}$)	Specific energy consumption (kWh ton^{-1})
Belt dryer	Full drying	from 5 to 30	700 to 1140
Direct drum dryer	Full drying, with dry product backmixing: $0.1 \leq X \leq 0.54$	from 3 to 8	900 to 1100
Flash dryer	Full drying	from 0.2 to 1	1200 to 1400

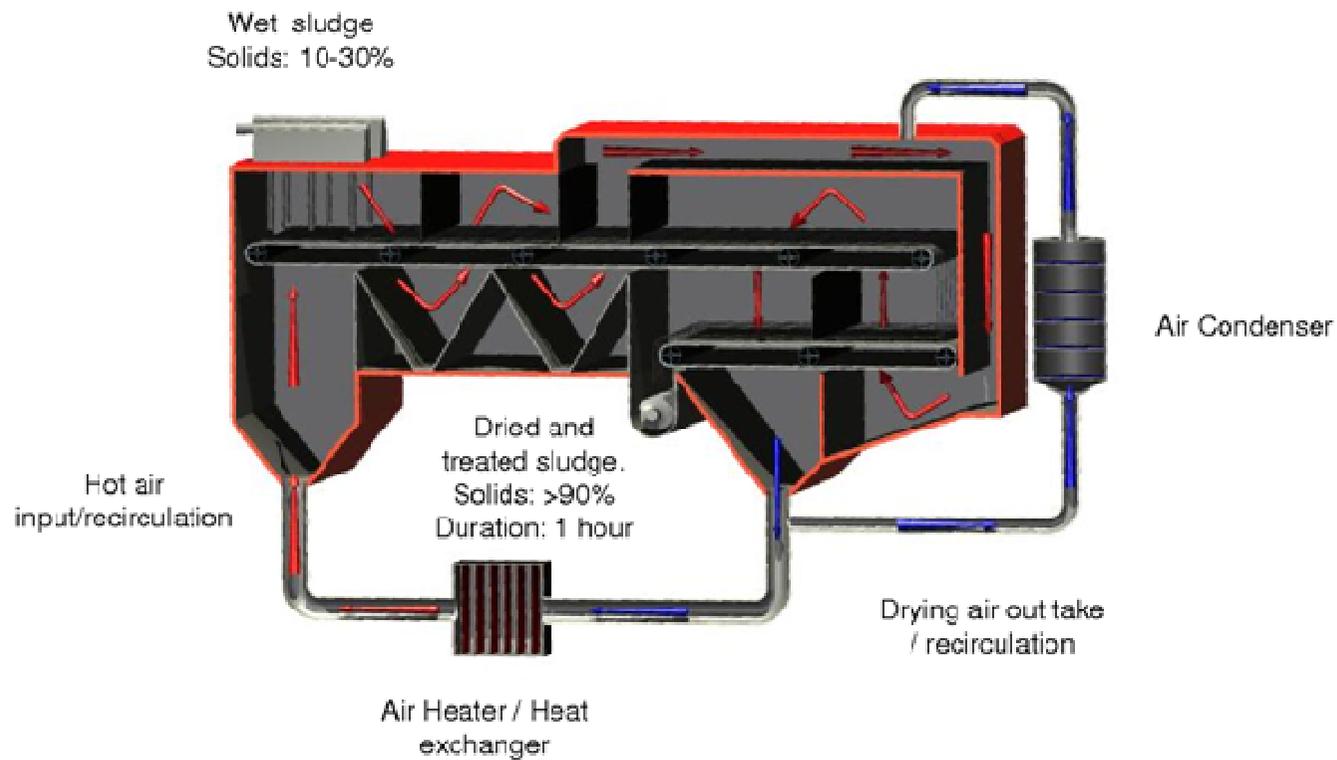
Drying technologies

- Belt dryer: Tenneville - Huber



Drying technologies

- Belt drying: BioCon® - Krüger (USA)



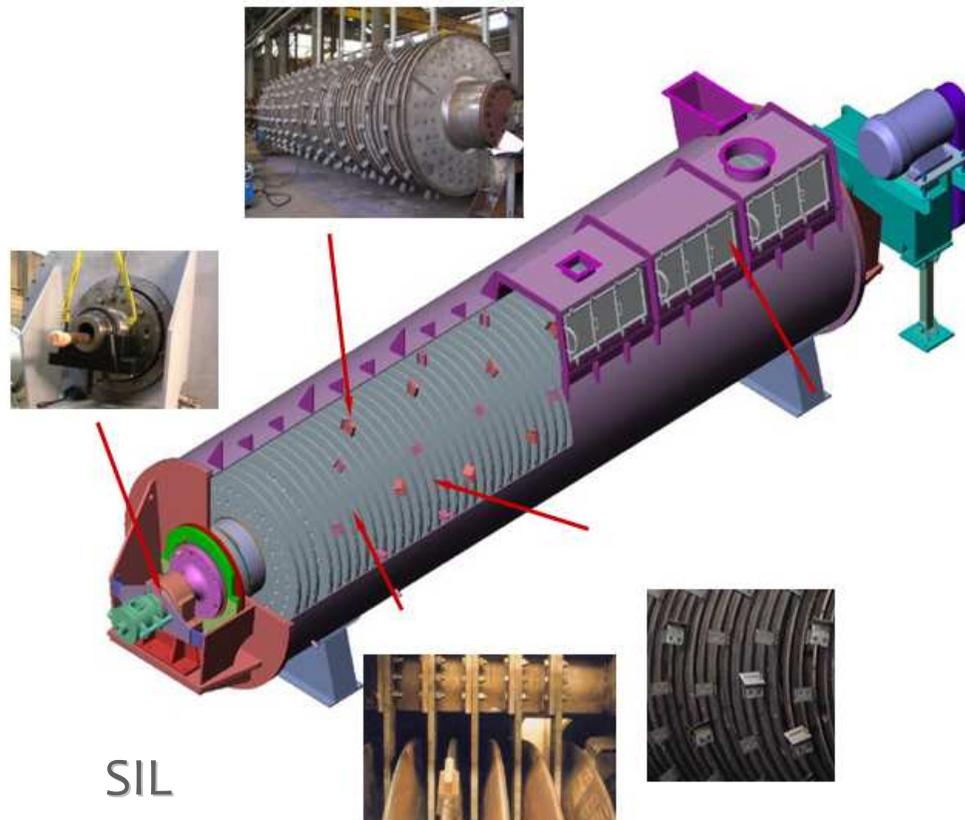
Sludge technologies

■ Conductive dryers

Dryer Type	Operating range (in terms of water content X , expressed on a dry basis)	Specific drying rate ($\text{kg m}^{-2} \text{h}^{-1}$)	Specific energy consumption (kWh ton^{-1})
Disc dryer	Partial drying: $1.25 \leq X \leq 4.5$	from 10 to 12	from 855 to 955
	Full drying, with recycling of dry product upstream : $0.1 \leq X \leq 0.54$	from 7 to 10	
Paddle dryer	Full drying: $0.1 \leq X \leq 4.5$	from 15 to 20	from 800 to 885
Thin film dryer	Partial drying: $0.54 \leq X \leq 4.5$	from 25 to 35	from 800 to 900

Drying technologies

- Disc dryers

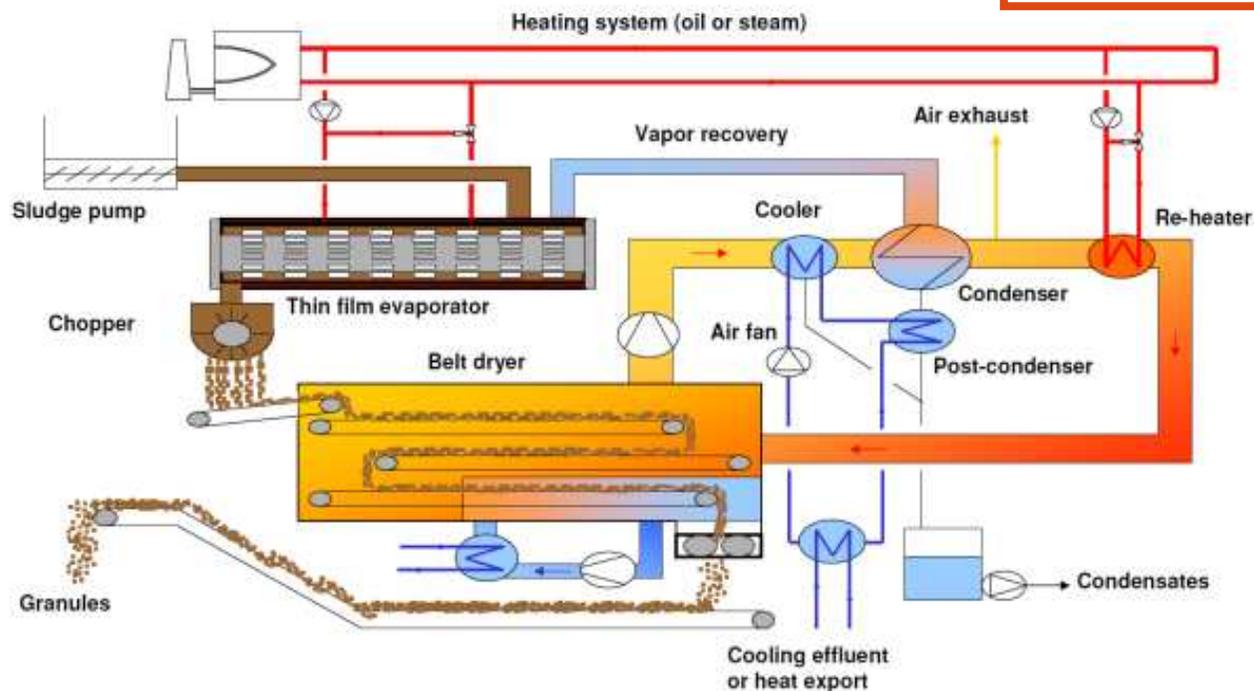


Gouda GMF

Drying technologies

- Hybrid systems: thin film evaporator + belt dryer

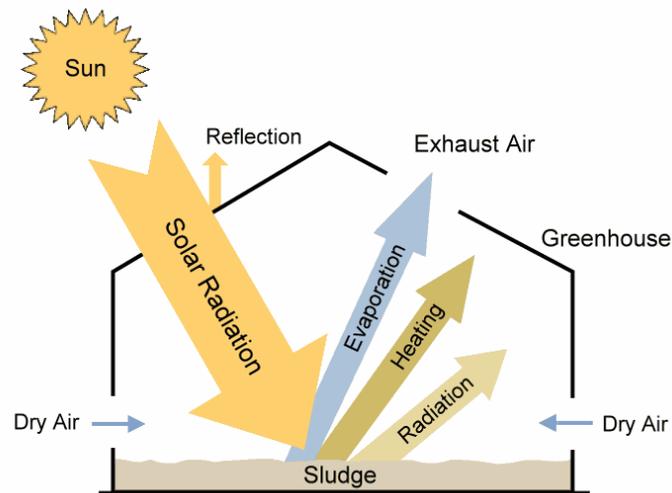
INNODRY 2E® drying process



700 to 900 kWh/t EW – 0.5 to 4 t/h

Drying technologies

- Solar dryers → greenhouses
 - Closed, open, combined with heated floor



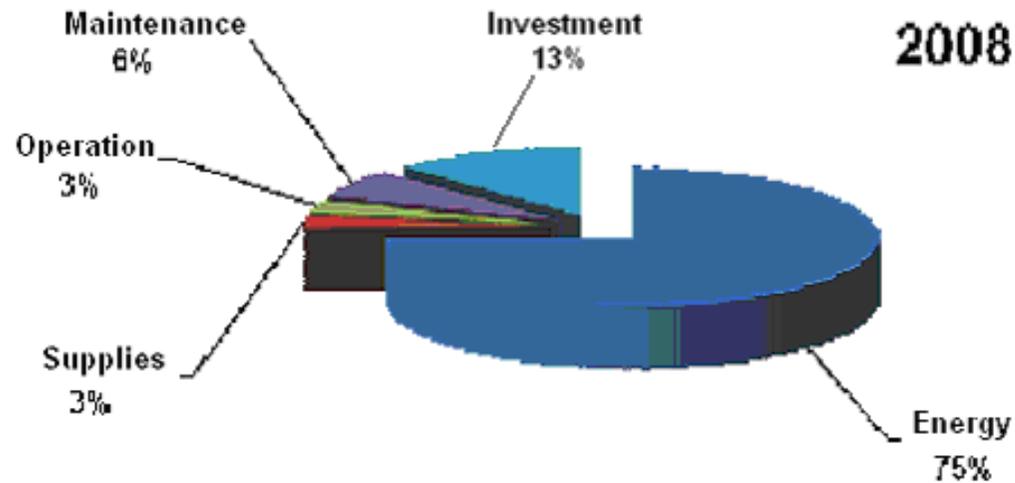
30 to 200 kWh/t EE – up to 1000 in the case of chemical desodorisation

Sludge drying

How to increase performances ?

Reduction of energy invoice

- Essential !!



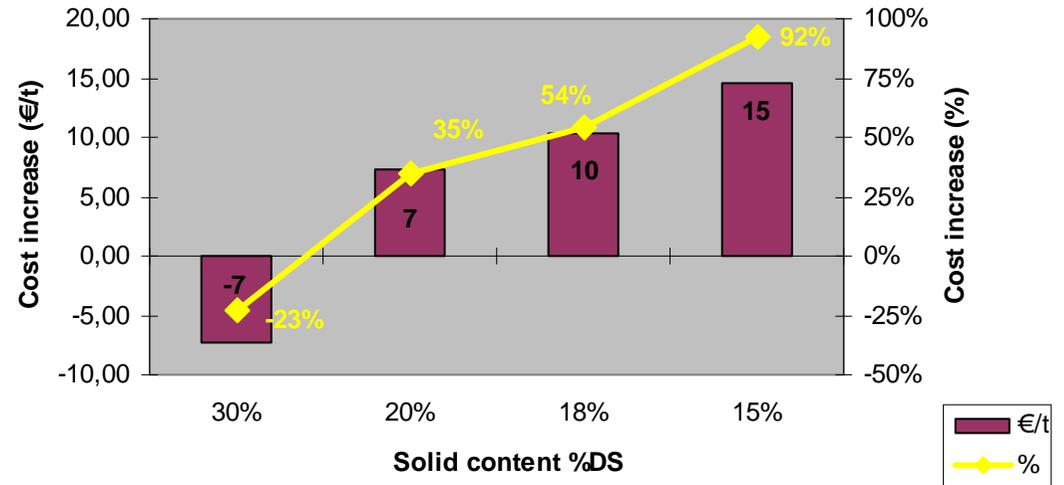
Sludge thermal drying costs distribution

D. Permuy, ECSM 2010, Budapest, Hungary

Reduction of energy invoice

- Inlet siccidity increase
- Losses reduction, design and operating conditions optimisation
- Heat valorisation on site
 - Use of biogas
 - Incineration waste heat
 - ...

ENERGY COSTS INCREASE
(Comparative with 25%DS)



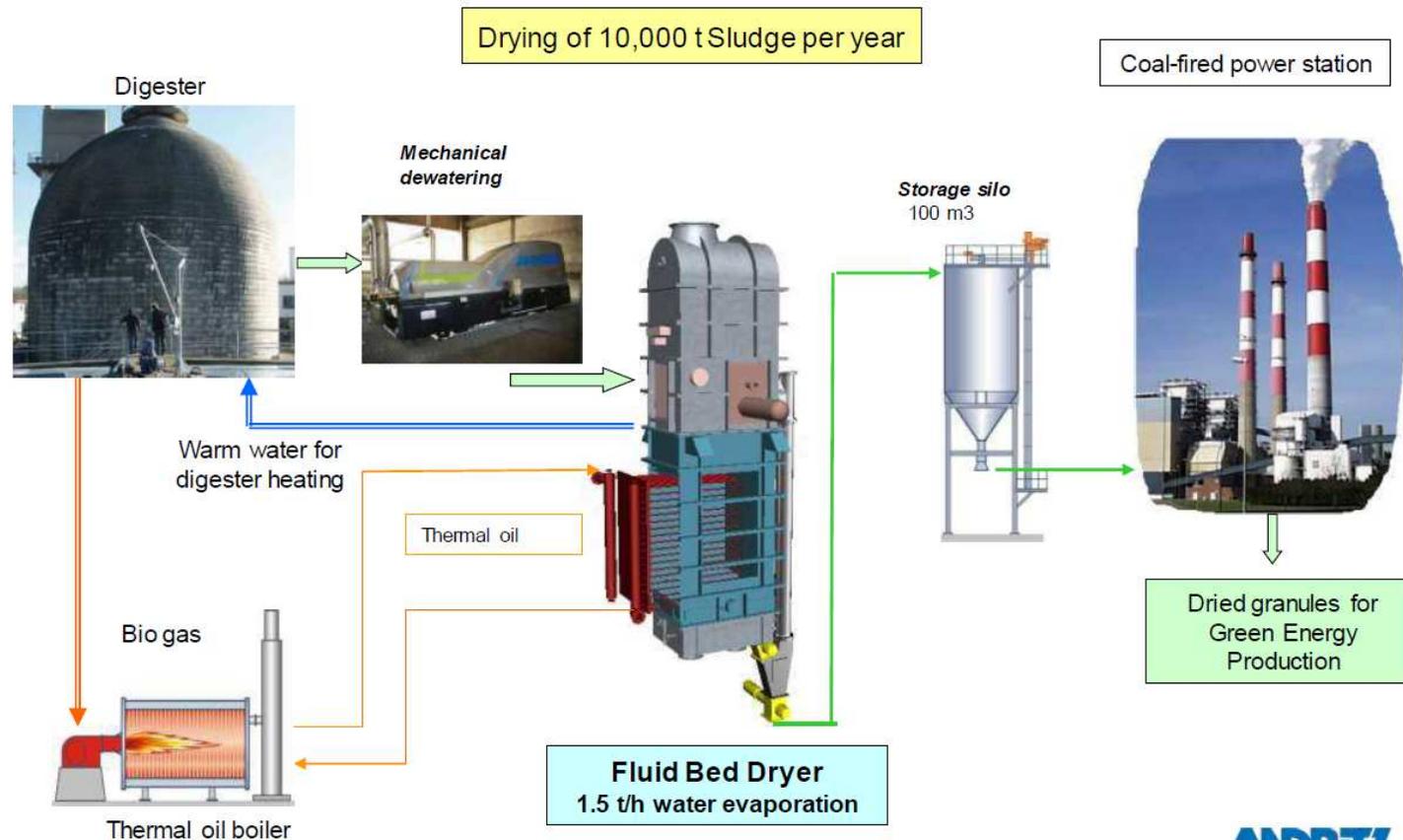
D. Permuy, ECSM 2008, Liège, Belgium



Example of energy integration

■ Biogas valorisation

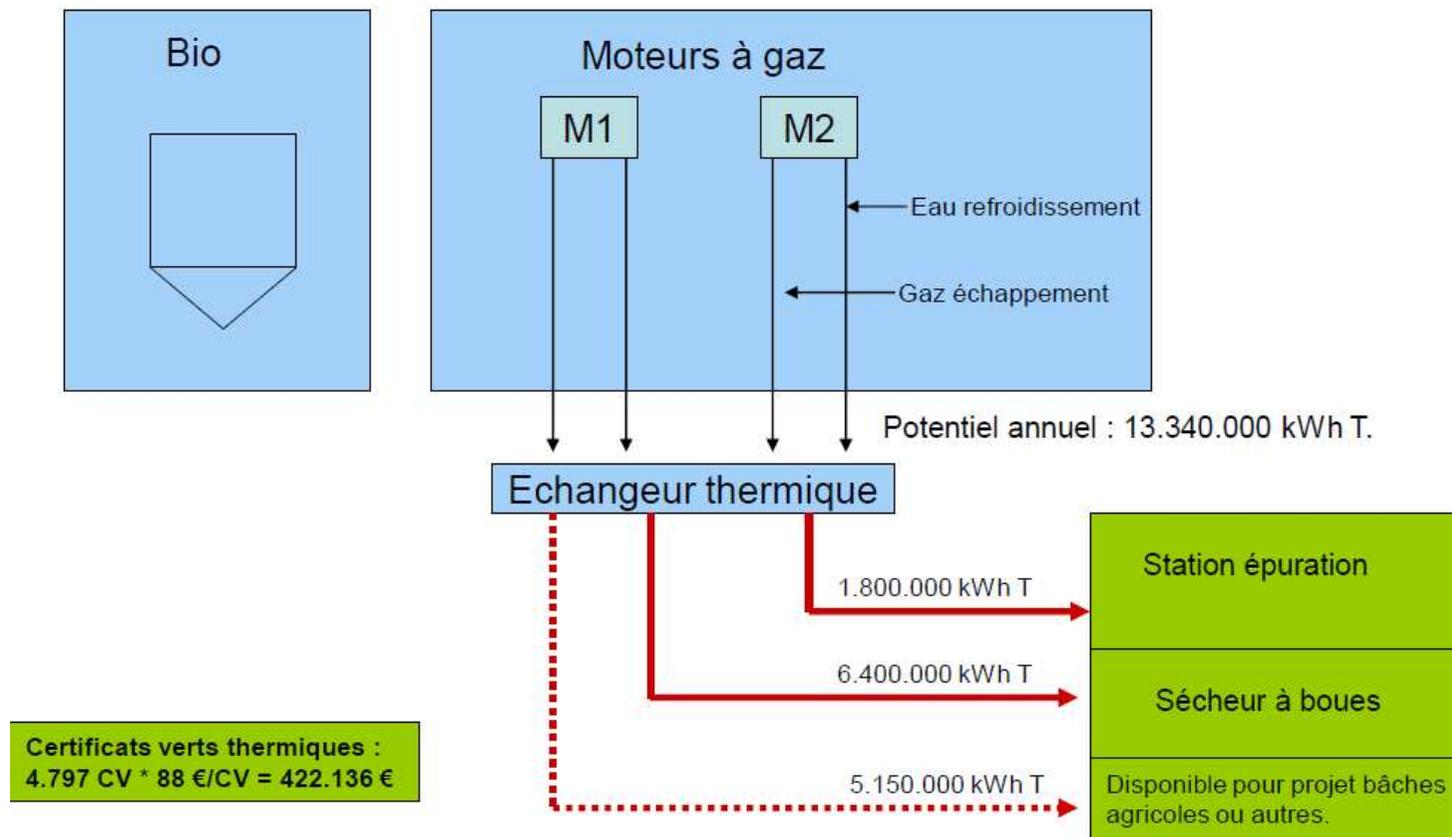
— *Drying with Bio gas in Memmingen, Germany*



ANDRITZ
Environment & Process

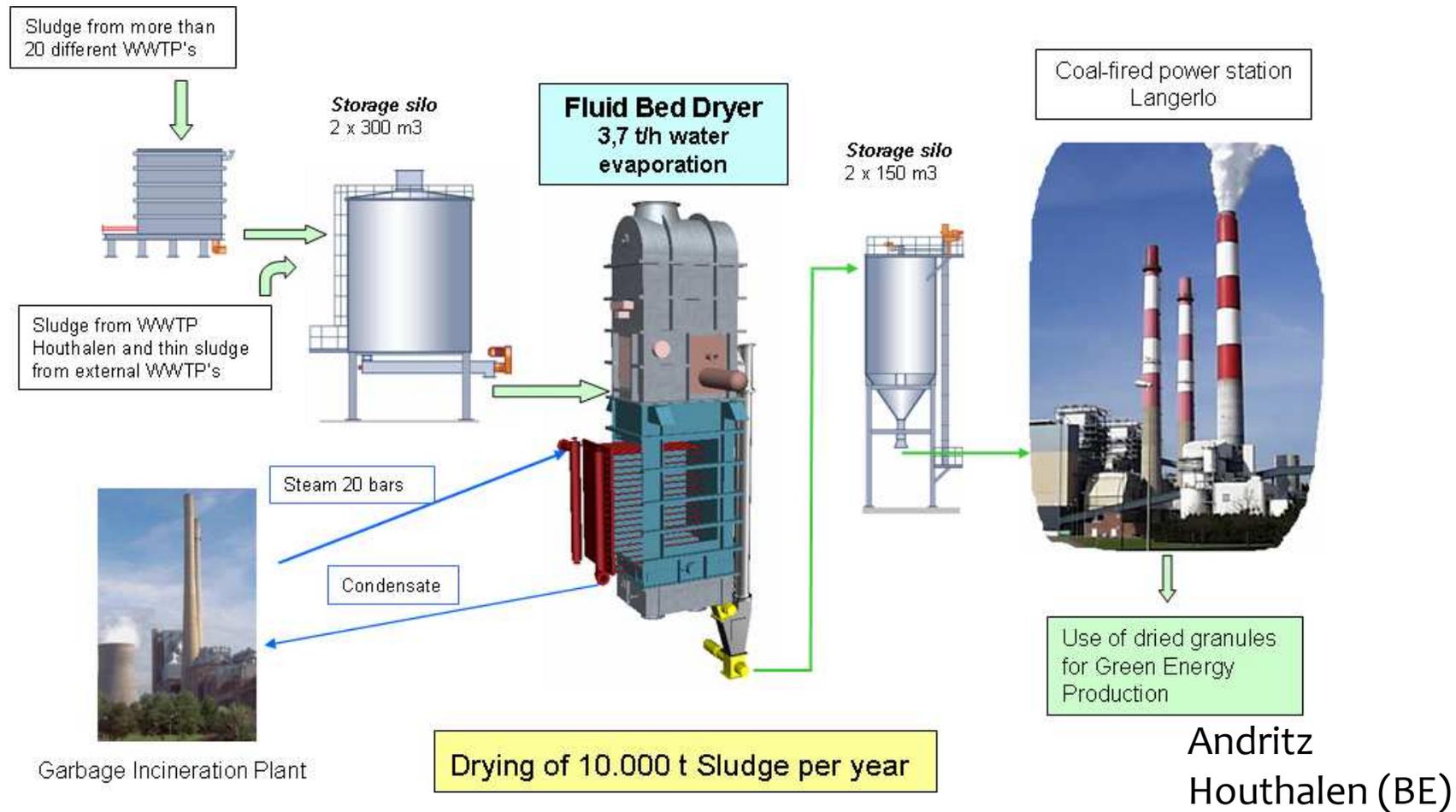
Example of energy integration

- Biogas valorisation: waste management integrated plant (Tenneville, Belgium)



Example of energy integration

■ Incinerator waste heat recovery

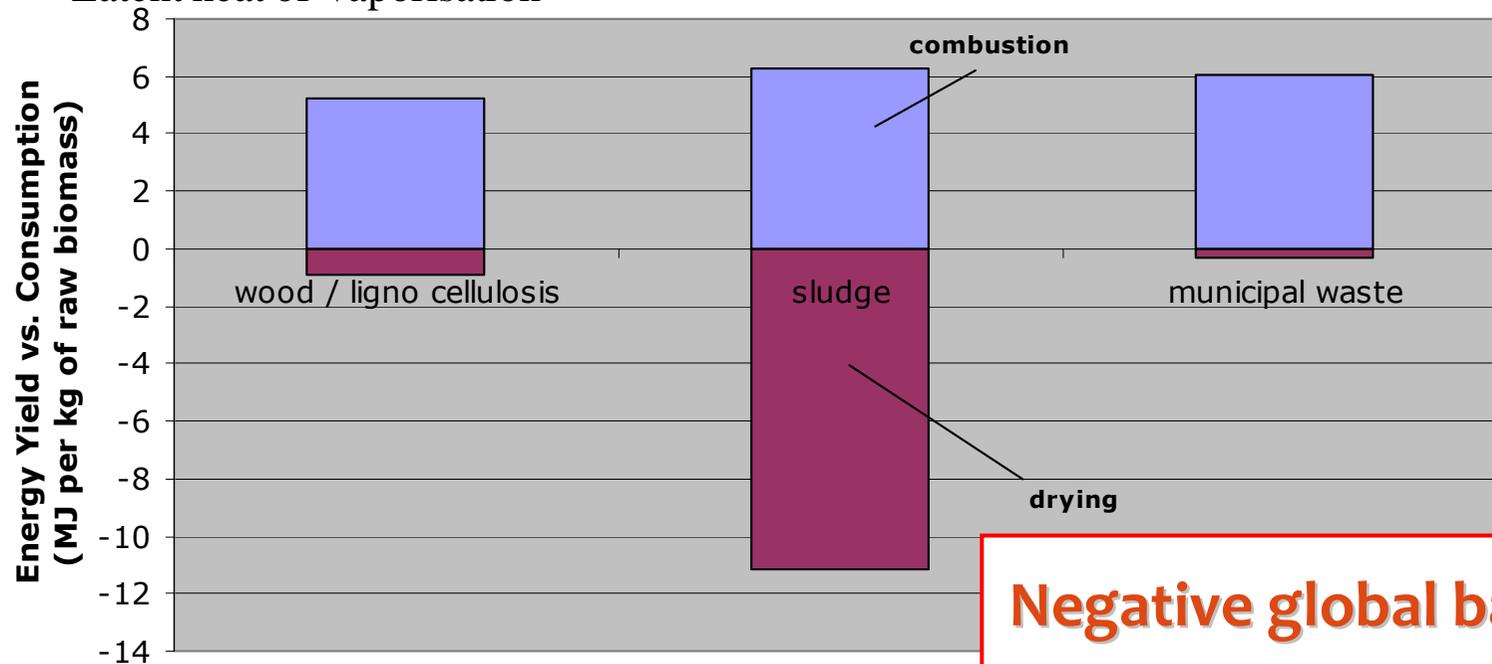


Importance of dryer efficiency

- Use of a dryer considered as 'efficient'

$$R_D = \frac{\text{Consumed energy}}{\text{Latent heat of vaporisation}} = 1.25$$

LHV = 8 MJ/kg for each fuel

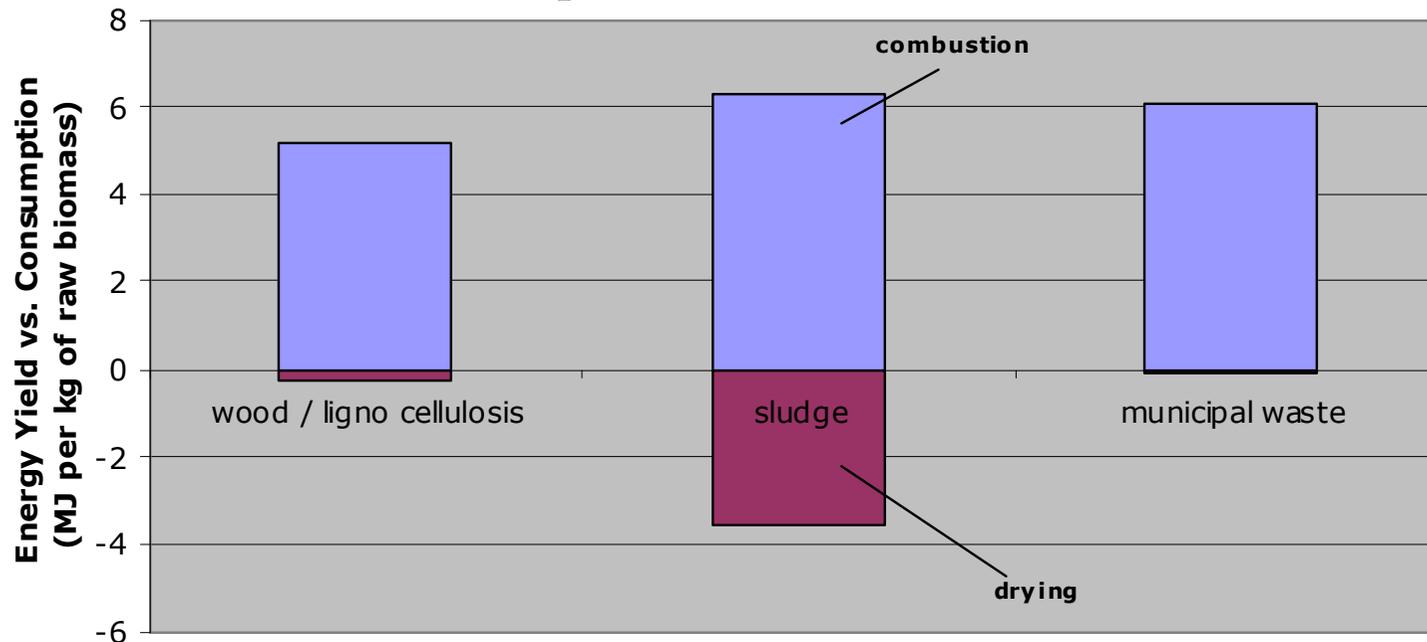


A. Léonard et al., Efficient sludge thermal processing: from drying to thermal valorization, Modern drying technology, Vol. 4

Importance of dryer efficiency

- Dewatering/drying coupled optimisation → positive balance

$$R_D = \frac{\text{Consumed energy}}{\text{Latent heat of vaporisation}} = 0.4$$



A. Léonard et al., Efficient sludge thermal processing: from drying to thermal valorization, Modern drying technology, Vol. 4

To conclude ...

Tomorrow ?

- Development of sludge drying within “zero energy” WWTP
- Vision of the whole site and sludge treatments to reach the energy optimum
- Diffusion of other drying technologies
 - SHS, frying, ...
- Research efforts
 - Links between sludge nature/history and drying
 - Low temperature + heat pump
 - Links between the texture of dry product and gasification/pyrolysis
 - ...

For more details ...

- Efficient sludge thermal processing: from drying to thermal valorization – Modern Drying Vol 4, edited by E. Tsotsas & A. Mujumdar, 2011, Wiley, 295-330, ISBN: 978-3-527-31559-8
- 3rd European Conference on Sludge Management – ECSM 2012, September 2012, Leon, Spain
- Contact us ...

Thanks for your attention !

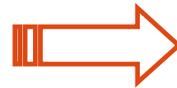
Considérations énergétiques



➤ Séchage des boues

750 à 1000 kWh/T eau
230 à 305 Euros/T MS

Sécher



Chaleur

Eliminer 1 kg d'eau



2250 kJ en théorie

Pertes, eau \pm liée



3000 à 5000 kJ en pratique

- Rendement : 60-65 %
- Pertes : min 5%